

1 A comparative study of heavy metals removal using agricultural waste biosorbents

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6 **Abstract**

7 The adsorption capabilities of rice husk, coconut coir and moringa seeds were evaluated for
8 the first time under the same experimental conditions for the removal of copper (Cu), nickel
9 (Ni) and zinc (Zn) from underground water. The effects of adsorbent dosage, pH and contact
10 time were studied. Copper and nickel were removed up to 99%, using rice husk, coconut coir
11 and moringa seeds. Zinc concentrations can only be reduced to up to 70% using rice husk.
12 However, removal was reached 99% when coconut coir and moringa seeds were used. Moring
13 seeds showed the highest adsorption capacities (Zn= 42.3 mg g⁻¹, Cu= 23.3 mg g⁻¹, Ni= 16.1
14 mg g⁻¹) amongst the biosorbents tested. Nickel was the least adsorbed heavy metal for all
15 biosorbents studied. Moringa seeds leached sulfur at acidic pH values (< 4). Models showed
16 that adsorption using these biosorbents follows Langmuir isotherm and Pseudo-second order
17 kinetic.

18 *Keywords: rice husk; coconut coir; moringa oleifera seeds; heavy metal removal; adsorption;*
19 *biosorbents*

20 **1. Introduction**

21 Water pollution is a global challenge and causes health problems throughout the world (Bakker,
22 2012). The contaminated water with heavy metals is known to be an environmental issue and
23 have a significant effect, particularly on the developing countries. Industrial processes such as
24 metal plating, fertilizer production, barrier fabrications, smelting and mining operations (Peng
25 et al., 2018), have greatly enhanced the mobilisation of the heavy metals. Hence, they are
26 entering directly or indirectly into the environment by means of various sources. They have

27 threatened to aquatic organisms and human life as they are known to be toxic or carcinogenic
28 (Fu and Wang, 2011). Although several heavy metals, such as zinc (Zn), iron (Fe), manganese
29 (Mn) and cobalt (Co), have an important role in biochemical processes in human body, they
30 are highly toxic as ions or in compound forms; they are soluble in water and may be readily
31 absorbed into living organisms. (Abdullah et al., 2019). Heavy metals of particular concern in
32 treatment of industrial wastewaters include zinc, copper, nickel, mercury, cadmium, lead and
33 chromium. Therefore, the mitigation of these heavy metals is of utmost significance. Too much
34 zinc can cause health problems, such as stomach cramps, skin irritations, vomiting, nausea and
35 anemia (Oyaro et al., 2007). Excessive ingestion of copper causes e.g. vomiting, cramps,
36 convulsions, or death (Paulino et al., 2006). High nickel levels may result serious lung and
37 kidney problems aside from gastrointestinal distress, pulmonary fibrosis and skin dermatitis
38 (Borba et al., 2006).

39 There are various treatment methods, such as membrane technology (Abdullah et al.,
40 2019), precipitation, coagulation-flocculation, ion exchange and adsorption, have been
41 implemented to treat these heavy metals from wastewater and water (Abdullah et al., 2019).
42 These methods have some drawbacks, including high energy cost, inefficient removal,
43 production of toxic sludge and fouling of metal ions (Sun et al., 2018). However, adsorption-
44 based technologies have potential to remove heavy metal ions due to their simplicity and cost
45 efficiency (Peng et al., 2018). A wide range of adsorbents, such as activated carbons
46 (Kołodzyńska et al., 2017), clays (Seliman et al., 2014), zeolites (Lu et al., 2016) and metal-
47 organic frameworks (Mon et al., 2016) , have been studied for the heavy removal from water.
48 In adsorption-based technologies, low-cost and environmentally friendly alternative sorbents
49 are still needed to be explored e.g., biosorbents, which are produced from agricultural waste.
50 Biosorbents that are available in nature and prepared from agro-wastes such as rice husk (
51 Shukla, 2008), coconut coir (Asim et al., 2020), maize straw (Guo et al., 2015), orange peel

52 (Gupta & Nayak, 2012) and moringa oleifera seeds (Obuseng et al., 2012;) have been used
53 with or without chemical modifications. In these studies, biosorbents were investigated for the
54 removal of lead (II), copper (II), zinc (II), manganese (II), nickel and arsenic from water. These
55 cost-effective and environmentally benign materials have exhibited effective removal of heavy
56 metals and thus are considered as sustainable sorbents used for heavy metals in water treatment
57 (Mohan and Sreelakshmi, 2008). Zhang et al (2014) determined the Cu adsorption capacity of
58 rice husk that they reported 89% removal and 17 mg g⁻¹ adsorption capacity. In contrast,
59 Marshall et al (1993) reported relatively low adsorption capacities for Cu (1.21 mg g⁻¹), Zn
60 (0.75 mg g⁻¹) and Ni (0.23 mg g⁻¹) using rice hulls and bran, which could be resulted from
61 multi-component adsorption effect and biosorbent properties. Studies using coconut coir for
62 adsorption of heavy metals are limited. Aravind et al (2017) reported up to 90% Ni and Cu
63 removal (from Ni= 5 mg l⁻¹, Cu=5 mg l⁻¹ and Cd= 0.9 mg l⁻¹ initial solution). Abdul Rahil et al
64 (2020) estimated the adsorption capacities for Cu and Ni approx. 0.15 mg g⁻¹ and 0.05 mg g⁻¹,
65 respectively, using coconut waste-based adsorbent. Performance of moringa seeds for heavy
66 metal removal were also studied. Obuseng et al (2012) showed that unmodified moringa
67 oleifera seeds can remove 5 mg l⁻¹ Cu, Zn and Ni from water up to 80%, 60% and 20%,
68 respectively, in an hour. Similarly, Maina et al (2016) reported up to 60% and 40 % removal
69 for Zn and Cu from multi-element solution. They also concluded that the pH, initial metal
70 concentration, biosorbent amount, particle size, and temperature affected the adsorption
71 process.

72 In this study, we explored the feasibility of using natural sorbents such as coconut coir,
73 rice husk and moringa seeds, for heavy metal removal, particularly copper, zinc and nickel,
74 from water. For the first time, these biosorbents were compared using the same initial heavy
75 metal concentrations, simulating heavy metals mixed in underground water sources. The
76 influences of adsorbent amount, solution pH and contact time on their adsorption capacity

77 towards mixed heavy metals were elucidated. Adsorption isotherms and kinetics were
78 determined. Biosorbents were also characterised using multiple techniques, including X-ray
79 diffraction (XRD), scanning electron microscopy (SEM), Fourier transform infrared
80 spectroscopy (FTIR) in order to explain heavy metal removal mechanism.

