

Review of solidification and melting performance of phase change materials in the presence of magnetic field, rotation, tilt angle, and vibration

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Abstract

Due to the poor thermal conductivity of phase change materials (PCMs), the operation of Latent heat thermal energy storage (LHTES) is restricted by the limited heat exchange rate between PCMs and heat sources or sinks. The current review discusses the effects of magnetic field, rotation, tilt angle, and vibration on the discharging and charging heat performance of PCMs and nano-enhanced PCMs (NEPCMs) which are encapsulated in various container geometries and orientations based on melting and solidification standpoints. From this review, it is concluded that the orientation and design of the heat exchanger has a significant effect on the melting/solidification performance. The melting and solidification performance have been improved by increasing the magnetic number and decreasing the Hartmann number. Moreover, rotating cavity in a counter direction of buoyancy flow has improved the melting rate/time. The optimum tilting angle varies depending on the thickness of PCM layers. In terms of the vibration effect, frequency and amplitude/frequency are found to have an important role at low

34 and high discharge rates, respectively. Following a comprehensive review, a few suggestions
35 are provided as future research topic in this field.

36 **Keywords:** Phase change materials; Latent heat thermal energy storage, Magnetic field;
37 Rotation; Tilt angle; Vibration.

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61

62 **1. Introduction**

63 To mitigate the solar fluctuations and ensure an uninterrupted supply of renewable energy,
64 electrochemical storage systems (ESS) and thermal energy storage (TES) systems enable the
65 storage of surplus energy for the use in downstream applications during high-demand periods.
66 There are three main methods to store thermal energy including sensible heat storage, latent

67 heat storage, and thermal storage—among which latent heat TES (LHTES) using phase change
68 materials (PCMs) provide a higher storage density at relatively smaller size and lower
69 temperature difference between releasing and storing processes [1,2].

70 PCMs have been widely used in the residential structures, building envelopes, and concentrated
71 solar thermal systems [3-5]. They are arranged in sphere, rods, solid cylinders, solid flat plates,
72 and other enclosure types [6-10]. PCMs are classified as organics (paraffins and non-
73 paraffins), inorganics (salt hydrates and metallics), and eutectics of inorganic and organic
74 compounds (organic-organic, inorganic-inorganic, and inorganic-organic) [11]. Inorganic
75 PCMs have high latent heat values and high thermal conductivity. However, the main
76 challenges with inorganic PCMs are corrosion, improper re-solidification, instability,
77 which result in phase decomposition, and sub-cooling. Organic PCMs are more chemically
78 stable than inorganic PCMs, but at the expense of inferior heat transfer characteristics,
79 higher volume change, and flammability. Eutectics, the final type of PCM, have a high
80 volumetric thermal storage density, high thermal conductivity, and a high latent heat of
81 fusion per unit volume, although they are relatively expensive and heavy [12].

82 In order to improve the heat transfer properties of PCMs, several heat transfer enhancement
83 techniques have been suggested in the literature. Active techniques rely on an external energy
84 source such as electrohydrodynamic (EHD), magnetohydrodynamics (MHD), surface
85 vibration, and mechanical motion to enhance the heat transfer rate [13, 14]. On the other hand,
86 passive techniques do not require external forces and are primarily concerned with (i) surface
87 modification through adding fins with various geometries (such as longitudinal fins [11, 15],
88 circular fins [16-20], angled fins [21, 22], twisted fins [23], and tree-like branching and
89 rectangular fins [24]), (ii) employing nanoparticles into the base fluid [25-27] (such as CuO
90 [28, 29], copper [30], aluminum oxide and silver [31], or aluminum matrix [32]), (iii) using
91 porous materials [33-35], (iv) changing the channel arrangement of the heat transfer fluid
92 (HTF) [36-38], and (v) changing the configuration of the systems [5, 39-42]. Compound
93 method is referred to a combination of active and passive techniques to improve the heat
94 transfer.

95 During recent years, there has been a growing tendency towards investigating the heat transfer
96 enhancement between PCMs and heat sources for various industrial applications. In this regard,
97 several review papers have been published considering the employment of different
98 enhancement methods including the metal foam [43], nanofluid [44], extended surfaces [45],
99 and hybrid approaches [11]. To the best of authors' knowledge, there is a lack of a detailed
100 review to highlight the effects of magnetic field, rotation, tilt angle, and vibration on the thermal

101 storage performance of PCMs and nano-enhanced PCMs (NEPCMs) at variable container
102 geometries. There are no holistic evaluations of the many findings from various experimental
103 and numerical investigations regarding the effect of these techniques in the literature. The
104 above-mentioned approaches have been deployed in a wide range of applications such as air
105 conditioning and refrigeration industries, heat exchanger, compact electronics, and medical
106 field [46]. Due to its significant contribution to improve the heat transfer [13, 14], this review
107 aims at evaluating the emerging trends in enhancing the heat transfer rate and shortening the
108 melting/solidification time of PCMs/NEPCMs for several industrial applications. This is
109 followed by concluding remarks complemented by key topics for future work.

110 **2. Methodology**

111 This paper presents a comprehensive review on the effect of magnetic field, rotation, tilting
112 angle, and vibration on the performance of PCM-based storage systems. A wide range of
113 PCM/NEPCM container geometries including rectangular, cylindrical, square, annulus, and
114 shell-and-tube is considered from melting and solidification perspectives. The advantages and
115 disadvantages of each parameter are discussed in detail. The literature review is based on the
116 papers selected from diverse academic databases and publishers including ELSEVIER, MDPI,
117 ScienceDirect, Springer, and international conferences.

118 The first section of this review is dedicated to magnetic field role in various containers of
119 PCMs/NEPCMs. Different important concepts including Lorentze force, Hatman number,
120 Reynolds number, nanoparticles effect, fins/metal foam addition, uniformity and types of the
121 magnetic field are discussed in this section. The second section focused on the role of rotation
122 on the melting and solidification performance of PCMs/NEPCMs. The objective of this section
123 is to gain further understanding on how rotational speed/mode and container geometries can
124 influence the phase change process. The next section presents a review on whether tilting angle
125 of either heating surface or phase change container enhances or deteriorates the PCM
126 melting/solidification processes. The synergy between this parameter and fin/nanoparticle
127 addition has been evaluated to check how the conclusions might change in the presence of these
128 parameters. The last section is devoted to the vibration effect considering PCM container
129 configurations, and the frequency/amplitude of the vibration. At the beginning of each section,
130 there is a table summarising the type of study either numerical or experimental, studied
131 parameters, and key take-away findings of each paper. This is followed by a detailed discussion
132 in the subsequent subsections. The last section summarises the key findings of this review
133 followed by some recommendations for future work.

134 This paper provides a well-organized review that includes the definition, description,
135 configuration, examined parameters, and most important conclusions of the selected articles.
136 The emerging trends in renewable energy uptake, more specifically solar energy, for various
137 industrial applications require a detailed review, essentially pointing toward techniques to
138 overcome the challenges associated with charging/discharging response of LHTES
139 technologies.

140 **3. Effect of magnetic field**

141 Magnetic-field is a method to control the convective heat transfer inside an enclosure. Table 1
142 lists the geometrical, operating conditions, and key take-away findings of recent studies
143 addressing the role magnetic field on the melting/solidification procedures of PCMs/NEPCMs
144 encapsulated inside an enclosure with different geometries. The citation list [8, 47–65] focuses
145 on this importance in different geometries as summarized in the following subsections.

Table 1. A summary of studies on magnetic field effect on the melting/solidification procedures of PCMs/NEPCMs inside an enclosure with different geometries

Authors (year)	Configuration	Type of study	Studied parameters	Highlighted results/findings
Sheikholeslami and Mahian (2019) [8]	Porous annulus containing NEPCM	Numerical	Effect of Lorentz force, NEPCM concentration, and Rayleigh number on the solidification process	23.5% reduction in the solidification time by increasing the Hartmann number from 0 to 10. 14% decrease in the solidification time can be accomplished by adding nanoparticle up to 4% concentration.
Lei et al. (2015) [47]	Rectangular cavity containing dispersed carbon nanomaterial and sodium dodecyl benzene sulfonate (SDBS) in paraffin	Experimental	Effect of magnetic field on the solidification process	Homogeneous distribution of the particles in the solid area as a result of induced electromagnetic field.
Laouer et al. (2021) [48]	Copper-water NEPCM inside a rectangular cavity enclosure	Numerical	Effect of Hartmann number, nanoparticle volume fraction, and Rayleigh number on the melting of Cu-Ice	Decreased melting time by 10% at high Rayleigh number of 10^5 in the absence of magnetic field. Shortening the charging time at low Rayleigh number, while extending at high Rayleigh number with the addition of nanoparticle and in the presence of magnetic field.
Fan et al. (2021) [49]	Scattered magnetic particles with rotating magnetic field and PCM inside an inner layer of a glass casting cylinder	Experimental	Effect of particle fraction and rotational speed on the melting process	Rotational speed of 20 r.min^{-1} with 1.0 wt.% particle fraction shortened the melting time by 22.9%. Vertical solid-liquid interface as a result of induced forced convection by the magnetic field.
Farahani et al. (2022) [50]	Employing fins with different shapes in a 3D cylindrical enclosure containing PCM	Numerical	Effect of fin shapes, non-uniform magnetic field and fin materials on the melting process	Improvement in the charging rate by 31.8% and 37.87% for continuous spiral fins and rectangular fins. Non-uniform magnetic field as a dominant parameter in accelerating the melting rate by 78% in case of spiral fins. 3% enhancement in the melting process through fabricating the fins from copper rather than aluminum.
Farahani et al. (2022) [51]	Nanoparticles embedded PCM in a 3D cylindrical enclosure with novel fin shapes	Numerical	Effect of non-uniform magnetic field, fin shape, and nanoparticle volume fraction on the melting process	Wide range of improvement in the melting process (i.e. 2–40%) depending of the fin shape. 1.5–2.5% increase in the melting fraction as a result of an increase in the nanoparticle volume fraction from 2.5 to 5%. Enhancement in the charging process when the strength of the magnetic field increased in the range of 16–57%.
Saha (2022) [52]	Gallium PCM in a semi-circular container with the heated circumferential wall	Numerical	Effect of magnetic field strength/direction, Rayleigh number, gravity conditions, and Marangoni number on the melting and solidification processes	Marginal effect of magnetic field direction on the charging/discharging performance. Prolonged duration of the melting time at higher Hartmann numbers. Shortened melting time under microgravity condition due to the thermos-capillary convection with/without the magnetic field.

Selimefendigil and Öztop (2022) [53]	Convection of hybrid nanofluid in a PCM-filled cylinder	Numerical	Effect of bifurcation location, Hartmann number, Reynolds number, and nanoparticle concentration on the melting and solidification processes	Decrease in the phase change time by 73% and 26% for bifurcating and flat channels at higher Reynolds number. Opposite behavior of phase-change dynamics for bifurcation and flat channels when magnetic field strength varied.
Kohyani et al. (2017) [54]	Cyclohexane–copper nano-PCM in a square porous cavity	Numerical	Effect of porosity, Hartmann number, solid volume fraction, and Rayleigh number (Ra) on the melting process	Reducing the melting time in the presence of the magnetic field. Intensified melting rate by increasing the Rayleigh number. Porosity as a more dominant factor compared to solid volume fraction.
Ghalambaz et al. (2019) [55]	Non-Newtonian behavior of magneto- and ferro-hydrodynamic PCM in a filled 2D square enclosure	Numerical	Effect of Rayleigh number, Hartmann number, Power-law index, and magnetic parameter on the melting front, Nusselt number, and normalized melt volume fraction (NMVF)	Slowing down the melting process by increasing the Hartmann number. Intensification in the Nusselt number by increasing the power index and magnetic parameter, and reducing the Hartmann number. Enhancement and reduction in the NMVF by increasing magnetic parameter and Hartmann number.
Mehryan et al. (2019) [56]	PCM-filled 2D square cavity subjected to two magnetic fields	Numerical	Effect of non-uniform magnetic source with different strength on the melting process	Intensity of the magnetic fields as the dominant factor on the progress of the melting front. Reduction in the melting front by an increase in the Hartmann number.
Kumar et al. (2022) [57]	Paraffin PCM and copper nanoparticles in a 2D square cavity	Numerical	Effect of heated wall orientation and nanoparticle volume fraction on the melting process under uniform magnetic field on the melting process	Maximum melting rate and energy storage capacity at a 2% and 0.5% nanoparticle concentration. Reduction in the stored energy capacity by 9% under different orientations of the cavity due to an increase in the magnetic field intensity.
Dibavar et al. (2018) [58]	NEPCM inside an annulus enclosure	Numerical	Effect of non-uniform magnetic on the melting and solidification processes	Reducing the time required for charging and discharging processes by up to 39.91% and 14.29% for non-electrical conductive magnetic nanofluid. Accelerated melting/solidification by increasing the magnetic number, while deteriorated melting/solidification by increasing the Hartmann number in case of electrical conductive ferrofluid.
Sheikholeslami (2018) [59]	CuO nanoparticles NEPCM in a porous TES curved enclosure in the presence of	Numerical	Effect of Hartmann number, volume fraction of nanofluid and Rayleigh number on the solidification process	Promoting the solidification performance by applying Lorentz forces. Reverse relationship between the solidification time with the volume fraction of nanofluid and Hartmann number.
Ghalambaz et al. (2019) [60]	Analysing the transmission of heat via moving mesh method in electrically conductive PCM inside a cavity enclosure	Numerical	Effect of Hartmann number and the location of non-uniform magnetic fields on the melting process	Significant effect of magnetic field at later stages of the melting process (Fourier number, Fo, greater than 1.15). Reduced Fo from 10.4 to 9.0 by changing the location of magnetic source from the bottom to middle of the cavity.
Shi et al. (2020) [61]	Paraffin type A16 with Fe ₃ O ₄ nanoparticles in a 3D shell and multi-tube TES system	Numerical	Effect of quadrupole magnet field on the melting and solidification processes,	80.02% and 53.19% improvement in the charging and discharging time for the magnetic field with 50 mT intensity. Longer solidification time compared to the charging time with and without magnetic field.

