

1 **Microwave subcritical water pre-treatment and enzymatic hydrolysis of Geographical Identification (GI)**
2 **tag Indian black rice (*Chakhao Poireiton*) straw for fermentable sugar production**

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8

9 **Abstract**

10 Rice straw is an important feedstock for second-generation biorefineries, the majority being conventional
11 white rice. This research investigated the potential of the straw of black rice *Chakhao Poireiton*, a rice variety
12 of increasing importance, for biorefining. Pre-treatment of black rice straw was carried out in a pressurized
13 microwave reactor and free sugar release was measured following digestion with Cellic[®] CTec3. This was
14 compared to white rice straw. Pre-treatment (100 - 200° C for 5 min) did not drastically impact the sugar
15 composition but brought about an enhanced release of glucose after enzymatic hydrolysis from 25 to 50%
16 (black rice) and from 26 to 55% (white rice). For xylose digestibility, the increase was around seven-fold for
17 black rice (8 to 57%) and five-fold for white rice (13 to 64%). This improvement in digestibility of the straw
18 samples could have come from modification in the lignocellulose structural features making the
19 polysaccharides more susceptible to hydrolysis. Black rice could be a suitable feedstock for a combined
20 biorefinery – food and nutraceuticals from grain (much higher than white rice) and the straw for fermentable
21 sugars comparable to white rice straw for biofuels.

22

23 **Keywords**

24 Black rice; *Chakhao Poireiton*; Straw; Microwave Hydrothermal Pre-treatment; Enzymatic Saccharification;
25 Biorefining.

26

27 Introduction

28 As we strive towards self-reliance in terms of energy requirements, bioenergy is becoming more attractive,
29 especially, for its positive impact on the environment [1-4]. The residual straw from rice, which is the main
30 staple crop for many Asian countries and the third most grown cereal in the world, with a global production
31 of over 748 million tons [5], is currently a major biomass for the production of bioenergy. However, research
32 for other unconventional feedstock is necessary to meet the demand for biofuel production. Rice can be
33 differentiated based on its colours such as brown, white (polished brown rice), red, purple or black, and more
34 importantly based on its geographical origin. White rice is the most widely consumed rice, however,
35 pigmented rice such as black rice has higher overall health-beneficial components [6,7] (Table 1). Geographical
36 origin or place of production influences the characteristics or quality of food, and ultimately the purchasing
37 decision of consumers [8]. This is why certain food products are given Geographical Identification (GI). Black
38 rice *Chakhao Poireiton* from Manipur (India) which was awarded a GI tag in 2020 [9]. Figure 1 shows the
39 production process for rice. The unpolished grain and the husk are obtained from paddy rice (d) following
40 industrial milling. For conventional rice, the unpolished grain is what is called brown rice, which gets polished
41 to give white rice. However, black rice is usually not polished to maintain its nutritious bran and colour
42 characteristics [10].



43
44 **Figure 1** Production of black rice (*Chakhao Poireiton*) in Manipur, India. a) Three-month-old Black Rice field in
45 Manipur; b) Mature crop harvested and sundried in the field; c) Sundried crop (pile on left) threshed to get
46 grain (collected behind the machine) and straw (pile on right); d) Black rice paddy; e) Black rice grain de-husked
47 (or brown rice); f) Black rice husk; g) Black rice paddy bag and straw pile in the field; h) Black rice straw; i)
48 Burning of straw in the field. (e) and (f) are obtained after processing the paddy (d) in a rice mill where it
49 undergoes dehusking.

50

51

Table 1 Nutritional and phytochemical profiles of black, red and white rice

Phytochemicals^a	Black rice	Red rice	White rice⁺
Total Phytochemical content (µg/g)	4,351	297	32
Anthocyanins (%) ¹	80	1	0
Flavone and flavonols (%) ¹	11	7	75
γ oryzanol (%) ¹	1	27	25
Flavan-3-ols (%) ¹	8	65	0
Nutritional component^b	Black rice	Red rice	White rice⁺
Carbohydrate (%) ²	73	75	75
Ash (%) ²	1.56	1.36	1.26
Protein (%) ²	10.15	7.86	10.12
Fat (%) ²	2.85	2.48	2.92
Water (%) ²	13.01	13.32	11.08

52 ^a represents data obtained from Pereira-Caro et al [11]; ^b represents data obtained from Fatchiyah et al [12].

53 ¹ is expressed as a percentage of the total phytochemical content. ² is expressed as a percentage of the grain
54 biomass.