81 **2. Experimental**

82 **Biosorbent preparation**

83 Asian rice husk was purchased from Thailand (T.K. Rice Mill, Bangkok). After
84 crushing (Retsch Mill SM2000) and sieving (250 μm), samples were washed thoroughly for 15
85 minutes to remove any dirt and metals that could interact with the main experiments. The
86 samples were dried in an oven at 50 $^{\circ}\text{C}$ for 24 hours and then stored in polythene bags in a
87 desiccator at room temperature (RT) to avoid any increase in moisture content.

88 The coconut coir pith was purchased from Exotic Pets in the form of dense brick.
89 Samples were shredded using a Retsch Mill SM2000 and sieved to obtain average particle size
90 of 500 μm . They were washed thoroughly, dried at 90 $^{\circ}\text{C}$ in a conventional oven overnight and
91 then stored in polythene bags in a desiccator at room temperature.

92 The moringa oleifera seeds used in the experiment was supplied from Seeds-Store,
93 Germany (harvested in Egypt/Canary Islands). The dark-brown shells were manually cracked
94 in order to remove the kernels. The small and white seed kernels were shredded using a Retsch
95 M2000 Shredder. The powder was sieved in the range of 710-850 μm , resulting with an average
96 particle size of 783 μm . Samples were then stored in polythene bags in a desiccator at room
97 temperature.

98 **Characterisation of biosorbents**

99 X-ray diffraction (XRD) measurement was performed using a PANalytical X'Pert
100 Pro diffractometer operating at 40 kV, 40 mA and $\text{CuK}\alpha$ radiation (λ : 1.540598 \AA), equipped
101 with a PIXCell3D detector. The scan was obtained between 10-70 $^{\circ}$ (2 θ).

102 The morphology of the biosorbents were characteristics by scanning electron
103 microscopy (SEM, JEOL JSM-7100F). The samples were coated with 10-20 nm thick gold
104 layer before analyses. Imaging was conducted at 5 kV.

105 The functional groups present in the biosorbents were characterized by a Fourier
106 transform infrared (FTIR) spectrometer (Bruker IFS66) using diffuse reflectance mode. The
107 spectral range was varied from 4,000 to 400 cm^{-1} . All the spectra were obtained under
108 absorbance mode.

109 A Panalytical Epsilon 3XL model X-ray fluorescence analyser (XRF) was used in
110 determining both the qualitative and quantitative elemental composition of the samples.
111 Powder samples were placed in a plastic cup to about 4.9 cm in depth and covered with a plastic
112 film at the bottom. Approximately, 5 g of powder was used during measurements.

113 Zeta potential of samples (at pH 7) was determined using A Zetasizer Nano ZS
114 instrument (Malvern, UK). The pH was adjusted to 7 by mixing 0.25 g of biosorbent, 1 g of
115 NaCl, 100 ml of distilled water, and 1-2 ml of 0.5 M NaOH.

116 Specific surface area of biosorbents were estimated using nitrogen adsorption-
117 desorption isotherm measurements (Micrometrics 3Flex adsorber). Dried samples were
118 degassed for 3 h at 150 °C before analysis and cooled to -196 °C using liquid nitrogen. The
119 distribution of micropores was analysed by the *t*-plot method.

120 **Heavy metal solution preparation**

121 Multi-component solutions of Cu, Zn and Ni were freshly prepared prior to each
122 adsorption experiment to simulate the water sources. For adsorption tests, brackish water
123 solutions were obtained by dissolving sodium chloride (NaCl), copper (II) chloride dihydrate
124 ($\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$), zinc sulfate heptahydrate ($\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$) and nickel (II) nitrate hexahydrate
125 ($\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$) in water purified using Milli-Q®-IQ 7015 Ultrapure lab water purification

126 system (at 18.2 MΩ.cm resistivity). All chemicals were purchased from Sigma-Aldrich and
 127 used without further treatment.

128 **Quantitative analysis of heavy metal concentrations in water**

129 For analyses using inductively coupled plasma atomic emission spectroscopy (ICP-
 130 AES, Perkin Elmer 300 DV), around 25 ml of samples was taken from the solutions at
 131 predetermined times. The adsorbents were separated from solutions *via* centrifugation (Hettich,
 132 Rotofix 32 A) at 3,000 rpm for 5 min. The supernatant was decanted and passed through a
 133 Minisart® (0.45 μm, hydrophilic) syringe filter. A 10 ml aliquot of the filtered solution was
 134 then pipetted in a 15 ml polypropylene conical tube and the sample was acidified with 5 ml of
 135 30% (v/v) nitric acid and refrigerated to prevent metal precipitation and microbial degradation.

136 Calibration standards were prepared by using a multi-element solution. Three-point
 137 calibration curves were established for each metal species. For quality control, ultrapure water
 138 sample (18.2 MΩ.cm resistivity) was included in every batch of analysis.

139 **Adsorption experiments**

140 Batch adsorption studies were conducted at room temperature (21 ± 3 °C) using 400 ml
 141 of heavy metal solution. Solutions were continuously stirred at a constant rate using a magnetic
 142 stirrer. The details of the initial contaminant concentrations and experimental conditions are
 143 given in Table 1.

144 **Table 1.** Initial concentrations of heavy metals and experimental conditions.

Biosorbents	Contaminants	Concentration of Adsorbents in Water (g l ⁻¹)	Initial Concentration of the Contaminants (mg l ⁻¹)	pH
Coconut Coir	Copper	2, 5, 10, 20, 40	2.9	6
	Zinc	2, 5, 10, 40	0.84	
	Nickel		0.174	
Rice Husk	Copper		2.9	6

	Zinc	2, 5, 10, 40	0.84	
	Nickel		0.174	
Moringa Oleifera	Copper		2.9	6
	Zinc	2, 5, 10, 40	0.84	
	Nickel		0.174	

145 The effect of precipitation was quantified by control experiments where pH of the
146 solution was adjusted to 3.5, 6.5 and 10.5 with mixed heavy metal solutions without
147 biosorbents. The heavy metal concentrations were set to 1 mg l⁻¹ and 12.5 mg l⁻¹ and initial/final
148 concentrations of heavy metals were measured. During the adsorption experiments, pH was
149 continuously monitored and adjusted by adding 5 M NaOH and/or HCl dropwise to the
150 working solution under vigorous stirring and using a Hanna HI 5522-02 pH-meter, which was
151 calibrated daily using fresh buffer solutions. No more than 4 ml of 5 M NaOH and/or HCl were
152 needed to adjust the pH to a desired value in all the experiments. The effect of pH on the uptake
153 of copper using rice husk, coconut coir and moringa seeds was also studied at the pH values of
154 4, 6, 8 and 10 at a constant adsorbent dosage (10 g l⁻¹) for 2 h. This is because copper solubility
155 in water dramatically reduces from 20 to 0.05 mg l⁻¹ between pH 6-8 hydroxide
156 (<https://heienv.com/hydroxide-precipitation-of-metals/>)

157 To determine the adsorbent dosage and contact time for the adsorption tests, 2-40 g l⁻¹
158 of coconut coir, rice husk and moringa seeds were added to the water samples (at optimum pH
159 determined) and solutions were mixed on a magnetic stirrer. Adsorption isotherms were
160 constructed using 40 g l⁻¹ biosorbents with the heavy metal concentration range of 1-150 mg l⁻¹
161 at pH 6.