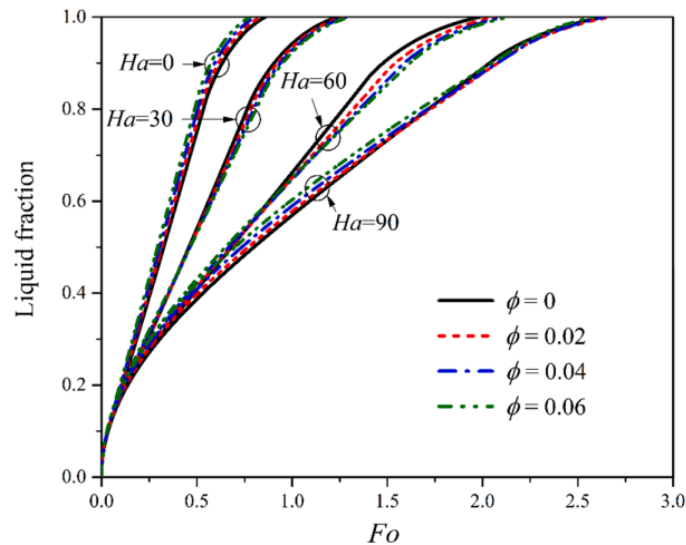
				Improving the cyclic processes through reducing the difference between charging and discharging time in the presence of the magnetic field.
Selimefendigil and Öztop (2020) [62]	Artificial neural network (ANN) to predict the thermal performance of PCM in a 2D cavity	Numerical	Effect of Hartmann numbers, hybrid nanoparticle volume, and porosity of the medium on the melting process	Hartmann number of 40 reduced the charging time by 40%. Maximum 18.5% decrease in the charging time in the presence of hybrid nanoparticles. Reliable prediction of the melting time by ANN modeling approach.
Fan et al. (2021) [63]	Magnetic particles driven by a magnetic field in liquid PCM moving between the solid-liquid interface and the heating surface	Experimental	Effect of particle fraction and magnetic field frequency on the melting process	An experimental correlation for predicting the Nusselt number. Decrease in the melting time by 15.8% in the case of heating surface having 55°C. Maximum enhancement in the heat transfer by 25.4%.
He et al. (2022) [64]	Fe ₃ O ₄ -paraffin PCM inside a cavity subjected to uniform magnetic field	Experimental	Effect of nanoparticle concentration and the strength/direction of the magnetic field on the solidification process	Local non-uniformity in the solid phase increased/decreased under positive/negative fields. Positive magnetic field increased the heat flux, energy release, and solid-phase fraction by 29.2%, 19.2%, and 24.8%, respectively. Unmanaged increase in the magnetic induction deteriorating the economic advantage of phase change regulation.
Aly et al. (2022) [65]	Incompressible Smoothed Particle Hydrodynamics (ISPH) method to analyse MHD thermosolutal convection of NEPCMs suspended in a porous wavy cavity containing high-temperature crescents	Numerical	Effect of time-fractional derivative, Hartmann number, nanoparticle concentration, and thermal radiation parameter	Reduction in the movement of NEPCM by increasing the time-fractional derivative, Hartmann number, and solid volume fraction. Decrease in the nanofluid speed by 26.3% by increasing the time-fractional derivative, α , from 0.95 to 1. Improvement in the nanofluid movement by increasing the thermal radiation factor.

148

149

150 3.1 Rectangular geometry

151 Lei et al. [47] dispersed graphene nanomaterials and sodium dodecyl benzene sulfonate
152 (SDBS) in PCM (paraffin), which was then solidified in a rectangular chamber with a vertical
153 orientation. An electromagnetic field was applied with an electric-field intensity of 110 volts
154 and a magnetic induction intensity of 0.1 tesla. The authors found that graphene nanoparticles
155 were dispersed more uniformly throughout the solid region in the presence of electromagnetic
156 field. In another work, Laouer et al. [48] investigated the impact of magnetic field on the
157 melting process of copper-water (ice) as NEPCM inside a rectangular enclosure. The Lattice
158 Boltzmann Method was used in the formulation and resolution of the phase change process.
159 Figure 1 shows the duration of the melting process, which is significantly extended at higher
160 Hartmann number. Adding nanoparticles in the absence of magnetic field increased the liquid
161 fraction, while the opposite trend was observed in case of Hartmann number of 30 and 60. For
162 Hartmann number of 90, the increase in the nanofluid volume fraction improved the liquid
163 fraction. These observations are all valid at Rayleigh number of 10^5 . Note that the Rayleigh
164 number is associated with buoyancy-driven flow and effect of natural convection. It is defined
165 as the product of Grashof number and Prandtl number



166

167 Figure 1. Liquid fraction time evolutions for various Hartmann number (Ha) and nanofluid
168 volume fraction (ϕ) at Rayleigh number of 10^5 (Figure reproduced from [48])

169

170 In Figure 1, Fourier number is defined as the ratio of the product of thermal diffusivity and time to the
171 characteristic length scale. The Hartmann number (Ha) is also the ratio of electromagnetic force to the
172 viscous force.

173 3.2 Cylindrical geometry

174 Fan et al. [49] intensified the convective heat transfer through employing rotating magnetic
175 field to accelerate the melting performance of 1-dodecanol PCM. As a result, magnetic particles
176 scattered in liquid PCM and moved circumferentially inside the heat reservoir. Under rotational
177 speed of 20 rpm and 1.0 wt% particle fraction as well as heating temperature of 35°C, total
178 melting time shortened by 22.9%. The solid-liquid interface takes the shape of heating surface
179 when the forced convection is more severe. Focusing on non-uniform magnetic field, Farahani
180 et al. [50] evaluated the melting behavior of lauric acid with ferric oxide nanoparticles PCM in
181 a 3D cylindrical container with discrete and continuous innovative fin designs. Introducing
182 non-uniform magnetic field has increased the PCM liquid fraction by 63–72%. The melting
183 rate also intensified by 31.8% and 37.87% for spiral fins and continuous rectangular fins,
184 respectively, as a result of increasing the surface area available for heat transmission. In another
185 work by the same research group, Farahani et al. [51] focused on seven innovative fin
186 configurations to improve the melting performance of PCM in the presence of non-uniform
187 magnetic field. The results demonstrated that the melting fraction can be improved by 1.5–
188 2.5% as a result of increasing the NPVF from 2.5–5%. Further improvement in the melting rate
189 was observed by 16–57% increase in the magnetic field strength.

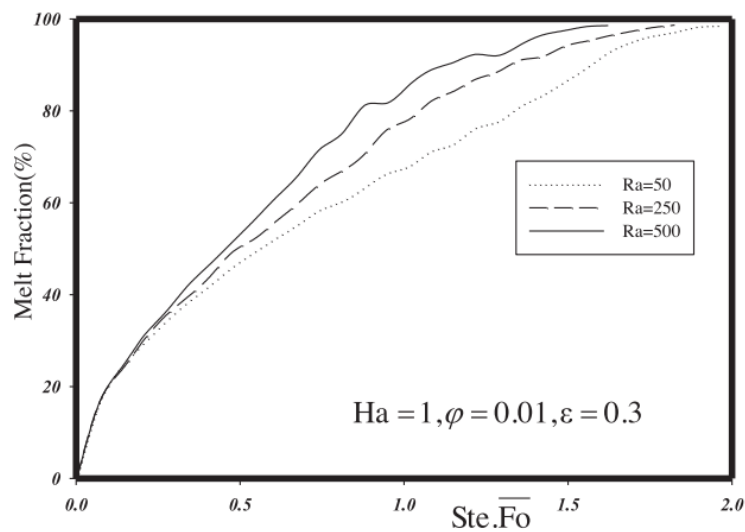
190 Saha [52] investigated the solidification and melting procedures of gallium in a semi-circular
191 cavity with a heated circumferential wall subjected to uniform magnetic domain and thermos-
192 capillary effects. A detailed parametric study was conducted over the magnetic field direction,
193 Hartmann number, Rayleigh number, Marangoni number, and gravity conditions. According
194 to this study, the angle of the magnetic field has an insignificant/marginal effect on the
195 solidification/melting of gallium. Under microgravity condition and in the absence of magnetic
196 field, the melting process has been improved by the thermos-capillary convection. The results
197 showed 7.6% reduction in the melting time under 0.05 g and 20.22 °C temperatures difference
198 between the phase change and hot wall. In the presence of magnetic field, the melting time has
199 been extended by 5.48% due to increasing the Hartmann number from 0 to 25 at the magnetic
200 angle of 45°.

201 Selimefendigil and Öztop [53] investigated the effect of perturbations, bifurcation, and
202 magnetic field on the phase change process of spherical shaped encapsulated paraffin wax PCM
203 inside a cylindrical enclosure. The authors varied the Reynolds number values between 250 to
204 500, Hartmann number between 0 to 15, the junction place between 0.1H₂ to 0.3H₂, and
205 nanoparticle concentration between 0.02% to 0.1%. When the Re number increases, the entire

206 phase transition time (t-PC) decreases by about 73% and 26% for bifurcating and flat channels,
207 respectively. At Hartmann number of 15, t-PC decreases by 20% in case of a flat channel, while
208 it increases by 146% in case of a bifurcating channel.

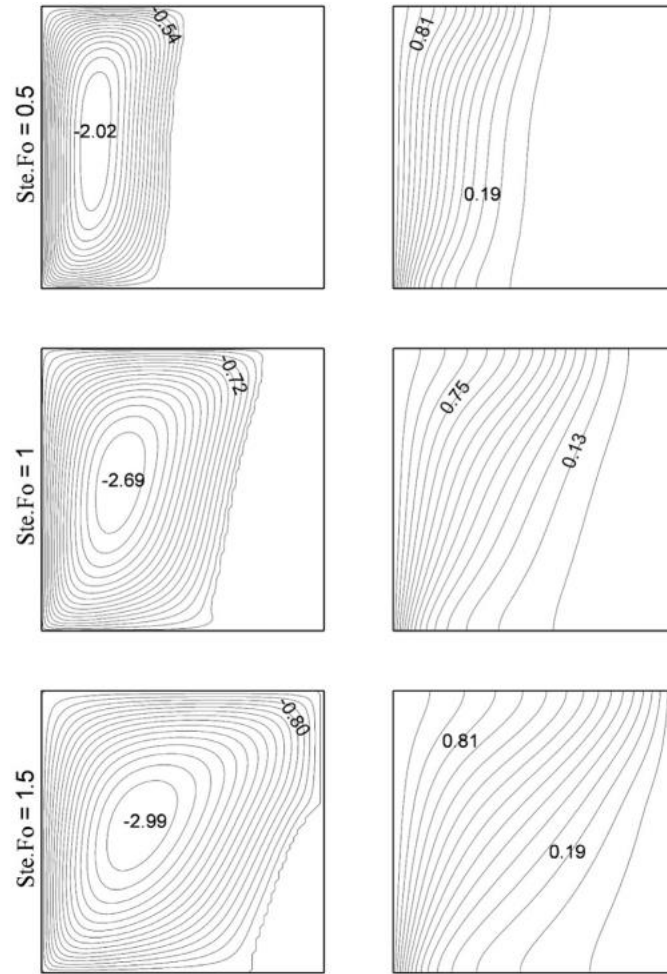
209 3.3 Square geometry

210 Kohyani et al. [54] investigated the effect of magnetic field on the melting of nano-PCM inside
211 a porous cavity. Changing the porosity of medium is a more dominant factor in the melting
212 process than varying the nanofluid volume fraction. They reported that a strong magnetic field
213 decreased the charging time and the predominance of conductive heat transfer inside the cavity.
214 Figure 2 shows the melting fraction as a function of $Ste.Fo$ for various Rayleigh numbers.
215 Increasing the Rayleigh number improved the melting rate due to an increase in the convective
216 heat transfer. Figure 3 shows the time history of isotherms and streamlines at constant Rayleigh
217 and Hartmann numbers, nano-PCM volume ratio and medium porosity parameters for three
218 values of $Ste.Fo$. The power of vortexes and the convection heat transfer increased with time
219 due to increasing the temperature difference between the up and bottom of the cavity.



220

221 Figure 2. Melt fraction as a function of $Ste.Fo$ for various Rayleigh numbers (Figure
222 reproduced from [54])



223

224 Figure 3. Streamlines (left) and isotherms (right) at fixed Rayleigh number of 100, Hartmann

225 number of 1, nano-PCM volume ratio of 0.01, and medium porosity of 0.3 (Figure

226

reproduced from [54])

227

228 Ghalambaz et al. [55] investigated the non-Newtonian behavior of a Ferro- and magneto-

229 hydrodynamic PCM during the melting process. They performed a detailed parametric study

230 over the Rayleigh number ($10^4 < Ra < 10^6$), the Hartman number ($0 < Ha < 250$), the Power-

231 law index ($0.7 < n < 1$), and the magnetic parameter ($0 < Mn_f < 7000$) on the normalized melt

232 volume fraction (NMVF), melting front, and the Nusselt number. Figure 4 shows the variation

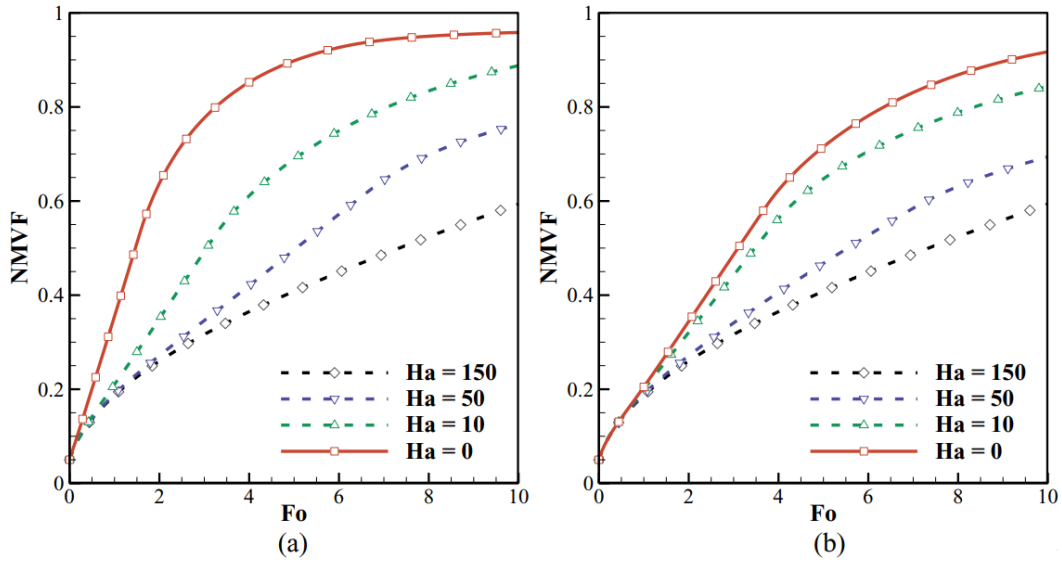
233 of NMVF with Hartman and magnetic parameters. An increase in the Hartman and magnetic

234 parameter decreased and increased the NMVF at different levels depending on the power-law

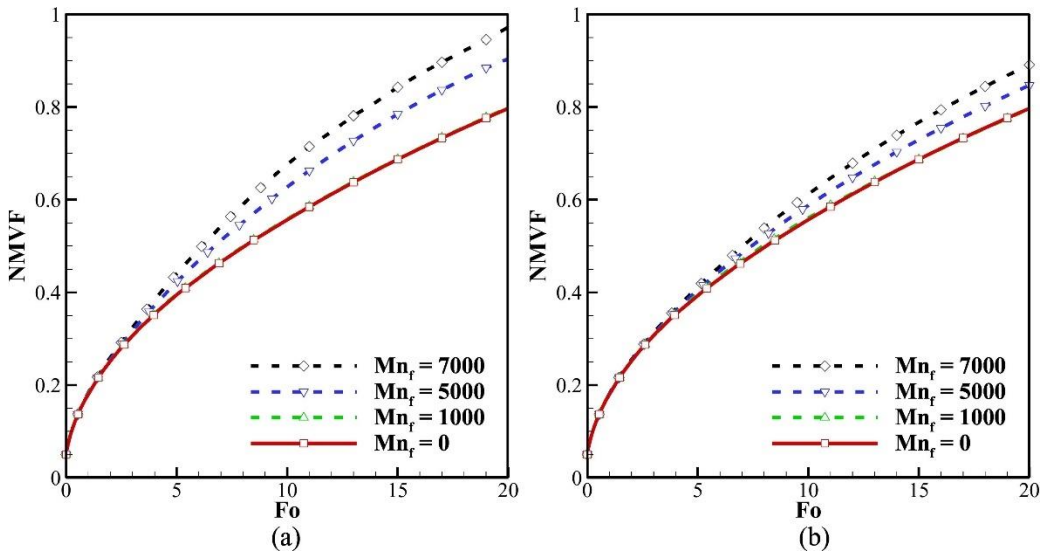
235 index. In the presence of magnetic field, the increase in power-law index worsened the NMVF

236 since the flow field is influenced by Lorentz force. Increasing the magnetic field parameter

237 decreases the melting time due to an increase in the convection heat transfer of the flow field.