55

56 Black rice is generally cultivated in Southeast Asian countries [13], with China accounting for 62% of the global
57 black rice production followed by Sri Lanka, Indonesia, India, and the Philippines [14]. Owing to their health
58 beneficial properties, interest in black rice consumption has been rapidly increasing [15]. In India, along with
59 the awarding of GI, recent developments such as 100% *Chakhao Poireiton* beer that showed enhanced
60 oxidative stability [10] and the search for food with bioactive components have renewed the interest in this
61 aromatic black rice. Straw from black rice (*Chakhao Poireiton*) has also been reported as a source of bioactive
62 compounds such as anthocyanin with anticancer and antioxidant properties similar to anthocyanin from the
63 black rice grain [16]. The residual straw may also represent a source of biomass for bioenergy.

64

65 In India a surplus amount (44.5 Mt) of rice straw is burned annually, contributing to around 0.05% of
66 greenhouse gas emissions in India [17]. Hence, economically viable, socially acceptable and eco-friendly
67 solutions for the alternative uses of rice straw are needed [18]. Additionally, with Asia, led by China and India,
68 expected to drive nearly 50% (416 quadrillions Btu) of the global energy demand in 2050 [19], advancements
69 in low carbon energy such as bioenergy will need to have a stronger region-centric approach. This makes rice
70 straw an attractive lignocellulosic feedstock for biorefinery such as bio-ethanol production in India and China.
71 Currently, the production cost for bioethanol from rice straw is (23–26 \$/GJ) which is comparable to that of
72 fossil fuels (20–30 \$/GJ) [20]. However, by improving the pre-treatment, enzyme hydrolysis and productive
73 utilization of residual biomass, the bioethanol production process cost (1.19 \$/L) could be lowered to 0.45 \$/L
74 as shown in Vietnam (plant size, 200 ML per year) [21].

75

76 One pre-treatment method is the use of microwave heating which can be conducted at atmospheric pressure
77 or under high pressure. High-pressure microwave pre-treatment takes place in pressurised reactors at
78 temperatures ranging from 150 to 250° C [22]. At elevated temperature (>160° C) microwave pre-treatment
79 is in essence, an acid-catalysed reaction as acidity increases with increasing temperature during the treatment
80 [23]. In rice straw, microwave heating disrupts the silica waxy surface, breaks down the lignin–hemicellulose
81 complex, partially removing silicon and lignin and thus improving enzymatic hydrolysis [24]. When used with
82 water it also acts as a hydrothermal treatment dissolving part of the lignin and hemicellulose of the rice straw
83 [25]. Microwave pre-treatment is reported to have a greater impact on structural features of the
84 lignocellulose, such as reducing the cellulose crystallinity and/or decreasing the size of cellulose crystals thus
85 improving its enzymatic hydrolysis, than on the composition of the biomass [26,27]. Microwave pre-treatment
86 has been applied to conventional rice straw with varying efficiencies. This includes glucose yields of 37.8%
87 (680 W, 24 min, water) [24]; glucose yields of 11.2% (100° C, 5 min, solid acid catalyst) [28]; total sugar yields
88 of 71.41% (230 W, 5 min, acetic acid) and 80.08% (230 W, 5 min, propionic acid) [29]; glucose yields of 65%
89 (700 W, 30 min, 1 % NaOH) [30]; total sugar yields of 10 - 19% (160° C, 15 min, 1% H₂SO₄), 18-40% (160° C, 15
90 min, 1% NaOH) and 9-14% (160° C, 15 min, water) depending on rice variety [31]. Microwave hydrothermal

91 extraction at low severity (100° C, 5 min, water) has also been used to extract bioactive compounds from black
92 rice *Chakhao Poireiton* straw [16].

93

94 The majority of rice grown worldwide is white rice and as such has been the focus of previous studies into
95 exploitation for biorefining. To the best of our knowledge, this is the first and foremost study on microwave
96 subcritical water pre-treatment of black rice straw for sugar production. The objective was to evaluate the
97 sugar composition and its saccharification following microwave pre-treatment and enzymatic hydrolysis by
98 Cellic® CTec3. The released renewable sugars could be used for biofuels and high-value chemical production.

99

100 **Materials and Methods**

101 ***Plant Material***

102 The black rice (*Chakhao poireiton*) straw was obtained from a rice field in Imphal (India) located at 24° 53'
103 27.762'' N and 94° 6' 26.800'' E with an elevation of 799.51 m. The straw was air-dried and milled to 2 mm
104 mesh size using a Pulverisette 19 knife mill (FRITSCH GmbH, Germany) and stored at 4° C in bags with airtight
105 seals. White *Brojen* rice straw, from a neighbouring field in Imphal (India) located at 24° 53' 27.768'' N and 94°
106 6' 16.610'' E with an elevation of 798.34 m, was used for comparison and was treated as above.