162 Sulfur leaching rate from moringa oleifera seeds (5 g l⁻¹) was also studied at various pH
163 values (4-7) up to 120 minutes. Sampling from water solutions and metals analysis were
164 performed, as explained previously.

165 Removal efficiency as percentage and adsorbed amount of metals were calculated using
166 the following equations, respectively.

167
$$Re (\%) = \frac{(C_0 - C_e)}{C_0} \times 100 \quad (1)$$

168
$$Q_e = \frac{(C_0 - C_e) V}{m} \quad (2)$$

169 where, R_e is removal efficiency (%), C_0 is the initial concentration (mg l^{-1}), C_e is the residual
 170 concentration (mg l^{-1}) at equilibrium, V is the volume of the solution and m is the adsorbent
 171 dosage (g).

172 The adsorbed amount on the biosorbents were calculated by using the mass-balance
 173 relationship, which is given in the following equation.

174
$$Q_t = (C_0 - C_t) \times \left(\frac{V}{m}\right) \quad (3)$$

175 where, Q_t (mg g^{-1}) is the amount adsorbed per unit mass of adsorbent in time t (min), C_0 (mg
 176 l^{-1}) is initial liquid-phase concentration of adsorbates at time equals to 0, C_t (mg l^{-1}) is liquid
 177 phase concentration of heavy metals at time equals to t (min), V (l) is the volume of the solution
 178 and m (g) is the mass of the biosorbent.

179
$$\ln(Q_e - Q_t) = \ln(Q_e) - k_1 \times t \quad (4)$$

180
$$\frac{t}{Q_t} = \frac{1}{k_2 \times Q_e^2} + \frac{1}{Q_e} \quad (5)$$

181 where, Q_t (mg g^{-1}) and Q_e (mg g^{-1}) are the adsorbed amount of metal ions at time t (min) and
 182 at equilibrium, respectively; k_1 (min^{-1}) is the pseudo first order rate constant and k_2 (g mg^{-1}
 183 min^{-1}) is the pseudo second order rate constant and t (min) is the adsorption time.

184 To determine the adsorption mechanism, Freundlich (Eq 6) and Langmuir (Eq 7)
 185 models were employed that are given by the following equations:

186
$$Q_e = K_F \cdot C_e^{\frac{1}{n}} \quad (6)$$

187 where K_F is the constant of Freundlich isotherm indicating the adsorption capacity of the
 188 biosorbent, C_e is the adsorbate concentration in the solution at equilibrium and $1/n$ is a
 189 representation of the adsorption intensity between the biosorbent and adsorbate molecules.

190
$$\frac{C_e}{q_e} = \left(\frac{1}{bq_m} \right) + \frac{C_e}{q_m} \quad (7)$$

191 where, C_e is the adsorbate concentration in the solution at equilibrium, q_e is the amount of
192 solute adsorbed per unit mass of biosorbent, b is the constant of Langmuir isotherm and q_m is
193 the maximum adsorptive capacity of the biosorbent at equilibrium.

194 **Results and Discussions**

195 **Characterisation**

196 The crystal structure of the biosorbents were evaluated using XRD. A broad reflection
197 was detected at the 2θ of 22.5° for rice husk that is a characteristic peak of amorphous silica
198 (Seliem et al., 2016). The XRD pattern of moringa seeds showed a broad band approx. at the
199 2θ of 20° , which is attributed to the amorphous nature of the material. This is due to the high
200 composition of protein and oil (Abdulkarim et al., 2005). Araújo et al (2010) suggested the
201 adsorbate can more easily penetrate the surface of the adsorbent, thus favouring the adsorption
202 process because of the amorphous nature of the adsorbent. XRD pattern of the coconut coir
203 also showed low crystallinity (amorphous). The amorphous characteristic of the coir is due to
204 the high lignin content in its structure (Rosa et al., 2010). The peaks $\sim 16^\circ$, 22° and 35° represent
205 cellulose (Tomczak et al., 2007).

206 The structures of of rice husk, coconut coir and moringa seeds were investigated via
207 SEM. The irregular superficial layer of silica and natural resins can be observed in rice husk
208 structure. Coconut coir pieces approx. 25 micron in size with the small entities on the surface
209 of the large pieces. The seeds of the *Moringa oleifera* is visible whilst they are agglomerated
210 and grouped together, resulting up to 50 micron in size.

211 The functional groups were determined in order to understand the interaction between
212 the biosorbents and the metal ions using FTIR. The broad peak that was observed approx. at
213 3340 cm^{-1} for all 3 biosorbents indicates strong O-H (H-bonded) stretching of cellulose and
214 lignin in macromolecular association (Tariq et al., 2018). The peak at 1060 cm^{-1} represents OH

215 group, which is derived from deformation modes of alcohol or phenol, with a sterically
 216 hindered OH and also represents functional groups of Si–O–Si (Pathiraja et al., 2014). The
 217 small peak observed at 1254 cm⁻¹ for coconut coir possibly represent C-C and C-O and
 218 stretching and COH bending at C6 in cellulose (Sangian et al., 2017) The FTIR spectra of
 219 moringa seed showed the presence of various functional groups, compared to rice husk coconut
 220 coir. The bands in approx. 2920 cm⁻¹ and 2854 cm⁻¹ in moringa seeds were attributed to the
 221 symmetric and asymmetric stretching of group C-H-CH₂ present in fatty acids (Araújo et al.,
 222 2010). Two strong absorption bands were observed at 1654 cm⁻¹ and 1546 cm⁻¹ that are
 223 characteristics of amide I and II respectively, which confirms the structure of the protein
 224 present in moringa seeds. The peak at 1747 cm⁻¹ belongs to the carbonyl (C=O) stretching
 225 vibration of the carboxyl groups of lignin in the moringa seeds (Feng et al., 2009).