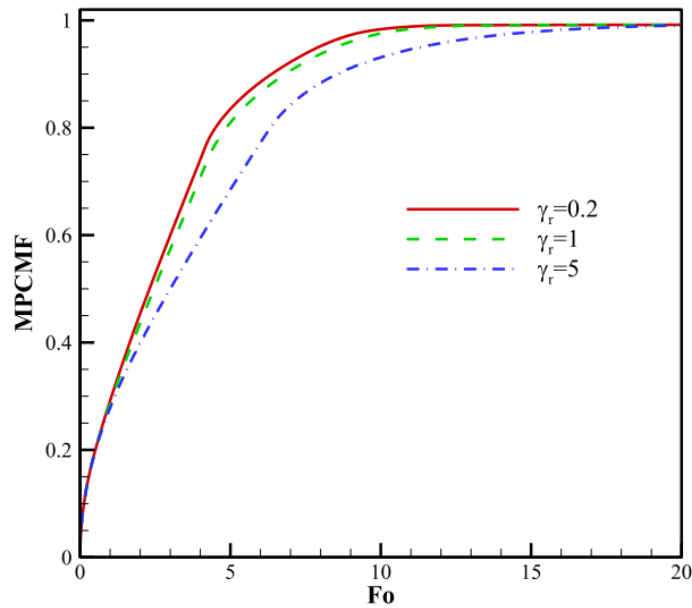
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239

240 Figure 4. Variation of NMVF with Hartman and magnetic parameters for power index of (a)
 241 0.7 and (b) 1 (Figure reproduced from [55])

242 Mehryan et al. [56] examined the impact of two magnetic sources with different strengths on
 243 the melting process of PCM inside a cavity. The authors used Galerkin FEM together with
 244 Lagrangian-Eulerian to solve the governing equations. The intensity ratio of these magnetic
 245 fields (γ_r) has significantly affected the melting front. Between the two parameters being
 246 magnetic and Hartman number, the latter has a more impact on the progress of the melting
 247 front. Figure 5 shows the melting fraction of PCM with Fourier number for different magnetic
 248 fields. As seen in this figure, the melting rate is consistent up to Fourier number of 1.5. Beyond
 249 this point there was a reduction in the melting fraction by increasing the magnetic field due to
 250 the increase in the flow vortices.

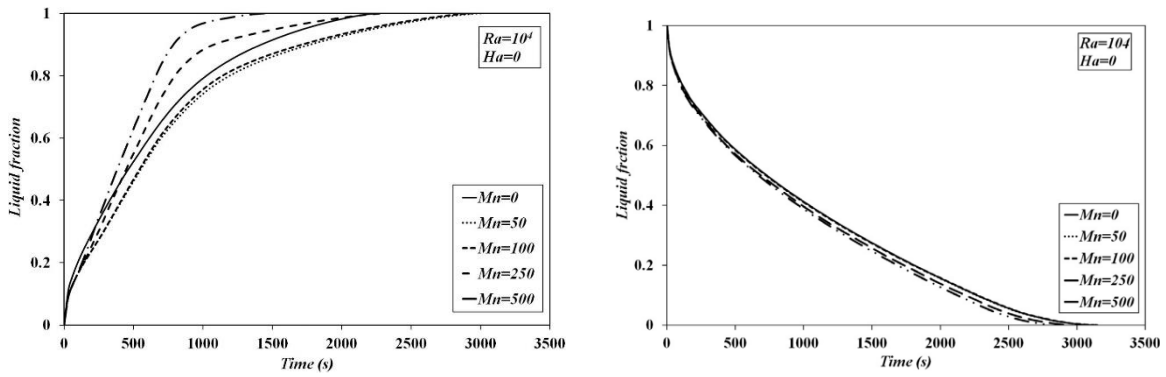


251
 252 Figure 5. Variation of the charging PCM fraction with Fourier number for different γ_r
 253 (Figure reproduced from [56])
 254

255 Kumar et al. [57] studied the melting of paraffin (PCM) with copper (Cu) nanoparticles in
 256 square cavity subjected to a constant external magnetic field in the horizontal direction. The
 257 free convection is suppressed when magnetic flux is employed in electrically conducting PCM.
 258 The energy storage capacity decreased by ~9% by increasing the Hartmann number from 0 to
 259 40. The maximum melting rate and energy storage capacity of NEPCM were found at 2% and
 260 0.5% nanoparticle concentration, respectively.

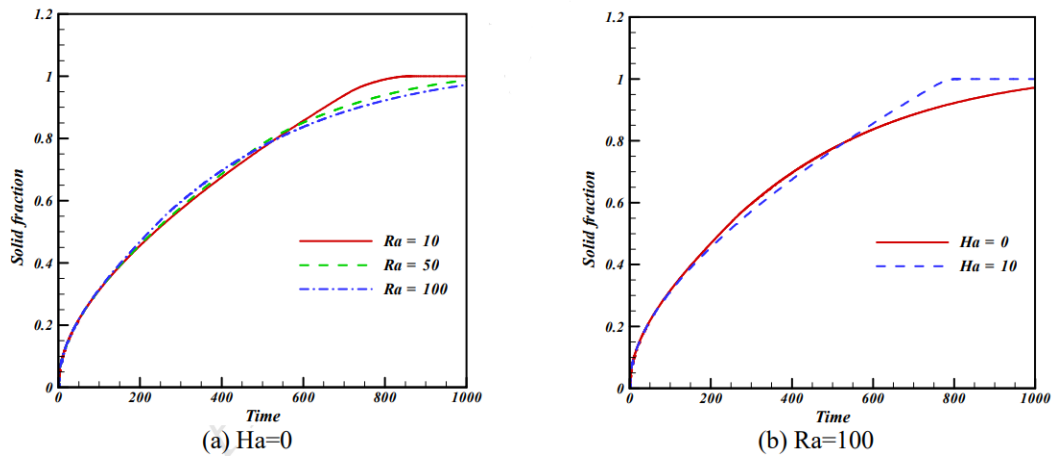
261 262 3.4 Annulus geometry

263 The influences of non-uniform magnetic fields on the charging and discharging of NEPCM in
 264 an annular domain were mathematically studied by Dibavar et al. [58]. A wire that carries an
 265 electrical current inside the annulus central point was used to create the magnetic field. Based
 266 on the results, the melting and solidification time reduced by 39.9% and 14.3% in the presence
 267 of magnetic field. Figure 6 shows the effect of magnetic field on the melting and solidification
 268 performance of ferrofluid in a non-electrical conductive field. From this figure, it is evident
 269 that the increase in the magnetic field had a more dominant effect on the charging than the
 270 discharging process at a constant Hartmann number and Rayleigh number. that an increase in
 271 the Hartmann number causes a significant reduction of the melting and solidification speeds.



272 Figure 6. Liquid fraction time evolution in the charging and discharging process of 5%
 273 volume fraction ferrofluid in a non-electrical conductive field at various strengths of a
 274 magnetic field (Figure reproduced from [58])

275 Sheikholeslami and Mahian [8] simulated the impact of magnetic field on the solidification
 276 rate of CuO nanoparticles PCM inside a porous energy storage device. They analysed the role
 277 of Lorentz forces, Rayleigh number, and nanofluid concentration on the solidification process
 278 of NEPCM. Figure 7 shows the solid fraction at different Rayleigh and Hartmann numbers at
 279 4% nanofluid concentration. The solidification time reduced by 23.5% when the Hartmann
 280 number increases from 0 to 10. Increasing the Rayleigh number from 0 to 100 reduced the
 281 solidification time by almost the same percentage. The addition of nanoparticle by 4% volume
 282 fraction into the PCM reduced the solidification time by 14%.



283 (a) $Ha=0$ (b) $Ra=100$
 284 Figure 7. Variation of solid fraction with time at 4% nanofluid concentration for various (a)
 285 Rayleigh and (b) Hartmann numbers (Figure reproduced from [8])

286 3.5 Other geometries

287 In the presence of a magnetic field, Sheikholeslami [59] used the finite element method (FEM)
 288 to model the discharging of NEPCM. The Darcy and Koo–Kleinstreuer–Li (KKL) models were

289 used to analyse nanofluid and porous media. The findings demonstrated that the growth in the
290 Hartmann number would decrease the solidification time.

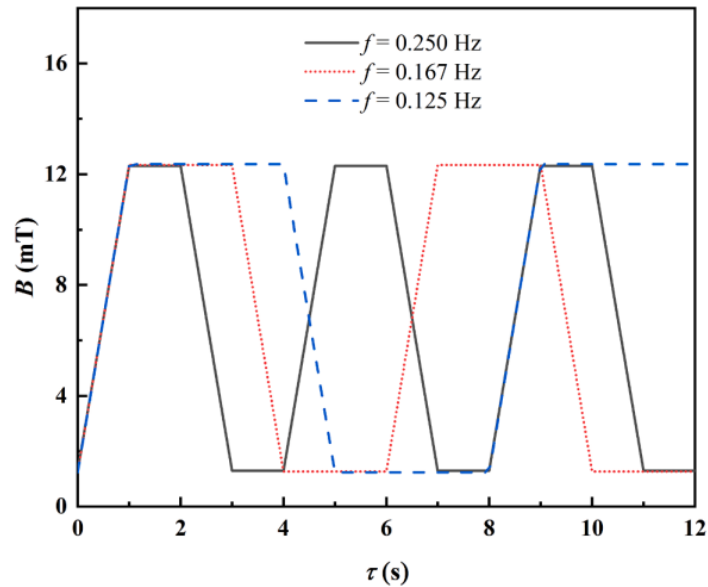
291 Ghalambaz et al. [60] studied the heat transfer and melting of electrically conductive phase
292 transition materials subjected to a magnetic field inside of a hollow domain. The sides of the
293 hollow were isothermal, while the higher and lower walls of the enclosure were adiabatic. The
294 hot wall temperature was greater than the fusion temperature of PCM, whereas the cold wall
295 temperature was less than or equal to fusion temperature. The role of magnetic field is more
296 pronounced by progressing with melting time. Changing the location of magnetic force from
297 bottom to middle of the cavity has a significant influence on reducing the non-dimensional
298 melting time by 13.5%.

299 Through a 3D transient numerical simulation, Shi et al. [61] evaluated the melting and
300 solidification performance of paraffin type A16 with Fe_3O_4 nanoparticles inside a shell and
301 multi-tube latent heat thermal energy storage. The complete melting and solidification time has
302 been decreased by 80.0% and 53.2%, respectively, through applying magnetic field with 50
303 mT intensity. The solidification time took longer than the melting time due to the formation of
304 a solidified layer on the outer surface of the tube, acting as an insulation layer between HTF
305 and PCM. The authors reported that the presence of magnetic field can decrease the difference
306 between the melting and solidification time, which is essential for a cyclic
307 melting/solidification processes.

308 Selimefendigil and Öztop [62] applied a uniform magnetic field in radial direction and field
309 with different magnitudes in various regions of the computational model to assess the melting
310 performance of PCM-filled vertical cylinder. Imposing the magnetic field has accelerated the
311 charging process and phase transition near the walls. Charging time can also be shortened by
312 40% and 14.5% with increasing the Hartmann number to 40 of the magnetic field in the PCM
313 domain and other domains, respectively. The authors developed a predictive modeling
314 approach to predict the melting time as a function of the magnetic field and volume fraction of
315 hybrid particles.

316 Applying a uniform magnetic field has a significant role in controlling the convective heat
317 transfer. Fan et al. [63] was the first who analysed the melting process of PCM under alternating
318 magnetic force. Intensified forced convection was induced in the liquid PCM as a result of
319 magnetic particles travelling between the solid-liquid interface and heating surface under
320 alternating magnetic force (see Figure 4). The suggested method reduced the PCM melting
321 time by 15.8% when the heating surface temperature was set at 55 °C. The maximum increment

322 of the overall heat transfer coefficient between the heating surface and the solid-liquid interface
323 was 25.4%.



324
325 Figure 8. Induction intensity of magnetic field in the center of heating surface (Figure
326 reproduced from [63])
327

328 The enthalpy porosity method was intensively used by several scholars to model solid-liquid
329 phase change process. However, He et al. [64] switched to thermo-magnetic convection model
330 to analyse the solidification behavior of paraffin wax PCM with Fe_3O_4 nanoparticles under a
331 uniform magnetic field. Depending on the magnetic field direction, the solidification process
332 was either enhanced or deteriorated. The amount of energy released and the solid fraction were
333 decreased and increased by 4.6% and 3.9%, and by 29.2% and 19.2%, under positive or
334 negative fields, respectively, due to the different nanoparticles motion pattern dominated by
335 Kelvin force.