107

108 ***Microwave pre-treatment***

109 Microwave pre-treatment was conducted in a pressurised Monowave 300 microwave generator (Anton Paar,
110 Germany) with 850 W maximum magnetron output power [32]. Accurate temperature control was maintained
111 using both external infrared and internal ruby based fibre optic thermometers. Output power and pressure
112 were not controllable, but controlled heating to a given set temperature in a given time was achieved by
113 choosing the inbuilt "as-fast-as-possible" mode followed by rapid cooling with a flow of nitrogen. 0.5 g of plant
114 material was added to 10 mL of water, steeped at room temperature for 2 min and then heated under pressure
115 for 5 min at six different temperatures 100° C, 120° C, 140° C, 160° C, 180° C and 200° C. The samples were
116 then centrifuged at 4472 x G for 10 min. The supernatants were filtered through 0.22 µm syringe filters, the

117 pH recorded and were stored at -20° C for further analysis. The residues were air-dried for 72 h, weighed and
118 were stored at 4° C for further analysis.

119

120 ***Sugar composition using High-Performance Anion-Exchange Chromatography (HPAEC)***

121 The sugar composition of raw biomass and the pre-treated residues was determined by Saeman hydrolysis
122 [33]. 1 mL of 12 M H₂SO₄ was added to 30 mg of the sample at 37° C for 1 h. This was followed by the addition
123 of 11 mL of MilliQ water (reducing the molarity to 1 M) and incubation at 100° C for 2 h. The hydrolysate was
124 analysed for monomer sugars by high-performance anion-exchange chromatography (HPAEC) on a Dionex ICS-
125 3000 comprised of a high-pressure GD 50 gradient pump, a guard column (Carbopac PA1, 4 mm × 50 mm), an
126 analytical column (Carbopac PA20, 4 mm × 250 mm) and a pulsed amperometric detector (PAD). 10 mM NaOH
127 was used as the mobile phase and the column was flushed with 200 mM NaOH between runs. The injection
128 volume was 10 µL and all chromatographic analyses were carried out at 30° C with a flow rate of 0.5 mL min⁻¹.
129 ¹. Samples and standards were diluted 1:100 in 10 mM NaOH and centrifuged at 4472 x G for 10 min before
130 loading to Dionex vials. Sugar standards ranged from 0.250 to 2 g L⁻¹ of arabinose, galactose, glucose and
131 xylose.

132

133 ***Digestibility Assay***

134 Air-dried pre-treated biomass residue was hydrolysed using Cellic[®] CTec3 (kindly provided by Novozyme A/S,
135 Denmark). This was carried out using a slight modification to the method described by the National Research
136 Energy Laboratory (NREL) [34]. The enzyme solution was made up using 5 mL of Cellic[®] CTec3 in 1 L of 50 mM
137 sodium citrate buffer, pH 3.76. 40 mL of the enzyme solution was added to 0.2 g of pre-treated residue and
138 incubated at 50° C, 150 rpm for 72 h in a shaking incubator (MaxQ 4358 shaking incubator, Thermo Scientific,
139 UK). Aliquots taken at 6 different time points; 0 h, 0.5 h, 3 h, 24 h, 48 h and 72 h were assessed for monomer
140 sugar composition using HPAEC. The sugar concentration present in the enzyme solution was also analysed
141 and subtracted to allow accurate calculation of the percentage of glucose released.

142

143 **Statistical analysis**

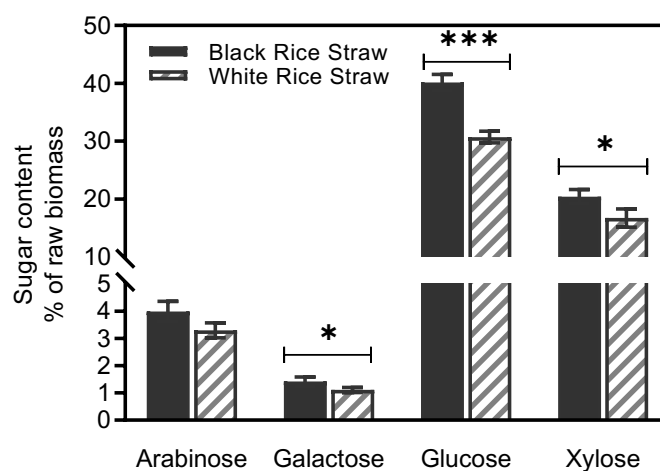
144 Statistical analysis of variance (ANOVA) and standard deviations were calculated using Prism 7.0b for Mac
145 (GraphPad Software, Inc) and Microsoft Excel 2016. All experiments were carried out in triplicates and the
146 results are mean \pm standard deviations. Differences were considered significant at $p < 0.05$, with * = $P \leq 0.05$;
147 ** = $P \leq 0.01$; *** = $P \leq 0.001$.