226 BET surface areas, estimated pore diameters and zeta potentials of the biosorbents are
 227 shown in Table 2. Moringa seeds and coconut coir have 2 times higher BET surface area than
 228 rice husk. However, results showed that the surface area of these biosorbents are much smaller
 229 (< 19 m² g⁻¹) than other adsorbents. Rice husk and moringa seeds have micropores (< 2 nm)
 230 while coconut coir has mesopores (2-50 nm). In agreement with the literature result, these
 231 biosorbents are negatively charged at pH 7, observed by zeta potential measurements (O'
 232 Bezerra et al., 2018).

233 **Table 2:** BET Surface area, estimated pore diameter and zeta potential of biosorbents

Biosorbent	BET surface area (m ² g ⁻¹)	Pore diameter (nm)	Zeta potential (mV)*
Rice husk	8.1 ± 0.1	1.5	-38.2 ± 0.2
Moringa seed	18.9 ± 0.2	1.6	-28 ± 0.012
Coconut coir	16.7 ± 0.3	3.9	-22 ± 0.5

234 *pH= 7, T= 25 °C

235 The chemical compositions of biosorbents used in this study are presented in Table 3.
 236 Quantitative analysis using XRF showed that rice husk mainly constitutes Si (94 mg g⁻¹). The

237 Si contents of coconut coir and moringa seeds are $\sim 13.6 \text{ mg g}^{-1}$ while moringa seeds also
 238 contain K (16.9 mg g^{-1}). All three biosorbents' Al content is similar (10.4 mg g^{-1}).

239 **Table 3:** Elements obtained in the biosorbents via XRF analysis.

Biosorbent	Al (mg g^{-1})	Si (mg g^{-1})	K (mg g^{-1})	Ca (mg g^{-1})
Rice husk	10.4 ± 0.4	94.0 ± 3	5.6 ± 0.2	1.7 ± 0.1
Moringa seeds	10.5 ± 0.2	13.6 ± 0.3	16.9 ± 0.4	4.1 ± 0.01
Coconut coir	10.5 ± 0.4	13.5 ± 0.2	3.2 ± 0.4	0.25 ± 0.14

240

241 **Adsorption experiments**

242 Table 4 shows the effect of pH on the precipitation of the heavy metals. There is no
 243 significant precipitation of heavy metals at pH 4 and 6 for both initial concentrations. The
 244 precipitation of copper and zinc started at pH 8. All three heavy metals precipitated at pH >10
 245 due to an increase in metal hydroxide formation that is insoluble. Copper's theoretical
 246 solubility is 20 mg l^{-1} at pH 6. This reduces to 0.05 mg l^{-1} at pH 8. Nickel's solubility has a
 247 similar trend, but drastic reduction occurs after pH ~ 9 (Solubility 70 mg l^{-1} and 0.1 mg l^{-1} at
 248 pH 8 and 10.2, respectively). Zinc's solubility has a minimum (0.1 mg l^{-1}) at pH ~ 10.5 . These
 249 results suggest that adsorption experiments can be conducted at pH 4 or 6 to avoid precipitation.

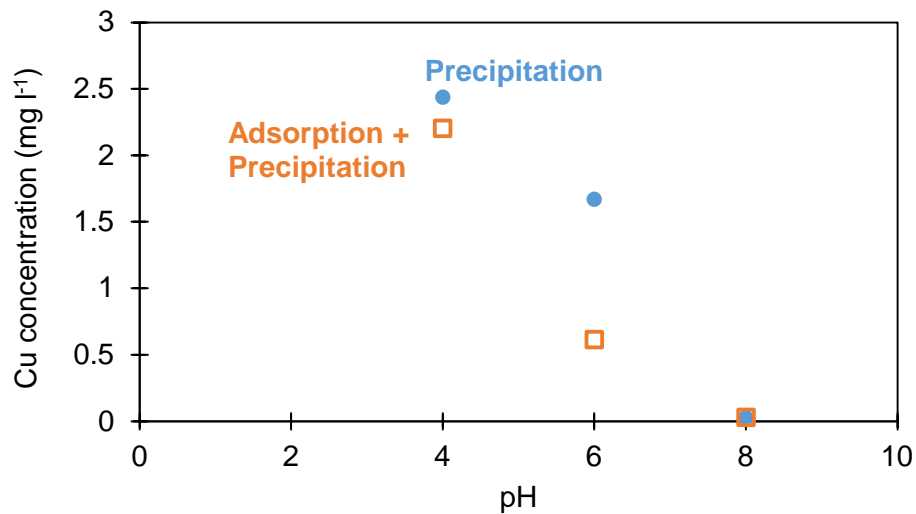
250 **Table 4:** Precipitation of heavy metals as a function of pH (4, 6, 8, 10) Initial metal
 251 concentrations are ~ 1 and $\sim 12.5 \text{ mg l}^{-1}$ for each heavy metal ($T = 20 \pm 2 \text{ }^\circ\text{C}$).

pH	Time (h)	Cu (mg l^{-1})		Zn (mg l^{-1})		Ni (mg l^{-1})	
4	0	1.1	12.5	1.1	12.6	1.1	12.5
	2	0.99	12.3	0.98	12.2	0.97	12.4
6	0	1.1	12.6	1.1	12.6	1.1	12.5
	2	0.95	9.8	0.99	12.4	0.98	12.3
8	0	1.1	12.4	1.1	12.4	1.1	12.4
	2	0.012	0.056	0.009	8.4	0.99	12.2
10	0	1.1	12.6	1.1	12.6	1.1	12.5
	2	0.005	0.009	0.004	0.0085	0.045	0.093

252 The copper concentration as a function of pH using rice husk were given in Figure 1.

253 The copper removal with adsorption increased by approx. 55% when the pH value was

254 increased from 4 to 6. In contrast, the reduction in copper concentration occurred at pH 8 and
255 10 was due to chemical precipitation rather than adsorption. The optimal pH value was
256 determined as 6 for the adsorption of Cu on rice husk, showing the highest removal (75%).
257 That is approx. three times greater than the copper removal by adsorption at pH 4. Therefore,
258 the rest of the experiments using rice husk was performed at pH 6.