336 Aly et al. [65] studied the effects of thermal energy on Magnetohydrodynamic (MHD)
337 thermosolutal convection of NEPCMs suspended in a horizontal wavy porous cavity with
338 embedded high-temperature crescents. Incompressible Soft Particle Hydrodynamics (ISPH)
339 was employed to solve the governing equations. The increase in time-fractional derivative,
340 Hartmann number, and solid size reduced the NEPCM motions. An increase in time-fractional
341 derivative from 0.95 to 1 slowed down the speed of nanofluid by 26.3%.

342 4. Effect of rotation

343 Storage rotation is identified as an active heat enhancement approach to accelerate the charging
344 and discharging performance of PCMs/NPCMs. This can be achieved through the use of
345 flexible pipes and couplings, which enables the rotation of storage medium in less than one
346 circle. Table 2 lists the geometrical, operating conditions, and key take-away findings of recent
347 studies addressing the role rotation on the melting/solidification procedures of PCMs/NEPCMs
348 inside an enclosure with different geometries. The citation list [66–73] focuses on this
349 importance in different geometries as summarized in the following subsections.

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Table 2. A summary of studies on the effect of rotation on the melting/solidification procedures of PCMs/NEPCMs inside an enclosure with different geometries

Authors (year)	Configuration	Type of study	Studied parameters	Highlighted results/findings
Khosroshahi and Hossainpour (2021) [66]	PCM filled in the annulus of a 2D double-pipe LHTES	Numerical	Effect of TES rotational speed and rotation scenario on the melting process	Reduced melting time by 3.45% under constant rotational speed compared to fixed operation. Maximum 15.5% reduction in the melting time through applying two opposite rotations considering 180° difference between the stop ends.
Kosroshahi and Hossainpour (2022) [67]	2D double-pipe with paraffin PCM in the annulus	Numerical	Effect of straight fins and TES rotation in 7 combinations on the melting process	Reduced melting time by 18.5% and 70% through employing TES rotation and fins. Optimal 72% decrease in the melting time by simultaneous use of both techniques.
Fathi and Mussa (2021) [68]	Paraffin wax PCM in a horizontal shell-and-tube LHTES	Experimental	Effect of rotational speed on the melting process	Marginal enhancement in the melting process under 9 rpm rotational speed, experimental limit of the rotation. Understanding the trade-off between moving to higher rotational speed and energy implications as the future work.
Soltani et al. (2021) [69]	N-eicosane PCM in a 2D cylinder enclosure containing fins	Numerical	Effect of adding fins in the inner cylinder and rotational speed of the HTF tube on the melting and solidification processes	Reduction in the solidification time by 83.21% through employing tube rotation mechanism. 12.89 W heat transfer rate at 1 rpm rotational speed. Improvement in the heat transfer ratio by 3.87 and 2.45 times in the solidification and melting processes, respectively.
Modi et al. (2022) [70]	Paraffin PCM in a 3D shell-and-tube LHTES	Numerical	Effect of intermittent rotation on the melting and solidification processes	Improved melting by 64–74% through employing bottom eccentricity of 0.6–0.75. Optimal top eccentricity between -0.15 and -0.3 for the discharging process 0.3 as the optimal eccentricity for both the charging and discharging processes.
Yang et al. (2022) [71]	PCM filled into a shell-and-tube LHTES considering heat conduction over the external shell	Experimental	Effect of different rotation mode including rotate, static, and flip on the melting process	Increase and then decrease in the melting time through the flipping time— with the optimal flipping time of 0.375. Shorten melting time by 35.42% accompanied by increase in the TES rate by 54.5%. Better melting performance under rotation mode, 19.35% reduction compared to the optimum flipping condition.
Farsani et al. (2020) [72]	Paraffin wax PCM in a rectangular cavity container	Numerical	Effect of Taylor number and Rayleigh number on the melting process	Rotating cavity in a counter direction of buoyancy flow improved the melting rate by 8%.
Alhashash and Saleh (2022) [73]	Free convection in a square enclosure filled with NEPCM subjected to counterclockwise rotation in the longitudinal direction	Numerical	Effect of rotational speed and NEPCM volume fraction on the melting process	Enhancement in the heat transfer rate by declining the Taylor number and rising the Stefan number. Less phase change and delayed heat transfer under higher rotational speed.

370 *4.1 Annulus geometry*

371 Khosroshahi and Hossainpour [66] developed a double-pipe LHTES unit with a PCM-filled
372 annulus and a storage rotation mechanism to accelerate the charging of PCMs. Constant-speed
373 and stepwise rotations were examined. The results revealed that storage rotating with a constant
374 rotation rate had a low impact on the required time of melting. However, using a step-by-step
375 rotation scenario reduced the charging time by 15.5% compared to the fixed mode. In another
376 study by the same research group, the authors established a two-dimensional model to
377 investigate the feasibility of a new simultaneous utilisation of storage rotation and longitudinal
378 fins techniques to decrease the melting rate and increase the amount of energy stored in a
379 double-channel heat exchanger [67]. Following a detailed analysis of several scenarios, the
380 authors found that embedding the fin on the bottom half of the fixed storage was a more
381 effective pathway to speed up the melting process. The melting time reduced by 72% through
382 employing both heat transfer enhancement techniques.

383

384 *4.2 Shell-and-tube and cylindrical geometries*

385 Fathi and Mussa [68] conducted a specific study to determine how the rotation of the tube can
386 affect the productivity of the LHTES. While water served as the HTF, paraffin (C_nH_{2n+2}) was
387 employed as the PCM in this experiment. The trials were carried out at three different rotational
388 speeds (i.e., 3, 6, and 9 revolutions per minute (rpm)). The findings were compared against
389 those obtained from the stationary case. Rotating the tube at the above-mentioned range of
390 speeds increased the percentage of the liquid fraction by 8.12% after about 11 hours of
391 simulation. Using enthalpy porosity method, Soltani et al. [69] simulated the effects of fins and
392 rotation on the solidification and melting of PCM. Figure 9 shows the effect of rotational speed
393 on the liquid fraction of PCM. It is observed that solidification time greatly reduced, by 83.2%,
394 at higher rotational speed. From this analysis, the authors reported that there was direct
395 relationship between the rotational speed and heat transmission from and to PCM—leading to
396 a maximum heat transfer ratio enhancement by 3.9 and 2.5 times during discharging and
397 charging processes.

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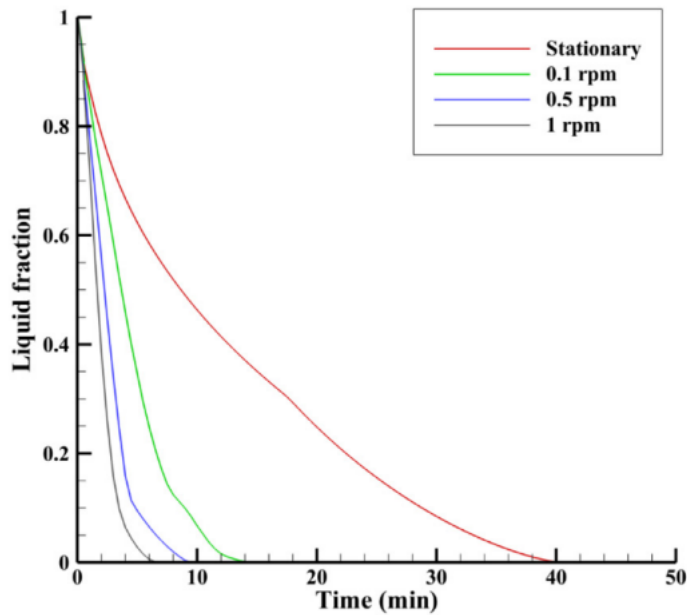


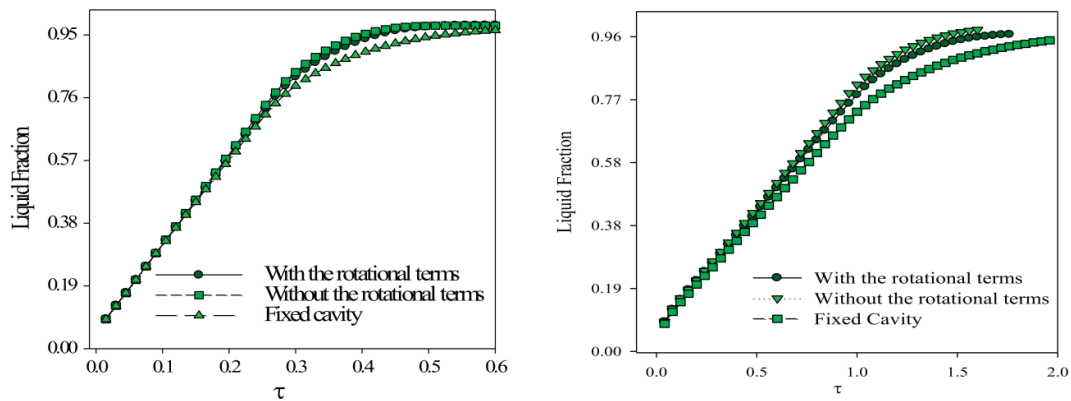
Figure 9. Liquid fraction time evolution in the discharging process of PCM at various rotational speeds (Figure reproduced from [69])

Modi et al. [70] studied the effect of eccentric inner HTF tube placements on a shell-and-tube LHTES system during solidification and melting. Intermittent LHTES unit rotation was suggested to effectively boost both the solidification and melting processes. Bottom eccentricity helped the melting process but hindered solidification. The unique rotating approach efficiently fitted bottom eccentricity to increase melting while top eccentricity to improve solidification. In the continuation of this work, a visual experimental examination was carried out by Yang et al. [71] to naturally assess the establishment impact of several rotation methods (static, rotate, and flip) and enhance the flipping duration with low extra energy consumption. The temperature distribution and phase interface location were explored under a variety of rotating settings and at a range of various input temperatures while considering the conductivity of the outer shell. The findings indicated that the charging time of LHTESU first increased and then decreased with the rise of the flipping period. When the dimensionless flipping time was equal to 0.375, the melting performance was at its highest possible level.

4.3 Rectangular and Square geometries

Farsani et al. [72] numerically examined PCM charging in a tracking solar panel cavity. The cavity was filled with paraffin and rotated steadily. Melting and heat transmission were

420 influenced by buoyancy-driven flow and rotational parameters. When rotation occurred
 421 contrary to buoyancy-driven flow in molten fluid, heat transmission and melting rate increased
 422 by up to 8%. Figure 10 shows the liquid fraction time evolution in the charging process for
 423 cases with/without Coriolis force and rotational buoyancies at two Rayleigh numbers. The
 424 results showed that the melting rate increased by about 2% through employing rotational
 425 buoyancies and Coriolis force.



426

427 Figure 10. Liquid fraction time evolution in the charging process for the cases with/without
 428 Coriolis force and rotational buoyancies for Rayleigh number of 2.72×10^6 (left) and 5.74×10^5
 429 (right) (Figure reproduced from [72])

430

431 Alhashash and Saleh [73] investigated the possibility of a thermal natural convective in hybrid
 432 nanofluids contained in a square container. The angular velocity of the enclosure was
 433 maintained at a constant counterclockwise direction. The results indicated that by raising the
 434 rotational speed, the amount of NEPCM undergoing phase change reduces—which slowed
 435 down the heat transmission. The authors also found that higher Stefan number and lower Taylor
 436 number leads to higher heat transfer rates.

437 5. Effect of tilt angle

438 During the procedure of melting PCM in a variety of configurations, there have been many
 439 practical and numerical investigations that have shown that buoyancy-driven convective heat
 440 transfer and orientation of the enclosure play an important role on the melting and solidification
 441 processes. A few studies have looked at the possibility that tilting the enclosure might change
 442 the form of the convection currents and, as a result, the PCM charging process [71]. Table 3
 443 lists the geometrical, operating conditions, and key take-away findings of recent studies
 444 addressing the role tilt angle on the melting/solidification procedures of PCMs/NEPCMs inside

445 an enclosure with different geometries. The citation list [74 – 90] focuses on this importance
446 in different geometries as summarized in the following subsections.

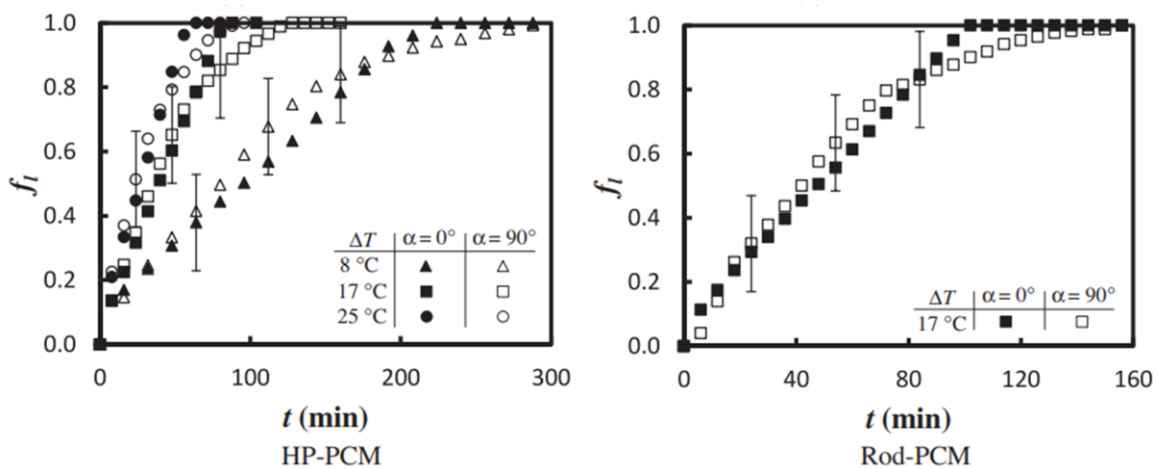
Table 3. A summary of studies on the effect of tilt angle on the melting/solidification procedures of PCMs/NEPCMs of an enclosure with different geometries