148

149 **Results and Discussion**

150 **Compositional analysis of straw**

151 The results of the sugar composition of the two straw samples are presented in Figure 2. Overall black rice
152 straw had a higher percentage of sugars than white straw. The glucose content of the straw was 40.2 ± 1.4
153 and $30.7 \pm 1\%$ for black and white rice, respectively. This being statistically significant ($p = 0.0003$). Whilst the
154 values for xylose were 20.4 ± 1 and $16.7 \pm 1.6\%$ for black and white rice, respectively, again this was statistically
155 significant ($p = 0.0230$). These values were in the range of the reported sugar composition of rice straw which
156 were 36-42% for glucose and 21-26% for xylose [35]. The other two sugars measured were, as expected, only
157 minor components of the straw. The differences between galactose of 1.4 ± 0.2 and $1.1 \pm 0.1\%$ ($p = 0.0377$)
158 were statistically significant while that for arabinose of 4.0 ± 0.4 and $3.3 \pm 0.3\%$ ($p = 0.0728$) was not significant,
159 for the black and white rice, respectively. The ratios of the sugars in each case are very similar and this may
160 suggest that black rice straw possesses a similar lignocellulosic make-up to that of white rice straw.



161 **Figure 2** Monomeric sugars composition of raw black rice straw compared against 'normal' white rice straw.
 162 Results are expressed as percentage of biomass (mean \pm SD, n = 3). * = P \leq 0.05; ** = P \leq 0.01; *** = P \leq 0.001.

163

164 ***Microwave pre-treatment***

165 Straw was subjected to pre-treatments at 100 - 200° C for 5 min. A short pre-treatment time was used since it
 166 has been shown that the effect of temperature is more important than residence time for reducing
 167 recalcitrance [36] and also avoids drastic degradation of the hydrolysate. Additionally, a previous study using
 168 autohydrolysis of rice straw by compressed liquid hot water at various temperatures (160, 180 and 200° C)
 169 and time (5, 10 and 15 min), found that the maximum glucose yield of 42.5% (percentage of pretreated
 170 biomass) was achieved at 200° C for 5 min [37].

171

172 The monomeric compositional changes in the pre-treated liquor are shown in Table 2. Increasing severity of
 173 the pre-treatment was accompanied by an increase in hemicellulosic derived arabinose in the pretreated
 174 liquor in both straw samples. At 200° C, galactose and xylose were detected, and the arabinose levels were
 175 double those found at 180° C. Glucose was detectable at 100° C in both straw samples and levels seemed to
 176 decline with increasing severity. This may represent free glucose or glucose derived from residual starch but
 177 in both straw samples, the glucose levels in the liquor at 200° C were very low. These values were in the range
 178 of the reported sugar composition of microwave pretreated rice straw (at 140° C - 210° C for 2.5 min to 160
 179 min) which were up to 0.2 % for glucose, 0.5 % for xylose, 0.35 % for galactose and 0.4 % for arabinose [38].

180

181 **Table 2** Changes in the composition of pre-treated rice straw liquor with different pre-treatment regime

Temp (° C) 5 min	Black Rice				White Rice			
	Sugars in pre-treated liquor (% of original biomass)				Sugars in pre-treated liquor (% of original biomass)			
	Ara	Gal	Glu	Xyl	Ara	Gal	Glu	Xyl
100	0	0	1.82 \pm 0.06	0	0	0	0.14 \pm 0.01	0
120	0	0	1.74 \pm 0.10	0	0	0	0.11 \pm 0.01	0
140	0.03 \pm 0	0	1.77 \pm 0.08	0	0	0	0.12 \pm 0.01	0

160	0.08 ± 0.01	0	1.75 ± 0.07	0	0.04 ± 0	0	0.11 ± 0.01	0
180	0.40 ± 0.06	0	1.57 ± 0.05	0.01 ± 0.02	0.30 ± 0.01	0	0.07 ± 0.01	0
200	0.96 ± 0.03	0.08 ± 0.01	1.00 ± 0.08	0.21 ± 0.09	0.6 ± 0.01	0.06 ± 0	0.04 ± 0	0.13 ± 0

182 Results are expressed as percentage of biomass (mean ± SD, n =3). Ara = arabinose; Gal = galactose; Glu =
 183 glucose; Xyl = xylose

184

185 The pH of the hydrolysate liquor was recorded and the solid residues were assessed for recovery and sugar
 186 composition as shown in Table 3. Overall, with an increase in severity of treatment, we observed a decrease
 187 in both the pH of the hydrolysate liquor and recovered weight of the solid residue along with subtle changes
 188 to the sugar composition of the recovered residue for both straws (black and white). In both straws pre-
 189 treatment up to 180° C does not seem to have a drastic impact on the composition of the pre-treated residue.
 190 However, between 180° C and 200° C there was a sudden decrease in the weight of the pre-treated biomass
 191 80% at 180° C - 67% at 200° C for black rice and 84 at 180° C - 73% at 200° C for the white rice. This compares
 192 with the changes seen in the sugar content of the pretreated liquor at 200° C (Table 2). This could be due to a
 193 combination of solubilisation of cell wall components (predominantly hemicelluloses and salts), hydrolysis and
 194 volatilisation of some wall components [39] as the severity was raised. The primary effect of the hydrothermal
 195 pre-treatment on biomass composition of both straw samples seems to have been partial but, incremental
 196 removal of hemicelluloses.