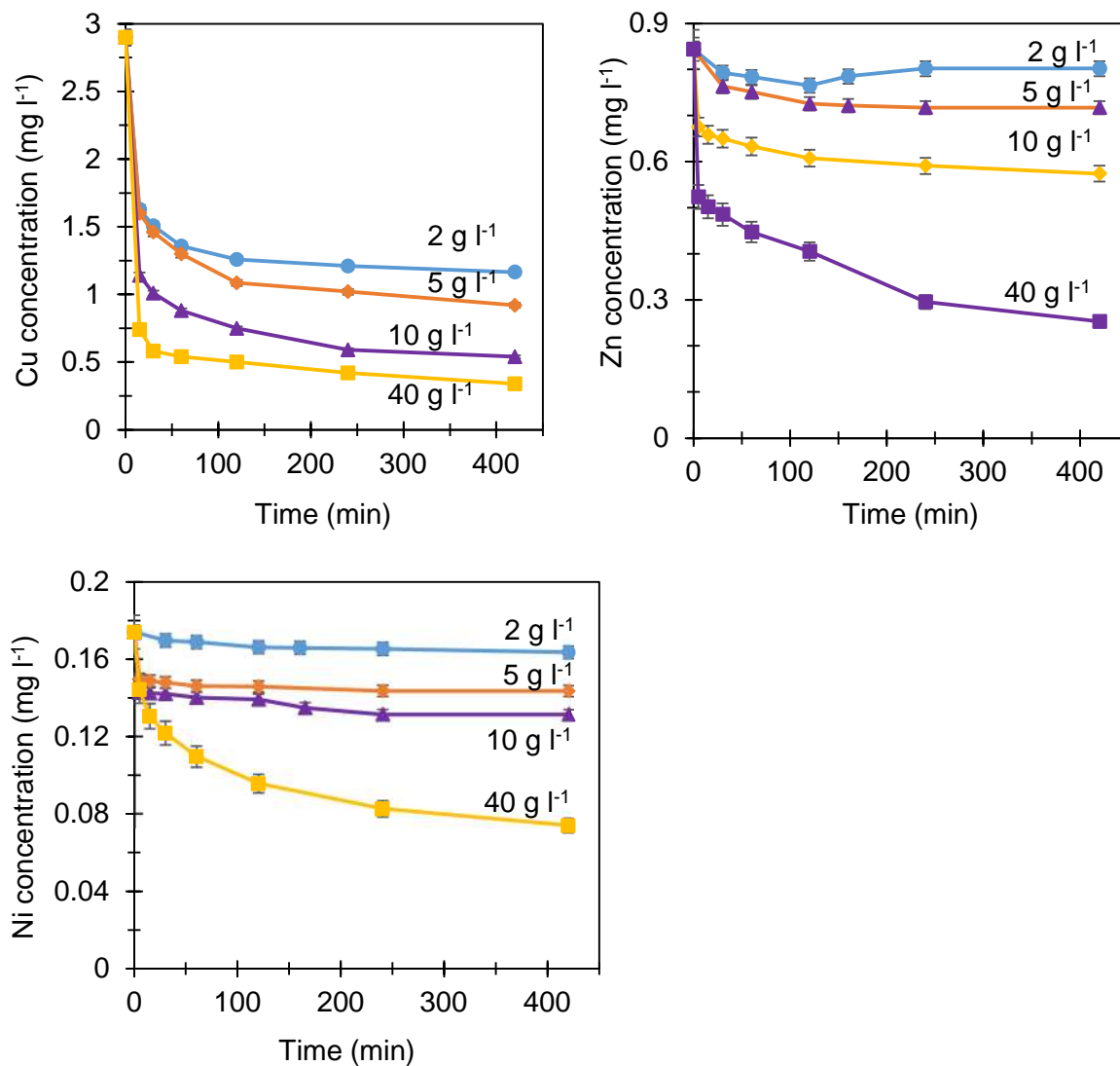


259

260 **Figure 1.** The effect of pH on the copper removal by precipitation and adsorption using rice
261 husk. (Rice husk amount=10 g l⁻¹, Temperature = 21 ± 3 °C, and initial Cu concentration = 2.9
262 mg l⁻¹, ± error < 2%).

263 Figure 2 shows the Cu, Zn and Ni concentrations in water as a function of contact time
264 at a range of rice husk dosages (2-40 g l⁻¹) at room temperature. The concentration of Cu and
265 Zn dropped drastically within the first 5-15 minutes. This can be attributed to the availability
266 of the abundant active sites on the surface of rice husk (Zhang et al., 2014). For all the rice
267 husk dosages investigated, the optimum contact time for Cu was observed approx. 2 hours as
268 the percentage removal did not increase significantly beyond this time (Fig 5). A maximum
269 removal percentage of Cu (98%) was achieved at 2 hour of contact time with 40 g l⁻¹ rice husk.
270 It is worth noting that around 75% of Cu was removed within the first 5 minutes using 40 g l⁻¹
271 rice husk. Although up to 70% of Zn was removed at 2 hour of contact time using 40 g l⁻¹ rice
272 husk, the saturation was reached after 6.7 hours. Removal percentage of Zn increased from 16
273 to 32, when 5 and 10 g l⁻¹ adsorbent used during the experiments. Approximately 98% of Ni

274 was removed using 40 g l⁻¹ of rice husk at pH 6 in 2 hours. Similarly, saturation was obtained
 275 ~ 7 h where up to 45% Ni was removed. These saturation times for Zn and Ni may suggest that
 276 adsorption of Zn and Ni on rice husk is slower than that of Cu.

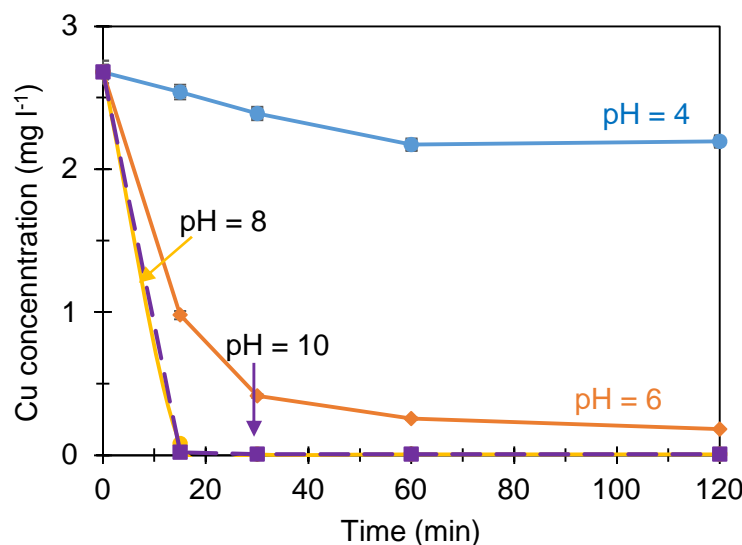


279 **Figure 2.** The concentrations of Cu, Zn and Ni in water as a function of time for rice husk
 280 dosages of 2-40 g l⁻¹ at pH 6 (\pm error < 5%).