Authors (year)	Configuration	Type of study	Studied parameters	Highlighted results/findings
Sharifi et al. (2013) [74]	PCM positioned concentrically inside a 3D vertical cylindrical container with outward melting	Experimental and numerical	Effect of tilting angle on the melting process	Strong effect of 3D geometry at the tilting angle of 5°. Substantial impact of inclination angle on the local temperature of the PCD.
Allen et al. (2014) [75]	PCM/NEPCM contained in a cylindrical enclosure with heat transfer occurring through a solid copper rod or a heat pipe (HP)—the latter is combined with foam and aluminum foils	Experimental	Effect of inclination angle and different configurations—including HP-Foam-PCM, HP-Foil-PCM, HP-PCM, Foam-PCM, Rod-PCM, and NEPCM—on the melting and solidification processes	Higher liquid fraction for Rod-PCM and HP-PCM in a horizontal orientation. Marginal improvement in the liquid fraction for HP-Foam-PCM and HP-Foil-PCM in a vertical orientation. Reduced melting and solidification time by 11% and 3% in case of HP-Foil-PCM compared to NEPCM irrespective to orientation.
Siyabi et al. (2019) [76]	Paraffin PCM inside a 2D cylindrical heat exchanger storage system	Experimental and numerical	Effect of tilting angle on the melting process	Reduction in the temperature difference as a result of an increase in the inclination angle. Faster melting in the inclination angle of 45°, 13% lower than 0° angle. Shorter PCM melting time when the movement of liquid PCM is in the same direction to that of buoyant force.
Zennouhi et al. (2016) [77]	Galium PCM inside in a 2D rectangular cavity	Numerical	Effect of tilting angle on the heat transfer and fluid flow structure during the melting process	Enhancement in the melting rate by reducing the title angle from 90° to 0°. Formation of Bénard convection cells in the liquid region of the solid-liquid interfaces.
Joneidi et al. (2017) [78]	RT35 PCM inside two designated holes at the right and top side of a rectangular enclosure	Experimental	Effect of tilting angle and heat flux of the heater on the melting process	Reduction in the melting time by increasing the heat flux. Increase in the angle of the heater was accompanied by increase in the melting time and the amount of energy stored in TES.
Kamkari and Groulx (2018) [79]	Lauric acid PCM in a finned rectangular side-heated enclosure	Experimental	Effect of tilting angle and number of fins on the melting process	Higher melting rate at lower inclination angle for both finned and un-finned cases. Minimum melting time in case of a horizontal enclosure with 3 fins. Orientation as a more influential factor than adding fins in terms of enhancing the heat transfer rate and shortening the charging time.
Abdulmunem et al. (2020) [80]	Paraffin PCM contained in a rectangular container	Experimental and numerical	Effect of tilting angle on the melting time	Prolonged melting process at lower inclination angle. Minimum melting time of 108 minutes at 90° tilt angle.
Abdulmunem et al. (2021) [81]	PCM as heat sink in the backside of a rectangular PV cell	Experimental and numerical	Effect of tilting angle on the melting process and PV cell temperature	Acceleration in the melting process by increase in an inclination angle. 12% decrease in the PV cell temperature at an inclination angle of 90°.
Kousha et al. (2016) [82]	Paraffin PCM in a shell-and-tube heat exchanger	Experimental	Effect of Stefan number, Reynolds number, inclination angle, and	More melting rate within the first half of the domain in the horizontal than the inclined orientations.

			Grashof number on the melting and solidification processes	Higher heat transfer rate in the vertical orientation during the discharging process. Insignificant influence of angle change on the solidification performance.
Shen et al. (2019) [83]	RT60 PCM in a vertical shell-and-tube heat exchanger	Numerical	Effect of tilting the lateral surface angle and Reynolds number on the melting and solidification processes	Improved/worsened the melting/solidification by increase in the tilting lateral surface angle. Reduction in the melting time by 45% at 7° compared to 0° tilting angle 4° as the optimal angle to reduce the melting and solidification time by 22% and 8.5%.
Avci and Yazici (2018) [84]	N-eicosane PCM in a flat heat sink exposed to a constant heat flux	Experimental	Effect of tilting angle on the thermal performance of the melting process	Significant effect of tilting effect on the thermal performance of a heat sink with PCM compared to a case without PCM. 5.5 times higher operating time for a heat sink with 90° tilting angle compared to 0° angle.
Karami and Kamkari (2018) [85]	Dodecanoic acid PCM placed inside a finned enclosure	Numerical	Effect of tilting angle and number of fins on the melting and solidification processes	Shortened melting time at lower inclination angle due to improvement in the natural convection. Maximum melting time reduction of 72% in case of 0° angle with 3 fins. Intensified heat content by decrease in the number of fins and increase in the tilting angle.
Ghalambaz et al. (2020) [86]	Non-Newtonian n-octadecane PCM with a mesoporous silica particles inside a 2D inclined container	Numerical	Effect of nanoparticle mass fraction and inclination angle on the melting process	Decrease in the latent heat capacity due to the presence of nanoparticles. Up to 50% reduction in the heat transfer at 5% nanoparticle mass fraction 80% reduction in the heat transfer at -75° tilting angle.
Sorour et al. (2021) [87]	PCM placed in the annulus of a double-pipe heat exchanger	Experimental and numerical	Effect of tilting angle on the melting process of the PCM with various thicknesses	Optimum inclination angle of 45° for the PCM with 14.5 mm thickness, leading to 18% reduction in the melting time. Horizontal orientation resulting in the least charging time for PCMs with small thickness.
Kothari et al. (2021) [88]	Paraffin PCM in a heat sink with/without plate fins	Experimental	Effect of tilting angle and heat flux on the melting process	Prolonged operating time at lower inclination angle both finned and un-finned cases. 44% and 30% decrease in the melting time through reducing the angle from 90° to 0° for un-finned and finned cases.
Yang et al. (2021) [89]	PCM embedded in metal foam inside a cavity with different aspect ratio	Experimental and numerical	Effect of tilting angle and cavity aspect ratio on the melting process	Negligible impact of inclination angle on the melting time/rate at a given aspect ratio. Higher temperature uniformity at a smaller aspect ratio, ~5 times greater in aspect ratio of 0.1 compared to 8.
Wang et al. (2022) [90]	Lauric acid as the PCM in a micro-heat pipe array LHTES unit	Experimental	Effect of tilting angle on the coupled heat transfer between PCM and heat pipe and eventually on the melting process	Decrease in the tilting angle from 90° to 15° was associated with 15.5% heat transfer enhancement and 1.9% increase in the melting time. First decrease and then increase in the heat pipe effective thermal conductivity under a tilting angle ranging from 30° to 90°. Deterioration in the heat transfer under heat flux greater than 30 W and tilting angle lower than 30°.

450 5.1 Cylindrical geometry

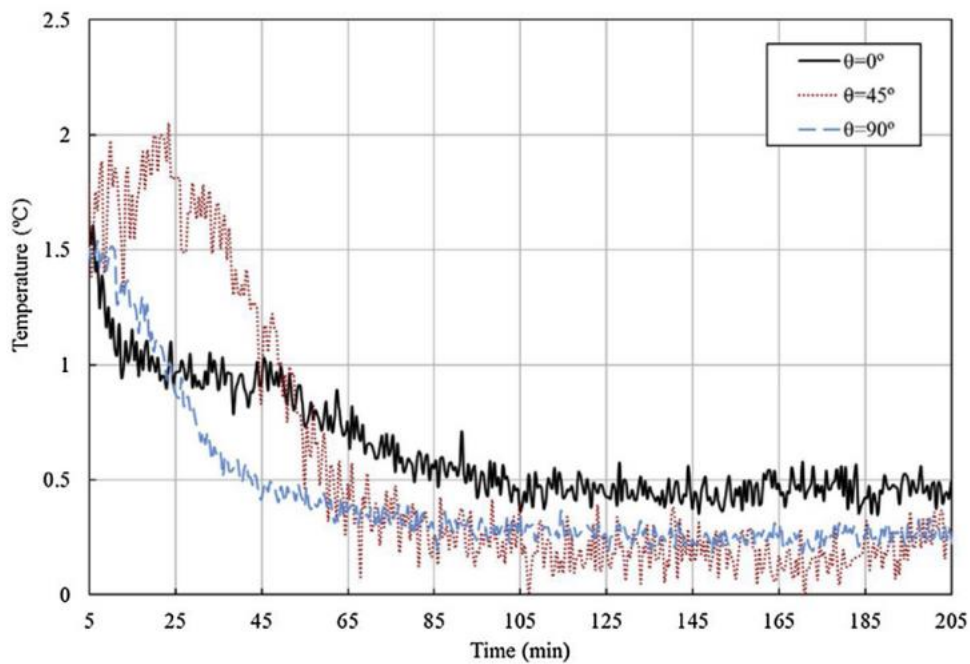
451 In an experimental study by Sharifi et al. [74], the authors focused on the effect of tilting angle
 452 on outward charging of a PCM as a result of a heated rod positioned inside a cylindrical
 453 enclosure. They also developed a two-dimensional model of the geometry for predicting the
 454 melting process for the non-tilted case. The results showed that a little tilting of the test cell
 455 had an extensive impact on the local temperature distribution inside the PCM. This was due to
 456 the three-dimensional nature of the experiments, which required a three-dimensional model to
 457 better capture the PCM melting. Allen et al. [75] experimentally tested the influence of tilt
 458 angle on PCM melting and solidification. Heat transfer occurred through a concentrically
 459 located heat pipe (HP) or solid copper rod and an underlying copper disc. Six configurations
 460 were investigated: HP-Foil-PCM, HP-Foam-PCM, HP-PCM, Rod-PCM, Foam-PCM and non-
 461 enhanced PCM. Due to conduction being the major mechanism of heat transport, experimental
 462 data showed that unit direction had a small influence on discharging rates in all cases. For the
 463 charging, the orientation of the enclosure had a higher effect due to higher impact of natural
 464 convection. Figure 11 shows the effect of ΔT and enclosure orientation on the liquid fraction
 465 during the melting process. It should also be noted that the orientation of the container has a
 466 significant impact on the charging process. Moreover, the effect of orientation is lower at
 467 higher ΔT . The authors concluded that the charging process is more influenced by the tilting
 468 angle than the discharging process.



469
 470 Figure 11. Effect of ΔT and container orientation on the liquid distribution during the
 471 charging process for HP-PCM and Rod-PCM cases (Figure reproduced from [75])
 472

473 Siyabi et al. [76] used experimental and computational methods to study the Paraffin wax PCM
 474 melting under various tilting angles. PCM melting behavior within the storage was defined by

475 the distribution of temperature, melting profiles imaging, thermal stored rate, and liquid stream
 476 of PCM. The PCM storage inclination angle affects temperature profile, charging period, and
 477 profile. The melting process is faster in the axial than radial direction in the 0° , while opposite
 478 trend was observed in 90° . Figure 12 shows that PCM stored at 45° from the horizontal had a
 479 higher melting rate compared to that of 0° and 90° because the melting behavior exhibited a
 480 similar rate in both directions. The results of numerical simulations indicate that the direction
 481 of buoyant force resulting from the melted liquid PCM had a major role in both melting rate
 482 and melting direction within the PCM storage.

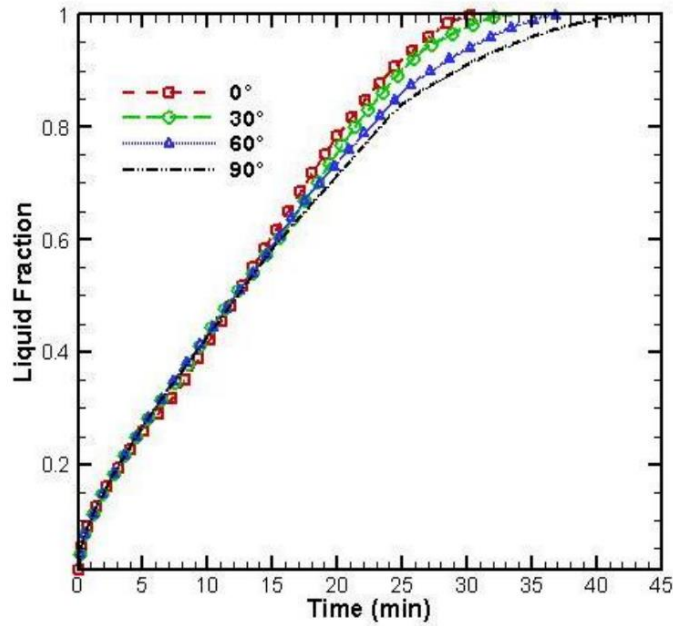


483
 484 Figure 12. Variation of HTF temperature with time for various tilting angles of PCM storage
 485 (Figure reproduced from [76])

486 5.2 Rectangular geometry

487 Zennouhi et al. [77] conducted a numerical simulation to assess the melting behavior of Galium
 488 PCM in a rectangular cavity under different tilting angles. Natural convection related to phase
 489 change was solved utilising a shapeless mesh, finite-volume approach, and enthalpy porosity
 490 methodology. Figure 13 shows the liquid fraction time evolution of PCM with respect to
 491 various tilting angles. As seen in this figure, the charging rate and, as a result, the liquid fraction
 492 increases by reducing the inclination angle. This is mainly due to the natural convection regime,
 493 which prevents the development of melting process at higher inclination angles. Bénard
 494 convection cells are generated in the liquid phase by carefully evaluating the solid-liquid
 495 interfaces.

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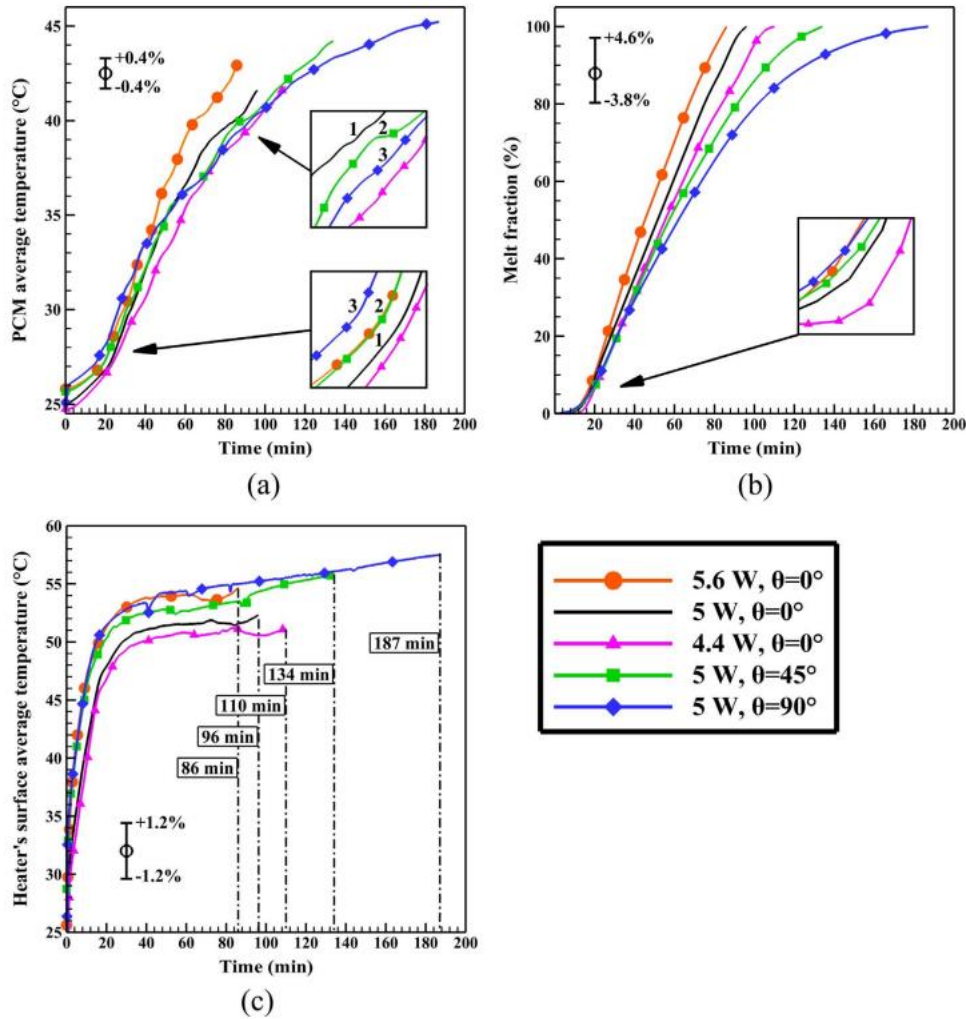
497

498 Figure 13. Liquid fraction time evolution in the charging process of PCM for various tilting
 499 angles (Figure reproduced from [77])

500

501 Joneidi et al. [78] studied the effect of heating power and inclination angle (i.e. 0, 45, 90°) on
 502 the melting time of RT35 PCM in a rectangular cavity. The domain was heated through the
 503 lower plate. Canon G9 camera used to capture the changes in the liquid-solid interface. Figure
 504 14 shows the mean average temperature of PCM, melt fraction, and average temperature of
 505 heater surface under various heating power and tilting angles. It is evident that increasing the
 506 heating power reduces the melting time and increases the mean average temperature of heating
 507 surface and PCM. Switching to higher inclination angles resulted in the accumulation of energy
 508 at the top of the rectangular cavity, which in turn increased the melting time and mean
 509 temperature of both heating surface and PCM. They concluded that the minimum melting time
 510 was achieved in an enclosure with a horizontal orientation.