197 **Table 3** Changes in rice straw residues composition associated with different pre-treatment regimes

Temp. (° C, 5 min)	Black Rice						White Rice					
	Solid recovery (wt. %)	pH of hydrolysate	Sugar in pre-treated residue (% of residue biomass)				Solid recovery (wt. %)	pH of hydrolysate	Sugar in pre-treated residue (% of residue biomass)			
			Ara	Gal	Glu	Xyl			Ara	Gal	Glu	Xyl
100	86.4 ± 1	6.1 ± 0.01	3.8 ± 0.2	1.2 ± 0.1	43.7 ± 1.4	33.9 ± 1.0	90.3 ± 0	6.7 ± 0.01	4.2 ± 0.1	1.4 ± 0.1	40.4 ± 1.9	22.6 ± 0.8
120	84.7 ± 0	6.0 ± 0.01	3.8 ± 0.2	1.2 ± 0.1	42.1 ± 1.9	32.8 ± 1.3	89.3 ± 1	6.5 ± 0.10	4.1 ± 0.3	1.4 ± 0.1	40.3 ± 2.3	22.3 ± 1.5
140	83.5 ± 1	5.7 ± 0.03	4.0 ± 0.2	1.2 ± 0.0	43.6 ± 1.4	34.2 ± 0.8	88.3 ± 1	6.2 ± 0.06	3.8 ± 0.4	1.3 ± 0.1	38.8 ± 1.8	21.0 ± 1.0

160	82.5 ±1	5.2 ±0.03	3.8 ±0.2	1.1 ±0.1	43.1 ±2.1	23.4 ±1.2	88.9 ±0	5.7 ±0.03	3.8 ±0.3	1.3 ±0.1	39.3 ±2.7	21.3 ±1.2
180	80.4 ±1	4.7 ±0.02	3.3 ±0.2	1.0 ±0.1	42.8 ±1.9	23.1 ±1.0	84.1 ±1	5.1 ±0.03	3.4 ±0.1	1.1 ±0.0	40.0 ±1.3	21.3 ±1.0
200	67.5 ±2	4.1 ±0.02	2.0 ±0.4	0.3 ±0.4	46.0 ±2.6	18.4 ±2.5	73.1 ±1	4.6 ±0.04	2.0 ±0.1	0.7 ±0.0	43.0 ±2.7	17.2 ±0.8

198 Results are expressed as the percentage of biomass (mean ± SD, n =3). Ara: arabinose; Gal: galactose; Glu:
199 glucose; Xyl: xylose
200

201 ***Enzymatic saccharification***

202 Glucose and xylose released after 72 h of hydrolysis of the pre-treated biomass are shown in Figure 3.
203 Digestibility was expressed as the percentage of available sugar in the pre-treated biomass released after 72
204 h. Associated with the drastic loss of weight between treatments at 180° C and 200° C, the residues showed
205 reduced recalcitrance from 180° C as demonstrated by an increase in digestibility. For both straw samples,
206 pre-treatment from 100° C to 200° C for 5 min resulted in a two-fold increase in glucose digestibility; 24.9 ±
207 0.35 to 49.6 ±1.4 and 26.81 ±1.08 to 55.1 ± 2.4% for black and white rice straw, respectively. For xylose
208 digestibility, the increase was around seven-fold for black rice (7.6 ± 1.3 to 57.0 ± 4.3%), while the increase
209 was around five-fold for white rice (13.2 ± 0.1 to 64.1 ± 3.1%). Galactose was detectable only from black rice
210 straw pre-treatment at 180° C and 200° C. This could be due to the low amounts of galactose in the pre-treated
211 residue. These differences in digestibility between the two straw samples under the same pre-treatment and
212 enzymatic hydrolysis further highlights the importance of rice variety on digestibility [31,40]. Depending on
213 rice variety, the digestibility of rice straw pre-treated with water at 160° C for 15 min has been shown to range
214 from 9 - 14% [31].
215

216 The highest enzymatic digestibility was obtained after pre-treatment at 200° C, with glucose digestibility of
217 49.6 ± 1.4% and 55.1 ± 2.4% for black and white rice straws, respectively (p = 0.03). These values equate to a
218 glucose yield of around 147 and 173 mg g⁻¹ of original straw for black and white straw, respectively. While the
219 xylose yield equates to around 67 and 80.2 mg g⁻¹ of original straw for black and white straw, respectively. The
220 theoretical yield of bioethanol from black rice straw would thus be about 110 g kg⁻¹ straw, based on the

221 theoretical ethanol yield per gram of biomass [41]. Hence, black rice straw is a lignocellulosic biorefinery
222 feedstock comparable to white rice straw. These values are also similar to a previously reported glucose
223 saccharification efficiency of 45% using steam explosion (220° C for 10 min) for rice straw [39].