281 The main factor contributing to the adsorption properties of the rice husk is the presence
 282 of silanol functional groups on its surface, which is related to its silica content that can reach
 283 up to 20 wt% (Ahmaruzzaman and Gupta, 2011). The porosity of the rice husk is low (Table
 284 3) and the main functional group present in the structure is Si-O-Si bonds as observed by FTIR
 285 spectra (Fig 3). Negative surface charge of rice husk is also one of the factors contributing to

286 adsorption of positively charged heavy metals on the surface. In addition to this, cellulose and
287 ligning components can also play role of the removal of the heavy metals [Rocha et al., 2009]

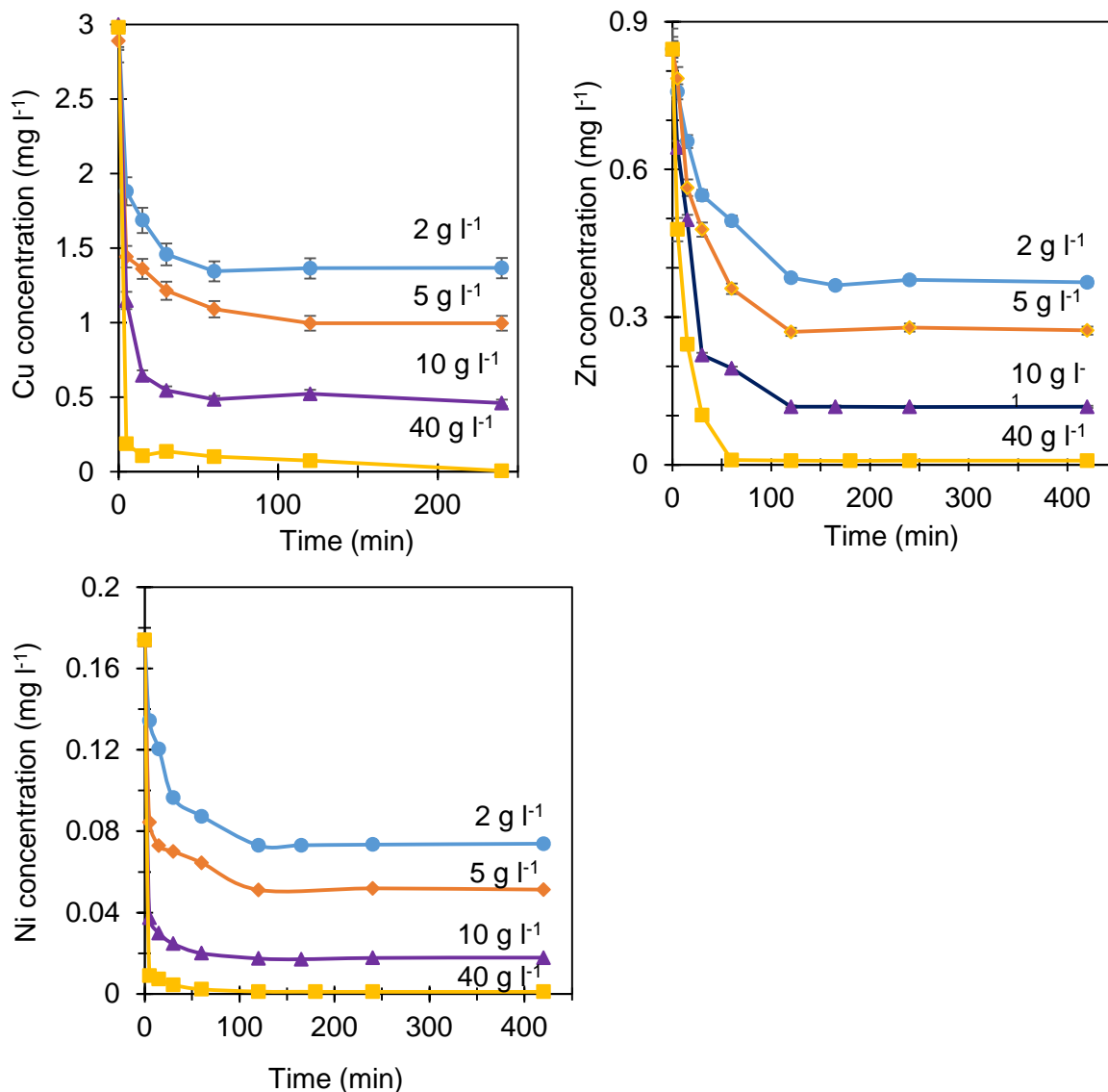
288 Figure 3 represents the removal of copper by adsorption and precipitation as a function
289 of pH using 10 g l^{-1} coconut coir for 2 hours. At pH 4, the copper concentration only decreased
290 to 2.25 mg l^{-1} (33% removal) while up to 92% of copper was removed at pH 6. The copper
291 concentration at pH 8 and 10 decreased below the detection limit (0.013 mg l^{-1}) of the ICP-
292 AES (Figure 6). These suggests that the copper removal using coconut coir significantly
293 increased at pH values > 6 due to the precipitation. Therefore, the rest of the adsorption
294 experiments of Cu on coconut coir were conducted at pH 6, showing the highest removal
295 efficiency of 92%. These observations coincide with the results published for copper adsorption
296 on coconut coir (Kadirvelu & Namasivayam, 2003) and the greater removal by adsorption and
297 predominantly by precipitation was observed at pH > 6 .



298
299 **Figure 3.** The effect of pH on the copper removal by adsorption and precipitation as a function
300 of time (Coconut coir amount= 10 g l^{-1} , initial concentration of Cu= 2.9 mg l^{-1} , \pm error $< 3\%$).

301 The uptake of copper increased when the coconut coir dose was increased in the range
302 of $2\text{-}40 \text{ g l}^{-1}$ (Figure 4). Most of the copper was removed within the first 5 minutes whilst
303 concentrations decreased until 2 h. Almost 85% of the copper in water was removed at pH 6,
304 using 10 g l^{-1} of coconut coir within 120 minutes. When the coconut coir concentration was

305 increased to 40 mg l⁻¹, the copper concentration dropped to 0.0065 mg l⁻¹. Unlike rice husk, 2
306 g l⁻¹ coconut coir can remove approx. 53% of all the heavy metals. Percentage removal are
307 similar to rice husk results for Zn (86%) and Ni (89%) using 10 g l⁻¹ of coconut coir. Up to
308 99% removal was achieved for all heavy metals when the coconut coir amount was increased
309 to 40 g l⁻¹. These results may indicate that Cu is adsorbed more by rice husk whilst coconut
310 coir adsorbs more Zn and Ni. The differences in surface area and functional groups affect the
311 adsorption properties of the biosorbents. The BET surface area and pore size of coconut coir
312 are approx. 2 times higher than rice husk. The functional groups that belong to cellulose in
313 coconut coir may also play a role during adsorption more than surface charges as both
314 biosorbents are expected to be negatively charged at pH 6.