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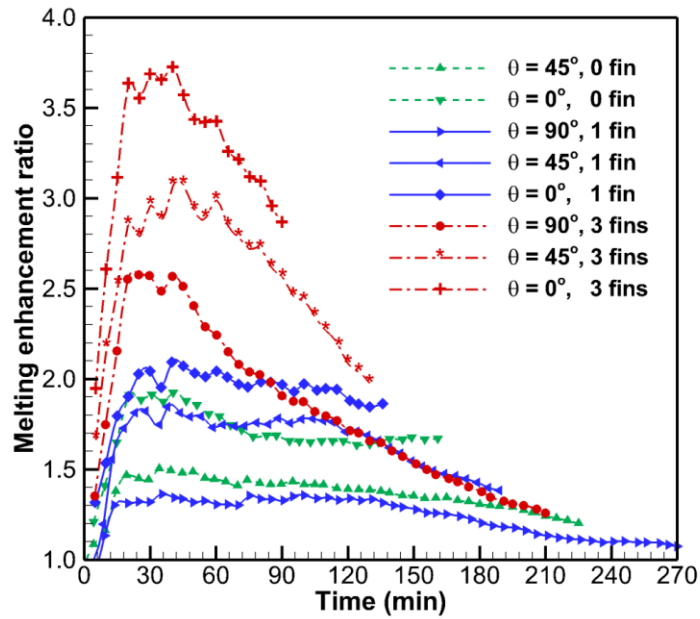


512

513 Figure 14. Mean average temperature of PCM, melt fraction, and average temperature of
 514 heater surface under various heating power and tilting angles (Figure reproduced from [78])

515 Kamkari and Groulx [79] studied the effect of adding fins together with inclination angles on
 516 the melting behavior of PCM in a rectangular enclosure. In this study, lauric acid melting in
 517 side-heated containers with variable numbers of fins was tested at 90°, 45°, and 0° inclination
 518 angles. The solid-liquid interface evolution showed higher melting rates at lower inclination
 519 angles for both finned and un-finned cases. Figure 15 shows the melting enhancement ratios as
 520 a function of time for different inclination angles and number of fins. In all the cases, there is
 521 a sharp increment in this ratio within the first few minutes of the melting process—stronger in
 522 the case of inclined enclosures with fin—attributed to vortical flow structures in the
 523 conduction-to-convection transition. This is followed by a reduction in this ratio after ~40
 524 minutes—more pronounced in the finned cases—as a result of higher thickness of the PCM
 525 liquid layer that impeded the convection flow inside PCM. The results corroborated the
 526 findings of other researchers regarding better melting rate at reduced inclination angle even in

527 case of finned configurations. Among the cases analysed, the maximum melting enhancement
 528 ratios of 3.7 was achieved in the 3-fin configuration—equivalent to 115% improvement in the
 529 heat transmission.

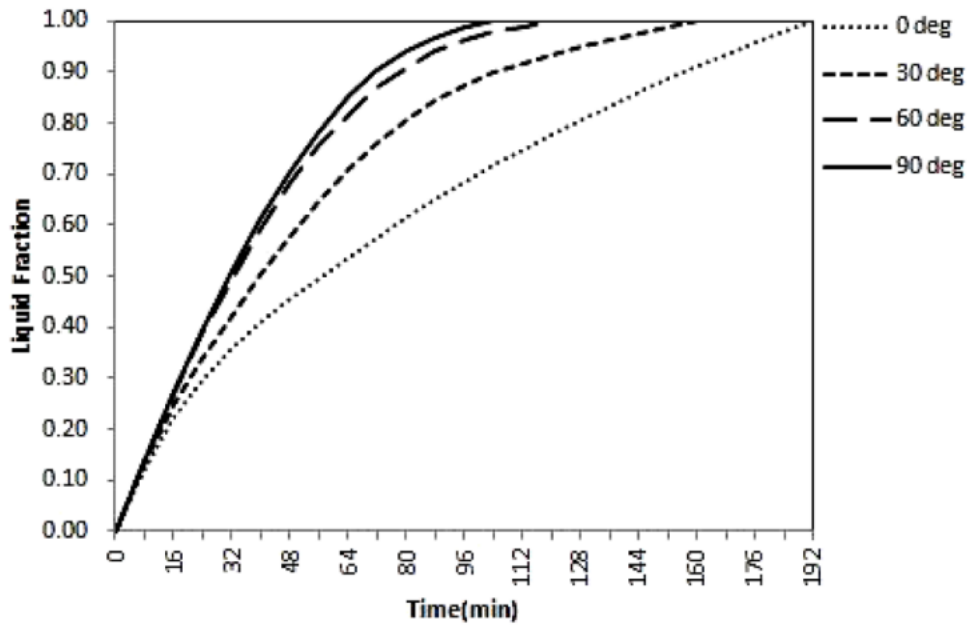


530

531 Figure 15. Melting enhancement ratios as a function of time for different inclination angles
 532 and number of fins (Figure reproduced from [79])

533 In the same line of thinking, Abdulmunem et al. [80] conducted experiments and numerical
 534 simulations to evaluate the paraffin wax PCM melting process as a passive cooling in a
 535 rectangular enclosure under different tilting angles (i.e. 0, 30, 60, and 90°). The geometry under
 536 consideration was subjected to 1000 sun simulator to maintain the temperature of an aluminum
 537 plate at 373 K. Figure 16 shows the liquid fraction time evolution in PCM charging process
 538 under various tilting angles. As seen in this figure, on contrary to other studies in the literature,
 539 the authors found that the melting time increased by lowering the tilting angle from 90° to 0°.
 540 They attributed this to lower convection heat transfer at lower inclination angle. In general, a
 541 shorter amount of time was needed for the PCM to completely melt, which indicates a more
 542 effective cooling performance. In another study, the authors focused on the charging
 543 performance of a PCM-based heat sink behind a rectangular domain of PV cells [81].
 544 According to this analysis, the authors achieved 0.4% to 12% reduction in the PV cell
 545 temperature as a result of changing the tilting angle from 0° to 90° (see Figure 17). However,
 546 the authors did not assess the energy, exergy, and electrical efficiency of PV-PCM under
 547 different inclination angles.

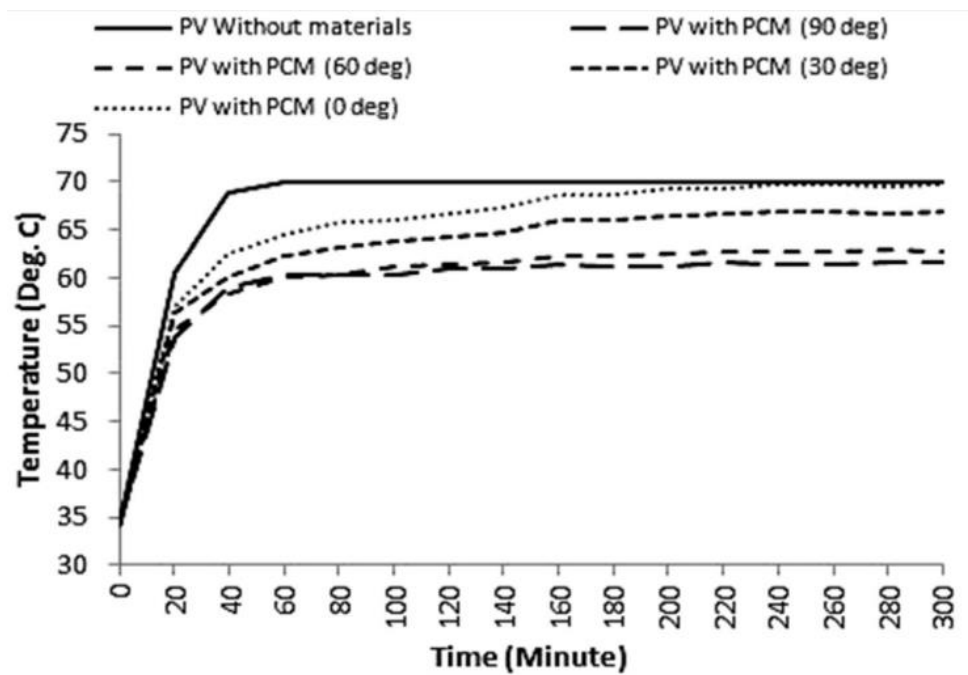
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549

550 Figure 16. Liquid fraction time evolution in the charging process of PCM for various tilting
 551 angles (Figure reproduced from [80])

552



553

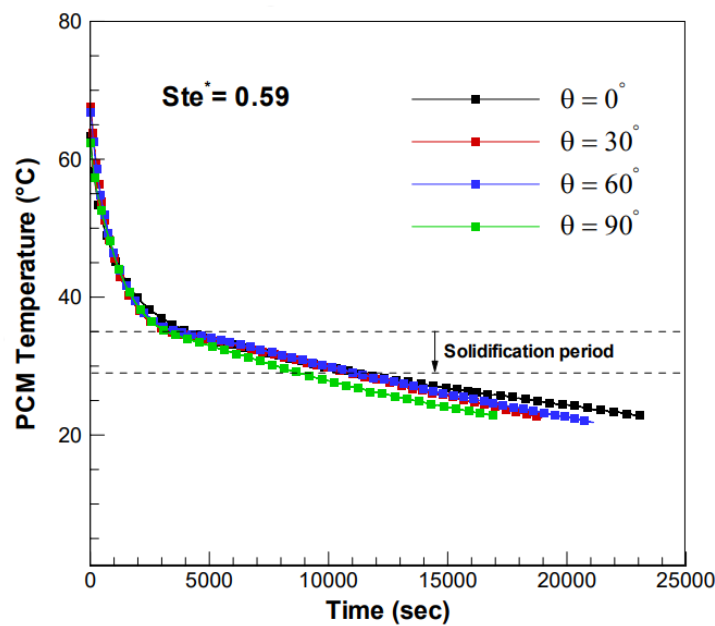
554 Figure 17. Variation of PV cell temperature with time for various tilting angles (Figure
 555 reproduced from [81])

556

557 *5.3 Shell-and-tube heat exchanger*

558 Kousha et al. [82] studies the melting and solidification performance of Paraffin RT35 PCM in
 559 a shell-and-tube heat exchanger under various inclination angles in the laminar flow regime.

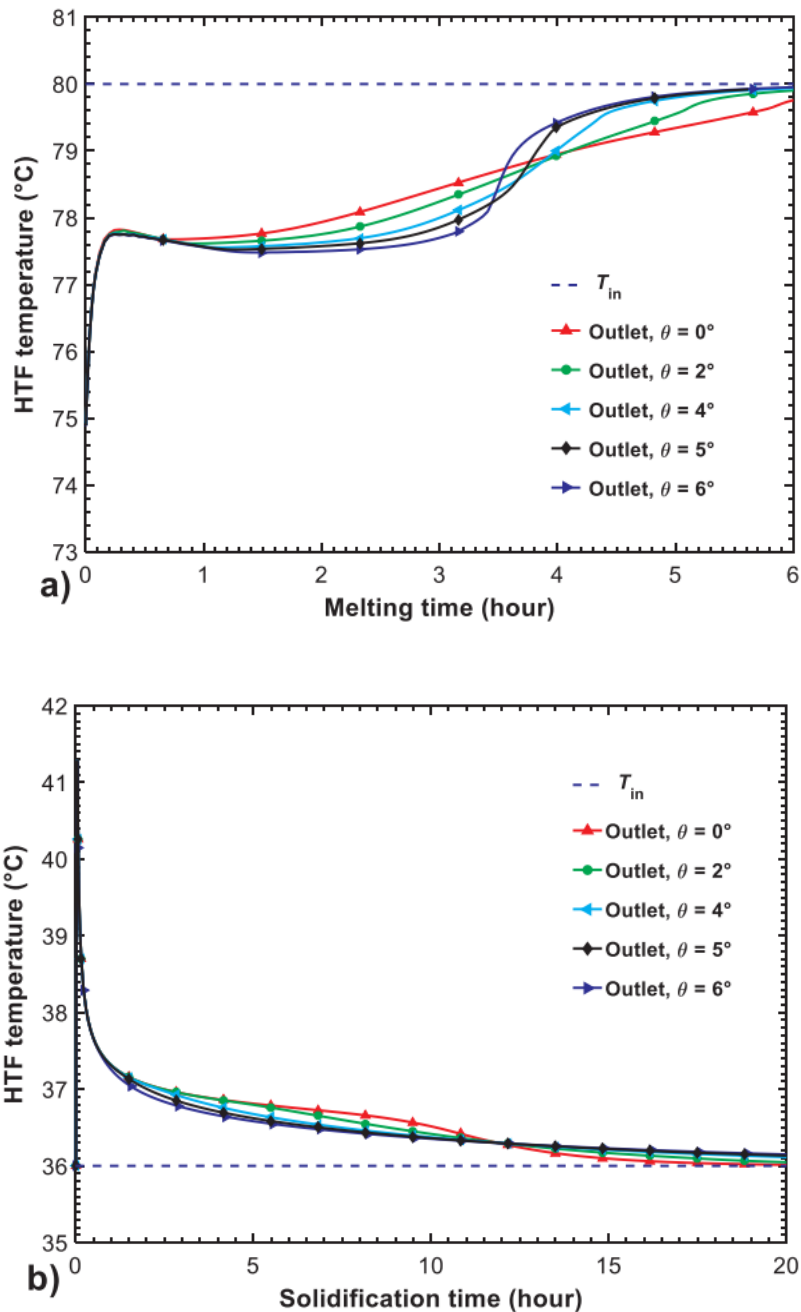
560 The authors evaluated the effect of various parameters including Stefan number (i.e. 0.46, 0.52,
 561 and 0.58) and tilting angle ranging from 0° to 90°. Reynolds number was set at 770 and Grashof
 562 number was ranging from 4.6×10^4 to 5.8×10^4 . They found that the increase in the inlet
 563 temperature was associated with faster melting process and lower melting time. The results
 564 showed that the melting/solidification rates were intensified in the horizontal/vertical
 565 orientation of the heat storage medium. Figure 18 shows the PCM temperature as a function of
 566 time during solidification for different tilting angles. As seen in this figure, there was a rapid
 567 reduction in the PCM temperature as a result of large temperature difference within the initial
 568 stage of the solidification process. The formation of solid PCM by progressing with time
 569 reduced the convection heat transfer by introducing the thermal resistance between the HTF
 570 and PCM. As a result, the conduction heat transfer was the more dominant mechanism during
 571 the solidification process. Regarding the effect of tilting angle, it was noticed that a LHTES
 572 system with 90° angle solidifies faster than other angles.