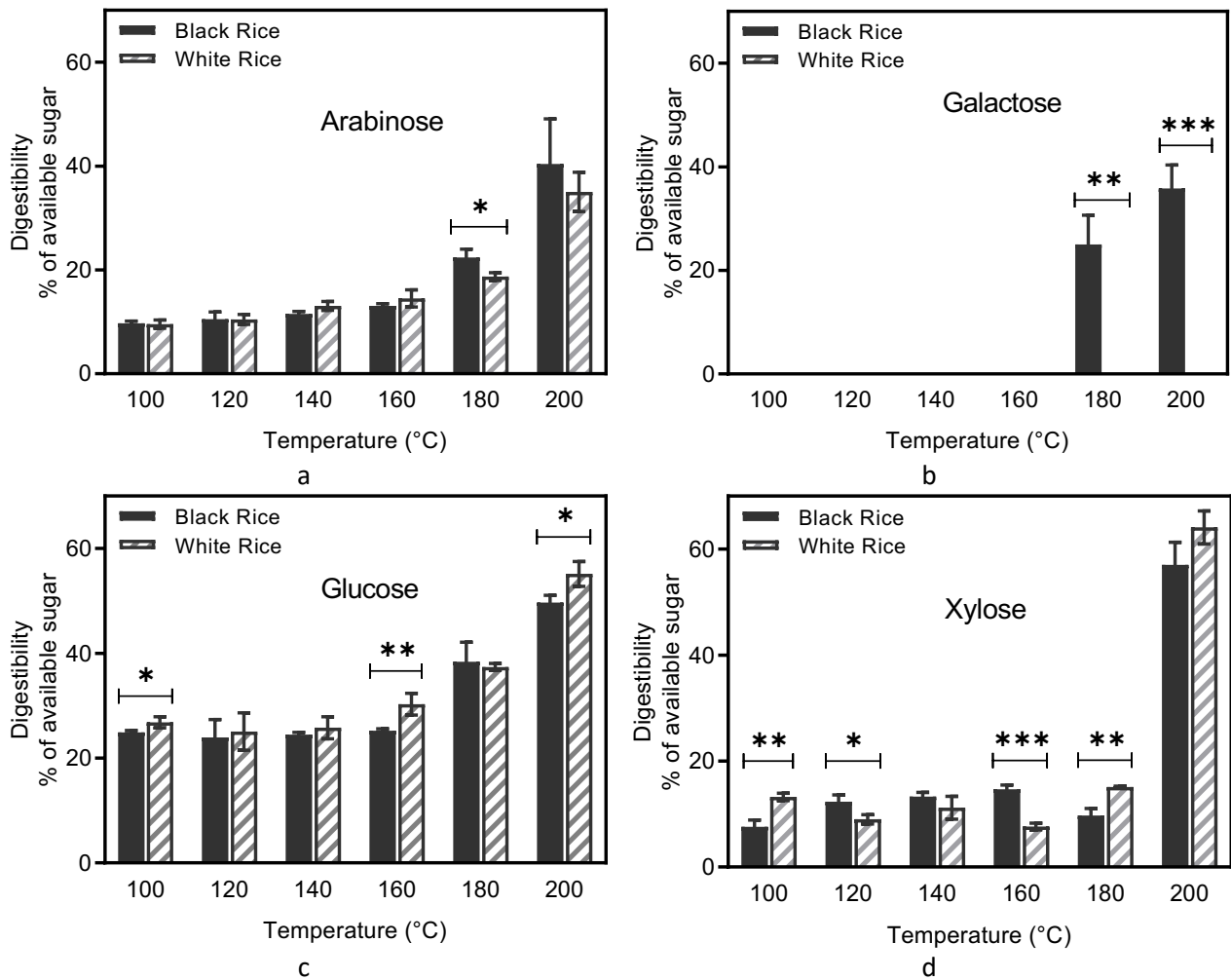
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225 The increase in digestibility could be due to a multitude of changes in the lignocellulose matrix brought about
226 by the pre-treatment. A) Reduction in cellulose crystallinity and/or decrease in the size of cellulose crystals
227 [26,27]. B) Alterations or changes in the surface area of pre-treated rice biomass [42]. C) Removal of barriers
228 to enzymatic hydrolysis such as hemicellulose and lignin [43]. In rice straw, microwave heating has been shown
229 to disrupt the silica waxy surface, break down the lignin–hemicellulose complex, partially remove silicon and
230 lignin thus improving enzymatic hydrolysis [24]. D) Creation of an explosion effect in the biomass matrix due
231 to microwave’s selective heating of the more polar parts of the lignocellulosic feedstock which facilitates the
232 degradation of recalcitrant structures more efficiently [44]. This has been reported to provide 12 times higher
233 sugar yield within half the time compared to conventional heating [45].