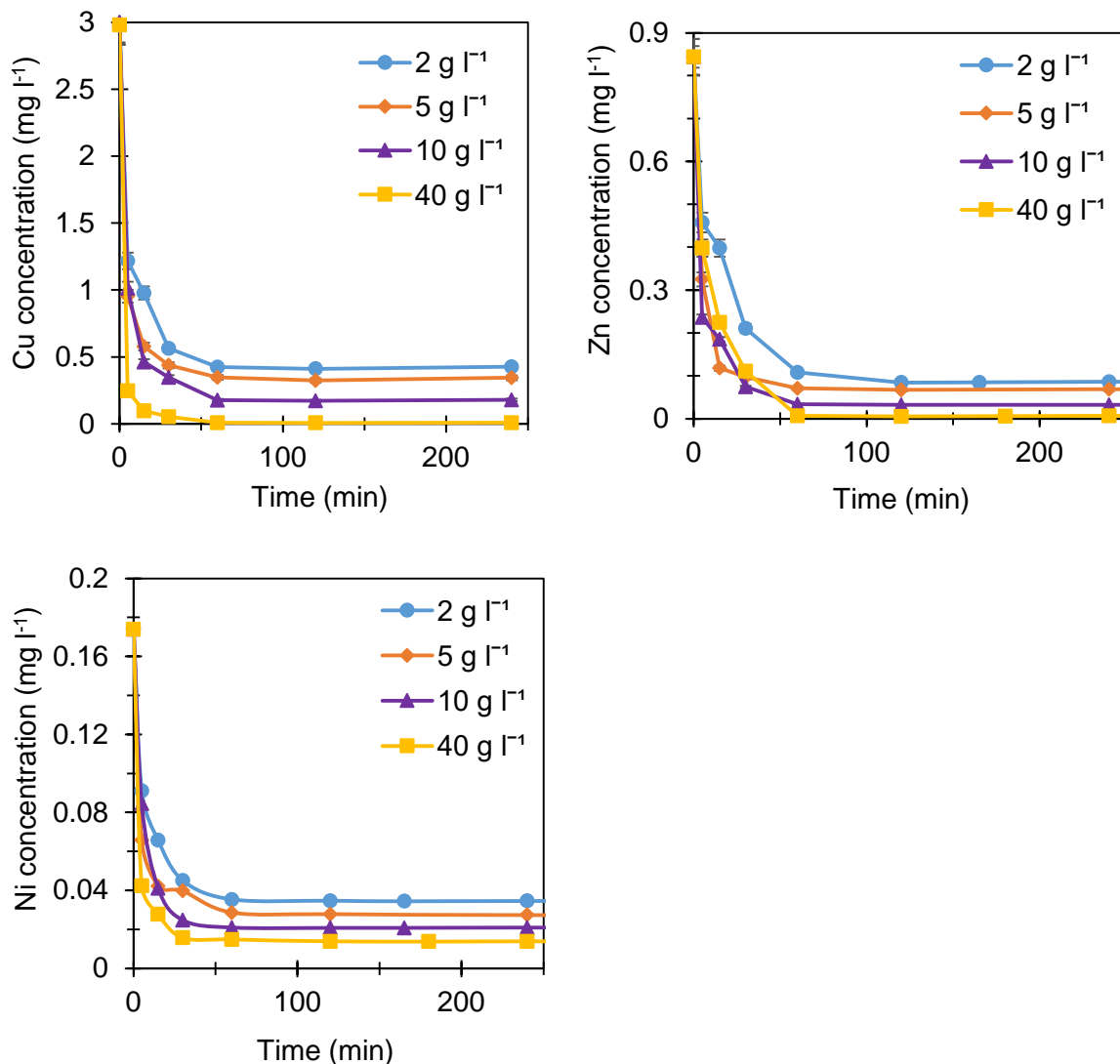


315

316

317 **Figure 4.** The concentrations of Cu, Zn and Ni in mixed heavy metal solution as a function of
 318 time for coconut coir amounts of 2-40 g l⁻¹ at pH 6 (\pm error < 5%).

319 The concentrations of Cu, Zn and Ni in mixed heavy metal solution as a function of
 320 time for moringa seeds are shown in Figure 5. Only 2 g l⁻¹ moringa seeds are sufficient to
 321 remove 90%, 85% and 80% of Zn, Cu and Ni, respectively, in 30 min. With increasing
 322 biosorbent dose (40 g l⁻¹), 99% removal was achieved for all heavy metals.



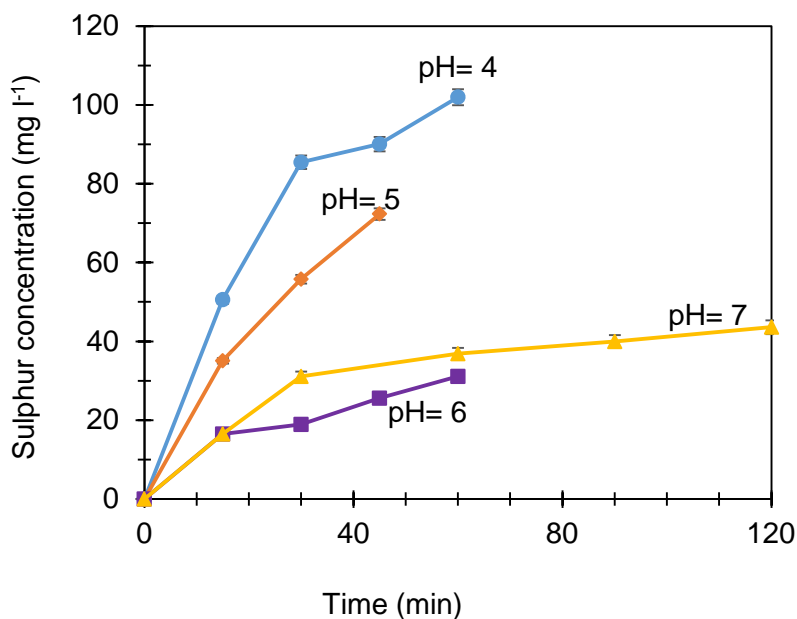
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324

325 **Figure 5.** The concentrations of Cu, Zn and Ni in mixed heavy metal solution as a function of
 326 time for moringa seeds amounts of 2-40 g l⁻¹ at pH 6 (\pm error < 5%).

327 These results may suggest that moringa seeds are convenient biosorbent for the removal
 328 of Zn, Cu and Ni without multi-element effect, mostly seen during adsorption processes.
 329 Regarding the FTIR spectra, moringa seeds contain more functional groups than the other two
 330 biosorbents used in this study. This may be the reason of better removal obtained. In addition
 331 to this Bhatti et al (2007) reported an optimal pH range (5-8) for heavy metal removal using
 332 moringa oleifera seeds. Similarly, Araújo et al (2010), showed 80, 60, 20% Zn, Cu and Ni
 333 removal efficiency, respectively at the pH range of 4-6.