573
 574 Figure 18. Variation of PCM temperature with time for different inclination angles (Figure
 575 reproduced from [82])
 576

577 Shen et al. [83] developed a numerical model to evaluate the melting performance of a vertical
 578 shell-and-tube LHTES systems with variable tilting angles of the lateral surface. The results
 579 showed that increase in the tilting angle improved the heat transmission during the melting
 580 process while deteriorated the solidification performance. As a case in point, melting time
 581 shortened by 45% by increasing the angle from 0° to 7°. Figure 19 shows that the HTF
 582 temperature as a function of melting/solidification time. In case of the melting process, the

583 HTF outlet temperature was lower at higher tilting angle. This trend was then reversed when
 584 PCM starts the melting process due to the presence of more solid PCM in this case. In case of
 585 the solidification process, there was a marginal change in the HTF temperature with respect to
 586 the tilting angle. They also performed a detailed parametric study to find the optimum tilting
 587 angle of the lateral surface. According to their analysis, tilting angle of 4° was identified as the
 588 ideal angle—reducing the melting and solidification time by 22% and 8.5%.



589

590

591 Figure 19. HTF outlet temperatures during (a) the melting and (b) solidification processes

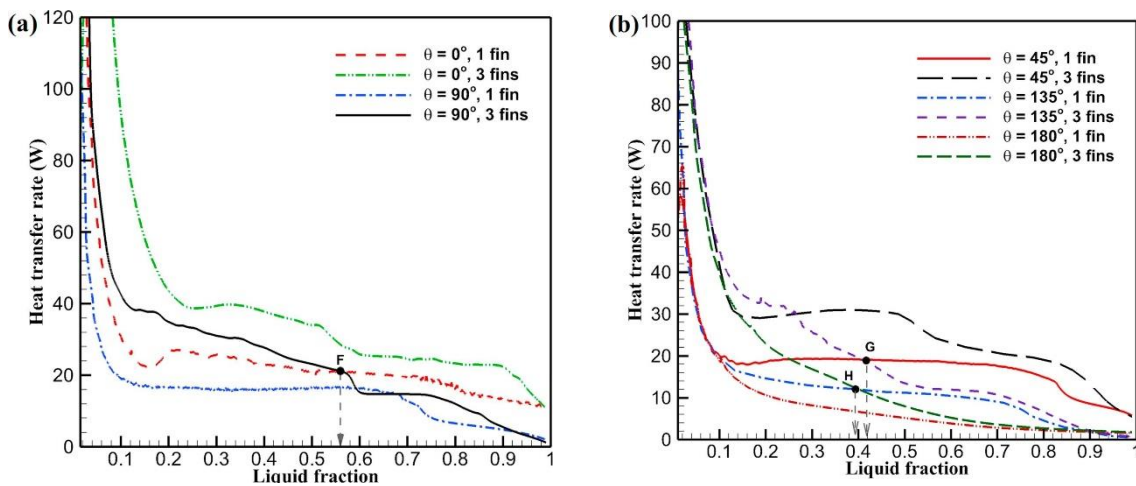
592

(Figure reproduced from [83])

593 5.4 Other geometries

594 Focusing on a flat-type heat sink, Avci and Yazici [84] assessed the melting performance of
 595 N-icosane PCM under a range of inclination angles from 0° to 90° . An imaging technique was
 596 employed to observe the solid-liquid melting interface. The main finding of this work was an
 597 increase in the velocity of the melting front as a result of increasing the tilting angle—leading
 598 to a more uniform temperature distribution on the back side of the flat-type heat sink. However,
 599 this effect was insignificant in the without PCM case.

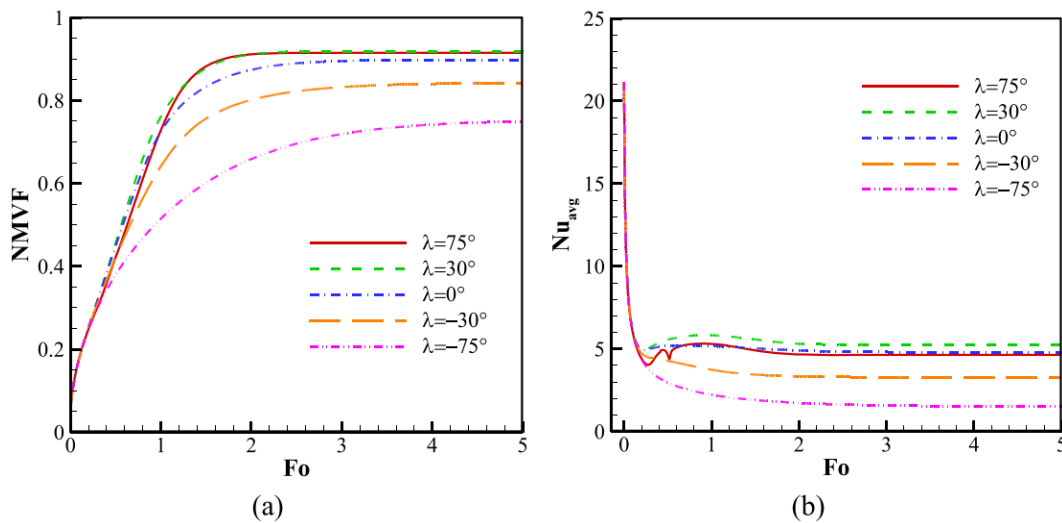
600 Karami and Kamkari [85] focused on the formation of convection flows in a finned cavities
 601 under different tilting angles (0° to 180°). They studied this effect for 3-fin and 1-fin
 602 rectangular cavities. The findings revealed that reducing the tilting angle shortened the melting
 603 duration due to more vortices and intensified natural convection in the liquid PCM. Figure 20
 604 shows the heat transfer rate as a function of liquid fraction for various inclination angles and
 605 number of fins. The heat transfer rate was generally enhanced by increasing the number of fins
 606 at a constant tilting angle. In some specific cases, the results were not consistent shown by
 607 point F, G, and H. At point F, the heat transfer was higher for 1-fin case at 0° than 3-fin case
 608 at 90° beyond 0.56 liquid fraction. For points G and H, the rate of heat transfer in 1-fin case at
 609 45° exceeds than 3-fin case at both 135° and 180° .



610 Figure 20. Variation of heat transfer rate with liquid fraction for various tilting angles and
 611 number of fins (Figure reproduced from [85])

612 Ghalambaz et al. [86] investigated the charging process of octadecane NEPCM with
 613 mesoporous silica particles in an inclined enclosure. The phase-change boundary and heat
 614 transmission in the enclosure were tracked using a deformed mesh model. The Arbitrary
 615 Lagrangian-Eulerian moving mesh approach and finite element method were used to solve the
 616 phase-change equations. Figure 21 shows the NMVF and average Nusselt number versus

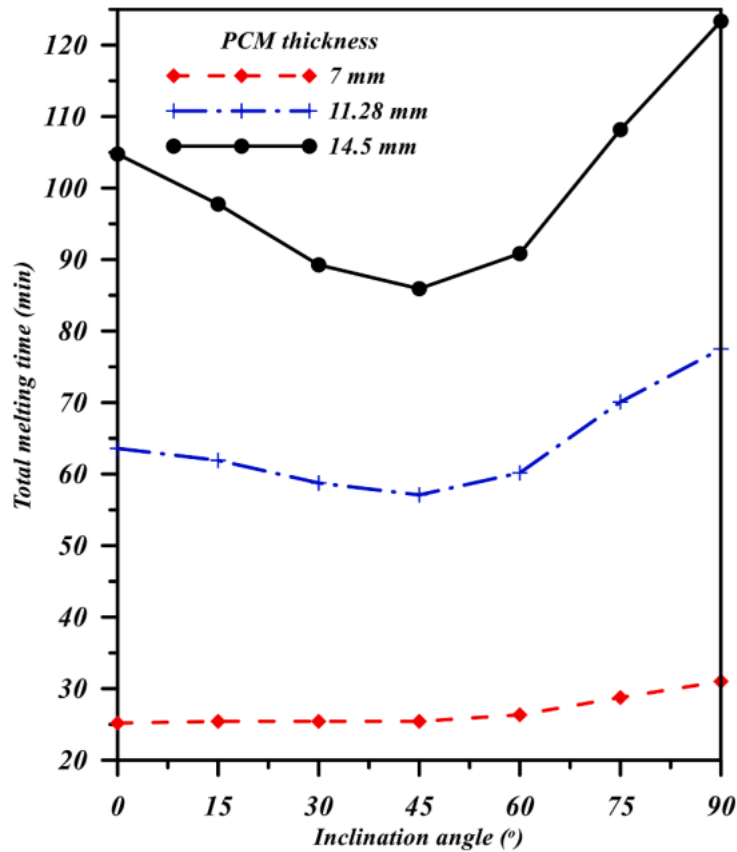
617 Fourier number for various tilting angles. Regarding the role of tilting angle, the authors found
 618 that heat transfer was reduced by 80% at -75° tilting angle. This was due to the hinderance in
 619 the convection flows and less melting at higher tilting angles. This was also evident in the
 620 average Nusselt number, a significant reduction at -75° angle as a result of lower heat transfer.
 621 With respect to nanoparticle addition, the results showed lower phase change heat transfer by
 622 adding nanoparticles. This was attributed to a higher viscosity of the liquid, which prevents the
 623 natural convection flow. As a case in point, employing 5% nanoparticles reduced the heat
 624 transfer by 50%.



625
 626 Figure 21. Variation of NMVF and average Nusselt number versus Fourier number for
 627 various tilting angles (Figure reproduced from [86])

628 Sorour et al. [87] studied the PCM melting in a double-pipe LHTES system with hot water
 629 flowing in the inner tube and PCM located in the annulus. They performed a detailed parametric
 630 study over the PCM mass (i.e. 0.154, 0.308, and 0.46 kg), PCM thickness (i.e. 7, 11.28, and
 631 14.5 mm), and LHTES tilting angles (i.e. 0° , 15° , 30° , 45° , 60° , 75° , and 90°). Depending on
 632 the thickness of PCM, the tilting angle showed different effects on the melting process. Figure
 633 22 shows the variation of melting time with inclination angle for various thickness of PCM. As
 634 seen in this figure, PCM with 7 mm thickness experiences the lowest duration of melting.
 635 However, switching to PCM thickness of 11.28, and 14.5 mm increased the optimum tilting
 636 angle to 45° . The proposed system had the highest melting time at 90° angle regardless of the
 637 PCM thickness.

638



639

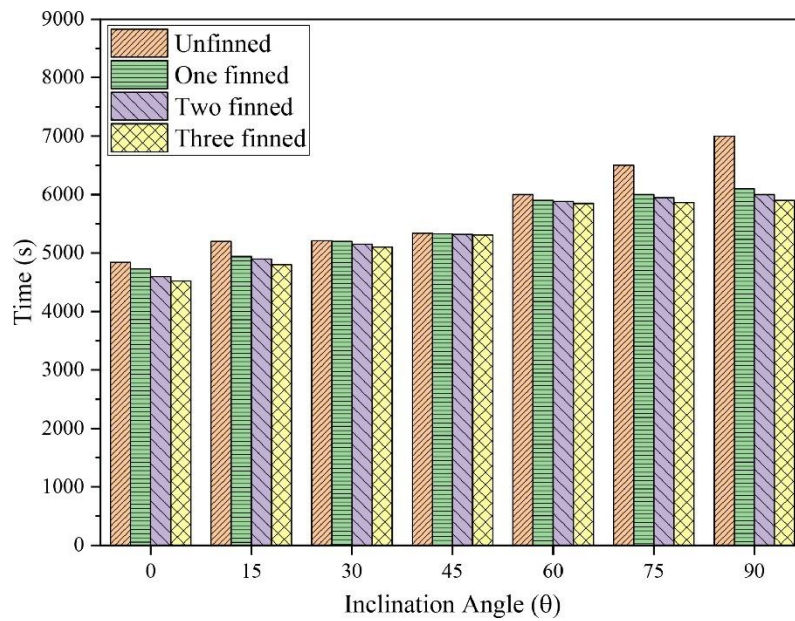
640 Figure 22. Variation of melting time with inclination angle for various thickness of PCM

641

(Figure reproduced from [87])

642

643 Following the same research direction, Kothari et al. [88] focused on Paraffin wax PCM
 644 melting in the heat sink with/without plate fins. The authors examined different heat flux values
 645 (i.e. 1.3, 2.0, and 2.7 kW/m²) and inclination angles (i.e. 0° to 90° with 15° interval). Figure 23
 646 shows the variation melting time with inclination angle for unfinned and finned PCM-based
 647 heat sinks. As seen in this figure, the lowest melting time was achieved in three-finned cases
 648 for all the inclination angles. It was found that the inclination angle of 0° was the optimum
 649 melting angle compared to other cases as a result of more circulation current in the liquid
 650 PCM—reducing the time by 44% and 30% for unfinned and finned configurations. It should
 651 be noted that there is an optimum fin number, beyond which there is no further reduction in the
 652 melting time due to the impediment in the convection flow of liquid PCM.