234

235 The observed glucose yields for both the black and white rice straws are comparable to previous reports of
236 white straw under similar treatment conditions. For example, a yield of 42.5% was obtained with compressed
237 liquid hot water pre-treatment at 200° C for 5 min [37]; 46.6% after a two-stage 0.5% H₂SO₄ at 15 bar for 10
238 min and 30 bar for 3 min pre-treatment [46]; 57.7% after a compressed liquid hot water pre-treatment at 180°
239 C for 10 min with 0.25% Oxalic acid [42]; 31.7% after a microwave pre-treatment at 680 W for 24 min with
240 water [24] and 45% after steam explosion pre-treatment at 220° C for 10 min [39].

241



242 **Figure 3** Monomeric sugar release from pre-treated black rice and white rice straw residues after 72 h of
 243 enzymatic saccharification (mean \pm SD, n = 3). a) Arabinose; b) Galactose; c) Glucose and d) Xylose digestibility
 244 expressed as a percentage of available sugar in the pre-treated biomass. * = $P \leq 0.05$; ** = $P \leq 0.01$; *** = $P \leq$
 245 0.001.

246

247 However, these observed glucose yields for both black and white rice straws were lower than reported using
 248 other pre-treatments. The glucose yields for white rice straw include 85% after pre-treatment with 0.8% H_2SO_4
 249 for 4 min at 190° C [47]; 76.3% after pre-treatment with 0.015% HCl at 200° C for 60 min and 85% after a hot-
 250 compressed water pre-treatment of 180° C for 30 min [48]; 95.4% after Glycerol- $AlCl_3$ pre-treatment at 146.8°
 251 C for 20 min [49]; 94% after 0.055 mol/L $AlCl_3$ pre-treatment at 150° C for 0.5 h [50] and 90.2% after a 3 h pre-
 252 treatment at 100° C and two-stage deep eutectic solvent pre-treatment [51]. Even though these reported
 253 yields were higher, these treatments were often conducted at higher severity or used chemicals that would
 254 involve neutralisation or other additional steps downstream before fermentation.

255

256 The impact of microwave pre-treatment on black rice husk was also explored (Table 4). Black rice husk showed
 257 good sugar composition in both raw (glucose 33.7% ± 1.1, expressed as a percentage of original biomass) and
 258 pre-treated states (glucose 41.3% ± 3.4, expressed as a percentage of pre-treated residual biomass). However,
 259 the digestibility of the husk following pre-treatment at 200° C for 5 min was only 15.5% ± 1.6, expressed as a
 260 percentage of available sugars. This observed value for black rice husk is similar to that reported for white rice
 261 husk (16.3% glucose digestibility after microwave pre-treatment at 210° C for 2 h) [52]. This high recalcitrance
 262 in the husk may be related to the fact that white rice husk has almost twice the lignin content of rice straw
 263 [52].

264

265 **Table 4** Sugar composition of raw black rice husk, its sugar composition and digestibility following pre-
 266 treatment at 200° C for 5 min

	Arabinose	Galactose	Glucose	Xylose
Sugar composition of raw husk (% of original biomass)	2.31 ± 0.04	0.94 ± 0.08	33.69 ± 1.06	16.15 ± 0.5
Sugar composition of pre-treated residue (% of pre-treated biomass) Wt. of recovered residue 76 % ± 1	1.05 ± 0.10	0.00 ± 0.00	41.25 ± 3.37	14.30 ± 1.34
Sugar composition of pre-treated liquor (% of pre-treated biomass) pH of pre-treated liquor 4.4 ± 0.05	0.4 ± 0.01	0.05 ± 0	0.13 ± 0.01	0.08 ± 0.06
Digestibility (% of available sugar)	0.00 ± 0.00	0.00 ± 0.00	15.48 ± 1.59	11.93 ± 0.46

267 Results are expressed as the percentage of biomass (mean ± SD, n =3). Raw sugar composition is expressed as
 268 a percentage of the original biomass. Sugar in the pre-treated biomass is expressed as a percentage of the pre-
 269 treated biomass. Digestibility of the pre-treated biomass is expressed as a percentage of available sugar in the
 270 pre-treated biomass measured via HPAEC.

271 The current study shows the potential of black rice as a source of lignocellulosic biomass suitable for second-
 272 generation biofuels by generating fermentable sugars comparable to white rice straw. The search for
 273 economical biofuels is crucial as they will not only contribute to reducing emission in road and aviation but

274 also in marine and inland transport [53]. Fermentation and recovery of bioethanol were not attempted in this
275 study. However, the potential theoretical yield of bioethanol from black rice straw from this study would be
276 about 110 g kg⁻¹ straw. However, further studies for pre-treatment and hydrolysis optimisation are required
277 to further enhance digestibility and sugar release. This could include optimising the microwave pre-treatment
278 with acid and alkali [31] or application of green pre-treatment method such as ionic liquids to further improve
279 its yield. However, these higher severity processes would also encompass higher cost and challenges
280 downstream through the potential production of fermentation inhibitors. The production cost for second-
281 generation biofuels is two to three times more expensive than petroleum fuels on an energy equivalent basis
282 [54]. With the black rice, the economics of its straw biorefinery could potentially be balanced by its high-value
283 grain. Valorising the learnings from white rice straw, it is reasonable to envisage that the different components
284 present in the black rice straw such as cellulose, hemicelluloses, lignin and extractives would also need to be
285 capitalised on to make the process economically viable.

286

287 Plants like black rice could help us move from a food vs fuel debate to a combined food, health and fuel
288 solution, within the limits of our planetary boundary. A combined biorefinery where black rice grain provides
289 food with health-promoting compounds, while the straw providing fermentable sugars for the production of
290 bioproducts such as biofuels could be further explored on a small scale. Similar concepts are available for
291 wheat - improving wheat to give better grain yield while also possessing straw suitable for biorefinery [55,56].

292 White rice straw has been reported to contain a variety of bioactive compounds such as water-soluble
293 phenolic acids (ferulic, p-coumaric and protocatechuic) and flavonoids [57,58]. Through response surface
294 methodology (RSM) the microwave subcritical water pre-treatment process could be optimised to develop a
295 two-step process where these bioactive compounds such as anthocyanin [17,70] could be extracted at a lower
296 severity from the black rice straw followed by pre-treatment at higher severity for fermentable sugars. Black
297 rice grain is popular for its nutraceutical properties and its production could further be fuelled by the renewed
298 interest in health-promoting foods and the award of GI tag. With the growing interest in the link between

299 health and food, exploring the biorefinery potential of by-products of plants such as black rice would be a
300 timely study.

301

302 In this research, we have explored the potential for producing fermentable sugars from black rice straw. These
303 sugars could be converted to various products such as liquid fuels, furfurals and hydroxymethylfurfurals
304 (HMFs). However, within this biochemical route, the straw's potential for producing biogas and aromatic
305 products could also be explored. Then, there is the thermochemical route, which could be more suitable for
306 black rice husk. Under this route, both the straw and the husk could be explored as a feedstock for producing
307 synthetic gas, bio-oil and heat and electricity [59]. Exploring the biorefinery potential of black rice straw would
308 be an important and timely step to develop an economically feasible biorefinery concept. Reduction in
309 greenhouse gas (GHG) from this concept could be delivered in three ways – i) reducing our reliance on fossil
310 fuels by providing biofuels, ii) reducing the burning of rice straws by diverting them to the biorefinery, and iii)
311 reutilising the by-products of Agri-Food Industry which is also a major contributor of GHGs.

312

313 **Conclusion**

314 In this study, a lab-scale microwave subcritical water pretreatment experiment followed by enzymatic
315 hydrolysis was conducted on the GI tag Indian black rice (*Chakhao Poireiton*) straw obtained from Imphal,
316 Manipur and compared white rice straw also obtained from Imphal. Following enzyme hydrolysis, the black
317 rice straw yielded fermentable sugars comparable to, or slightly higher than that obtained from white rice
318 straw. The sugar content of black rice straw was higher than white rice straw for all measured sugars
319 (arabinose, galactose, glucose and xylose). This indicates the potential of black rice straw as an additional
320 biomass substrate for the production of biofuels and biobased chemicals. However, this biomass required a
321 pre-treatment above 160° C for 5 min to obtain a significant impact on the subsequent enzyme hydrolysis,
322 with a glucose digestibility of 49.6 ±1.4% at 200° C for 5 min compared to 55.1 ± 2.4% observed with white rice
323 straw. This indicates the need for further study into the optimisation of pre-treatment technologies to improve
324 the digestibility of the black rice straw. Optimisation studies on the present process or alternative routes such

325 as thermochemical processes are needed for efficient utilisation of this feedstock which would otherwise be
326 burnt on the field creating environmental and health issues, and loss of biological resource. With the growing
327 interest in the link between health and food, exploring the biorefinery potential of plants residues, such as
328 black rice, would be a timely study.

329

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336

337 **Disclosure statement**

338 The authors declare that they have no conflict of interest.

339

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