653

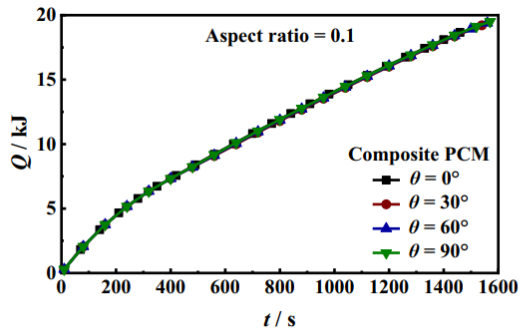
654 Figure 23. Variation of melting time with inclination angle for unfinned and finned PCM-
 655 based heat sinks (Figure reproduced from [88])

656

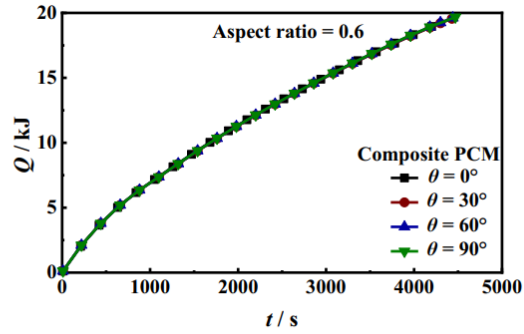
657 Yang et al. [89] conducted a numerical and experimental study on the melting process of PCM
 658 with metal foam in a cavity with various aspect ratios, defined as the width to height ratio of
 659 the cavity. They analysed the melting rate, phase interface, flow streamline, heat storage
 660 capacity, temperature distribution, and heat transfer performance. Figure 24 shows the
 661 variation of heat storage capacity with melting time for composite PCM at various aspect ratios
 662 of the enclosure and tilting angles of a heating surface. The results indicated that at a constant
 663 aspect ratio, the inclination of the heating surface had a negligible impact on the melting rate
 664 and heat storage capacity. However, the geometry with the aspect ratio of 0.1 experienced a
 665 better temperature uniformity and higher heat storage capacity in a shorter period of time.

666 Wang et al. [89] investigated the charging process of flat heat pipe LHTES unit under various
 667 tilting angles. They designed a LHTES unit using flat heat pipe and lauric acid with adjustable
 668 angles. The results showed a delayed melting time of the PCM at lower inclination angle even
 669 though the heat transfer was improved on the PCM side. They also noticed a decreasing and
 670 then increasing trend in the thermal conductivity when the tilting angle increased from 30° to
 671 90°. The feasibility analysis showed that heat transfer was deteriorated at higher power input
 672 of 30 W under low inclination angle of below 30°.

673

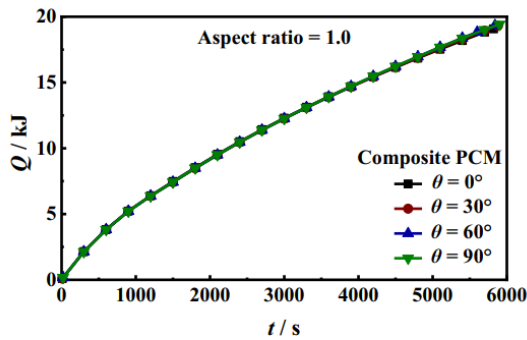


(a)

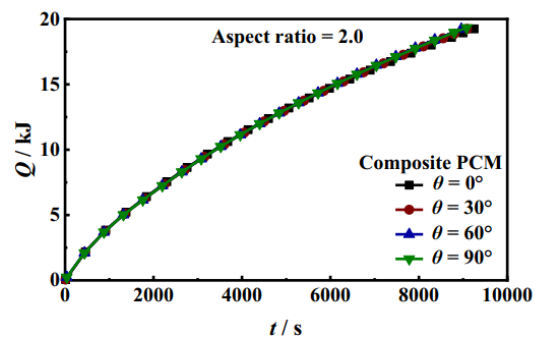


(b)

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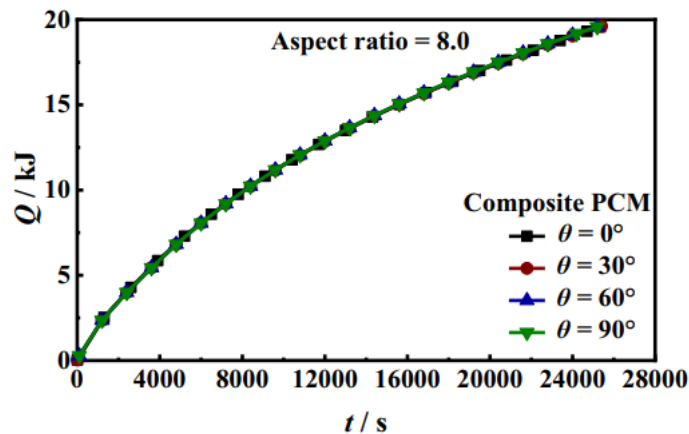


(c)



(d)

675



(e)

676

677 Figure 24. Variation of heat storage capacity with melting time for composite PCM at various
 678 aspect ratios of the enclosure and tilting angles of a heating surface (Figure reproduced from
 679 [89])

680 6. Effect of vibration

681 Vibration and oscillation have been used in several studies to improve heat and mass transfer
 682 in tubular laminar flow. Tubular laminar flow is often used in various energy transport systems,
 683 including chemical reactions, thermal sterilizing, slurry flow, and the industries of food and
 684 pharmaceuticals. Table 4 lists the geometrical, operating conditions, and key take-away

685 findings of recent studies addressing the role vibration on the melting/solidification procedures
 686 of PCMs/NEPCMs inside an enclosure with different geometries. The citation list [91–94]
 687 focuses on this importance in different geometries as summarized in the following subsections.

688 **Table 4.** A summary of studies on the effect of vibration on the melting/solidification
 689 procedures of PCMs/NEPCMs inside an enclosure with different geometries

Authors (year)	Configuration	Type of study	Studied parameters	Highlighted results/findings
Hajiyani et al. (2018) [91]	PCM placed in a cylindrical geometry	Numerical	Effect of vibration on the melting process	Different melting behavior in the presence of vibration force. No stratification observed as a result of vibration force, leading to equal melting rate at the bottom/top of the enclosure.
Joshy et al. (2020) [92]	PCM-based thermal management of electric vehicle Lithium-ion battery cells	Experimental	Effect of frequency and amplitude vibration on the solidification process	Frequency as the most dominant parameter on the temperature rise at low discharge rate. Amplitude and frequency as significant factors at high discharge rate. Lower temperature at the outer edges of the battery surface in a staggered arrangement of batteries.
Vadasz et al. (2012) [93]	RT35 PCM embedded in a spherical shell under vibration effect	Experimental	Effect of vibration on the solidification process	Shorter solidification time when PCM was subjected to vibration. More uniform solid structure at higher vibration frequency.
Zhou et al. (2018) [94]	Super-cooled sodium acetate PCM inside a rounded-rectangular enclosure vibrated through freely falling steel ball solution was cooled to very low temperatures.	Experimental and numerical	Effect of falling height, steel ball diameter, and percussion position on the solidification process	Better solidification performance under larger striking momentum. Effective commencement of the solidification process with percussion momentum imposed near the edges or cover lid.

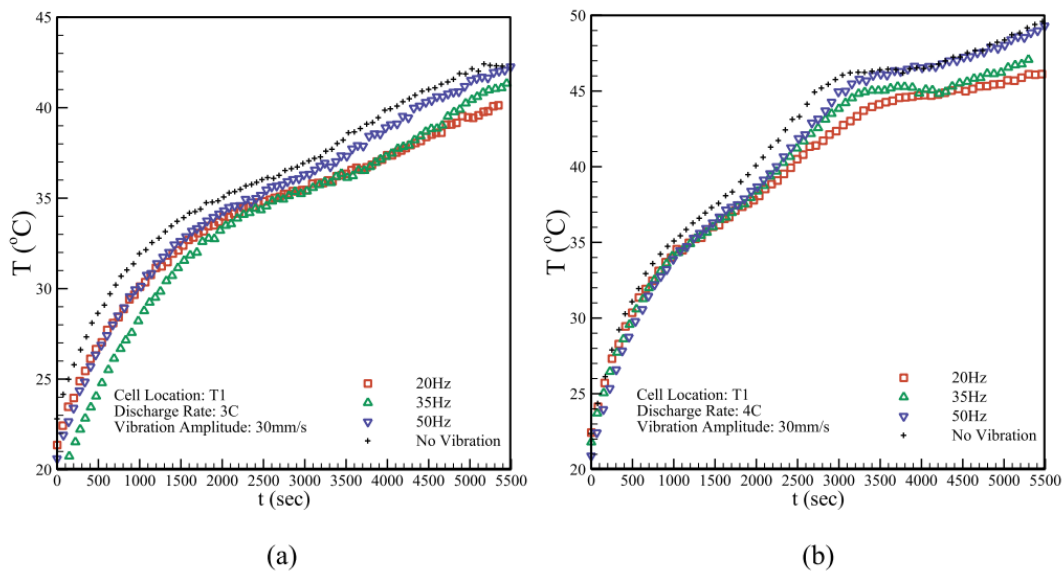
690

691 *6.1 Cylindrical geometry*

692 Hajiyani et al. [91] numerically studied the PCM charging inside a cylindrical container
 693 subjected to vibration effect. The phase transition of PCM was modeled using enthalpy-
 694 porosity method, applicable for convection-diffusion phase change during the melting process
 695 of a pure metal. To simulate the charging behavior of a PCM under vibrational circumstances,
 696 the COMSOL Multiphysics program was used. According to their findings, the behavior of the
 697 melting process is greatly impacted by vibration.

698 Joshy et al. [92] investigated the influence of vibration on battery thermal management (BTM)
 699 system embedded with PCM. Aluminum cylinders with ceramic cartridge heaters replicated
 700 the Lithium-ion batteries. The amplitude and frequency were varied from 30–50 mm/s and 20–
 701 30 Hz, as typical values for hybrid electric vehicles (PHEV). Figure 25 shows the variation of
 702 temperature at the selected battery surface (T1 cell location in this case) with time for various
 703 discharge rate. According to this figure, the battery temperature increased with the vibration

704 frequency for both cases. It should be noted that this effect was not significant when the
 705 temperature was below the PCM melting point. The liquid motion as a result of buoyancy effect
 706 helped with the formation of thermal boundary layer—leading to the expansion of liquid region
 707 at the top by thermal stratification effect in the no vibration case. However, the addition of
 708 vibration may help or deteriorate the gravitational force, which may assist or hinder the
 709 movement of liquid phase and natural convection flows.



710 (a) (b)
 711 Figure 25. Variation of temperature at the selected battery surface (T1 cell location in this
 712 case) with time for 30 mm/s amplitude: (a) 3C discharge rate and (b) 4C discharge rate
 713 (Figure reproduced from [92])

714 *6.2 Other geometries*

715 Vadasz et al. [93] evaluated the impacts of vibration on the discharging procedure of paraffin
 716 wax PCM in a spherical shell. Experiments were carried out on a sphere with a diameter of 40
 717 mm and wall temperature of 20°C lower than the mean solidification temperature. The setup
 718 was exposed to a vibration frequency ranging from 10 to 300 Hz. The authors compared the
 719 results with no vibration case. An improvement in heat transmission through the use of
 720 vibration decreased the amount of time required for discharging the heat from PCM. Zhou et
 721 al. [94] conducted a series of tests in a thermal storage unit of rounded-rectangular geometry
 722 to investigate the effect of percussive vibration on triggering the discharging of salt solution of
 723 super-cooled sodium acetate. The steel ball was allowed to freely fall to the PCM surface unit,
 724 which was then subjected to percussive vibration using the parameters of crystallization
 725 induction time and percussive number. According to the findings, it was best to activate the

726 discharging of the super-cooled sodium acetate solution using a percussion with a greater
727 momentum (a larger ball diameter and a higher falling height).

728 **7. Conclusions**

729 Given the intermittency nature of renewable energy resources, the development of fast-
730 responsive and low-cost thermal energy storage (TES) technologies are of vital importance.
731 However, latent heat thermal energy storage (LHTES) systems filled with phase change
732 materials (PCMs) often suffer from low heat transfer rates. Previous studies have primarily
733 focused on using fins and novel encapsulated PCMs (NEPCMs) as methods of enhancing heat
734 transfer. This paper aimed to provide a comprehensive review of the effect of other factors,
735 including the application of a magnetic field, rotation, tilt angle, and vibration, on the melting
736 and solidification performance of PCMs inside enclosures with various geometries.

737 It was found that increasing the magnetic number and decreasing the Hartmann number are
738 important to accelerate the melting and solidification processes of phase change materials
739 (PCMs) used in thermal energy storage (TES) systems. The direction of the magnetic field
740 showed marginal influence on the charging/discharging processes. A dual non-uniform
741 magnetic fields might have potential design and operational implications for PCM-TES
742 systems to enhance the heat transfer and improve the overall performance of TES systems.

743 Another design parameter was the rotation of LHTES unit. Reviewing the literature revealed
744 that rotating the enclosure in a counter direction of buoyancy flow improved the melting
745 rate/time. A possible method to greatly minimise the melting time was to use dual opposing
746 rotations with a 180° difference between the stop ends. In case of intermittent rotation, an
747 increase in bottom eccentricity was found to enhance the melting process, while an increase in
748 top eccentricity resulted in an improvement of the solidification process.

749 In terms of tilting angle effect, the maximum melting rate was achieved in the horizontal
750 orientation of the enclosure for PCMs with a small thickness. However, it was shown that
751 switching to sufficiently thicker PCM can increase the optimum tilting angle. Increasing the
752 tilting lateral surface angle of the cavity improved and deteriorated the charging and
753 discharging processes.

754 Even though vibration was identified as an effective approach to enhance the heat transfer in
755 LHTES unit, only a very few studies have focused on the performance of PCM under vibration
756 frequency. Taken together, it was found that frequency and amplitude/frequency were the
757 significant factors at low and high discharge rates, respectively. The percussion momentum
758 and strength are effective parameters to trigger the melting/solidification processes.

759 There are some interesting unanswered questions arising from the review of previously
760 published studies in this realm including: (i) the interaction between several active and passive
761 methods in terms of improving the melting and solidification processes, (ii) the determination
762 of optimum design parameters leading to maximum heat transfer during the
763 charging/discharging cycles, (iii) the use of machine learning algorithms together with CFD to
764 predict the thermal performance of PCMs under different operating conditions, and (iv) the
765 technical challenges and economic aspects of the proposed techniques.

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