334 A qualitative analysis of the treated water samples during the adsorption experiments
335 showed considerable amounts of sulfur being leached into the water (Figure 6). Due to the
336 potential health effects and colour and odour issues, sulfur leaching at various pH values were
337 further studied. The value of pH had a strong effect on the rate at which sulfur leached to the
338 aqueous solution, with higher acidity promoting the sulfur leaching. During the experiments,
339 the highest sulfur concentration ($100 \text{ mg l}^{-1} \pm 3$) was measured at pH 4. In contrast, for pH 6
340 and 7, the sulfur concentrations were approximately $40 \text{ mg l}^{-1} \pm 2$.



341
342 **Figure 6.** Increase in sulphur concentration as a function of time (pH=4-7, dosage= 5 g l^{-1}).

343 The leaching of sulfur from seeds may be attributed to the stronger competition between
344 H^+ ions and sulfur molecules at low pH values. No reporting of similar occurrences has been
345 published in literature; therefore, no data is available for comparison. There are no limits
346 imposed on elemental sulfur, sulfate or hydrogen sulphide in drinking water regulation.
347 However, the World Health Organisation reported that laxative effects of sulfate was observed
348 when water with concentrations of sulfate above 1000 mg l^{-1} was consumed (WHO, 2004). The
349 taste threshold is also indicated as 250 mg l^{-1} for sodium sulfate. Assuming most of the sulfur
350 detected by the ICP-AES instrument is present in water as sodium sulfate, the taste threshold

351 of 250 mg l⁻¹ corresponds to approximately 50 mg l⁻¹ of sulfur. As shown in Figure 6, the
 352 calculated threshold would not be exceeded when operating at pH 6 and 7, whereas for pH
 353 values of 4 and 5, the contact time will have to be limited at 30 minutes and 15 minutes,
 354 respectively.

355 **Adsorption kinetics of Cu, Zn and Ni**

356 To determine the adsorption kinetics of Cu, Zn and Ni using rice husk, coconut coir and
 357 moringa seeds, the samples were taken at specified times. Furthermore, the adsorbed amount
 358 values and the kinetic parameters were demonstrated using the linearized forms of the two
 359 kinetic models by fitting with the experimental data. As the pseudo-second order model best
 360 fitted the kinetic data ($R^2 > 0.99$) for all heavy metals using rice husk, coconut coir and moringa
 361 seed (Table 5). The first-order model produced low regression coefficients, indicating a weak
 362 correlation between this model and the experimental data. Therefore, only the results from the
 363 pseudo-second order model are presented in Table 5. These results are in agreement with the
 364 reports published in literature for rice husk (Zhang et al, 2014) and coconut coir (Shukla et al.,
 365 2006; Fu and Wang, 2011). The moringa seeds kinetic study has not published for the heavy
 366 metals investigated in this study. However, Kalavathy and Miranda (2010) reported that
 367 adsorption of Cu, Zn and Ni follow pseudo- second order kinetic model using moringa oleifera
 368 wood. Similarly, Ni adsorption on moringa oleifera seed husks followed pseudo-second order
 369 kinetics (Garcia-Fayos et al., 2015).

370 **Table 5:** Pseudo-second order model kinetic parameters for Cu, Zn and Ni adsorption on rice
 371 husk, coconut coir and moringa seeds at pH 6 using 5 g l⁻¹ biosorbent.,

Biosorbent	Metal ion & initial concentration (mg l ⁻¹)	k ₂ (g mg ⁻¹ min ⁻¹)	Q _{e (calc)} (mg g ⁻¹)	R ²
Rice husk	Cu, 3	0.19	0.41	0.9997
Coconut coir		0.6	0.38	0.9994
Moringa seeds		0.641	0.535	0.999

Rice husk	Zn, 0.844	6.57	0.0257	0.995
Coconut coir		0.0966	0.139	0.956
Moringa seeds		1.69	0.157	0.999
Rice husk	Ni, 0.174	12.3	0.0085	0.993
Coconut coir		12.6	0.0247	0.999
Moringa seeds		7.74	0.03	0.999

372 Moringa seeds exhibited the highest equilibrium capacities (Q_e) and pseudo-second
373 order rate constant (k_2) for Cu. Although the equilibrium capacities of Zn (0.157 mg g^{-1}) and
374 Ni (0.03 mg g^{-1}) were also the highest for moringa seeds, pseudo-second order rate constants
375 (k_2) for Zn and Ni were the highest when rice husk and coconut coir were used.

376 Studies have shown that adsorption behaviour that fits the second order kinetic model
377 well often can be explained by diffusion-based mechanisms. Therefore, adsorption kinetics of
378 cellulosic materials may mainly depend on diffusion-limited processes, as affected by
379 heterogeneous distributions of pore sizes and continual partitioning of solute species between
380 a dissolved state and a fixed state of adsorption, as discussed previously (Douven et al, 2015).
381 Alternatively, some studies concluded that the pseudo-second order model suggests either a
382 chemisorption or an ion-exchange mechanism, depending on the functional group of the
383 adsorbent (Blanchard et al., 1994). Since these biosorbents have low BET surface area (Table
384 3), in order words not very porous, diffusion of heavy metals may be critical only in the solution
385 while they are attracted to the surface of biosorbent through weak Van der Waal's forces
386 (electrostatic attraction). Rudi et al., 2020 suggested that the chemical bonds between the metal
387 ions and the rice husk surface occurred during adsorption. Therefore, Ahmaruzzaman and

388 Gupta (2011) emphasised the importance of improving the properties of the rice husk surface
 389 since the adsorption properties of the material could be enhanced.

390 **Adsorption isotherm models**

391 Langmuir model well-fitted the adsorption data obtained for 3 heavy metal ions using
 392 rice husk, coconut coir and moringa seeds since regression coefficients (R^2) are in the range of
 393 0.98-0.99 (Table 6). Freundlich model was also applied in describing adsorption isotherms for
 394 Cu, Zn and Ni that fit with lower regression coefficients ($R^2= 0.88-0.90$) and thus was not
 395 shown in Table 6.

396 **Table 6:** Langmuir adsorption isotherm model parameters for Cu, Zn and Ni using rice husk,
 397 coconut coir and moringa seeds as biosorbents. Adsorbent dose: 40 g l⁻¹, Heavy metal
 398 concentration: 1-150 mg l⁻¹, pH=6

Biosorbent	Parameter	Cu	Zn	Ni
Rice husk	q_{max} (mg g ⁻¹)	1.56	0.89	0.64
	b (l mg ⁻¹)	3.7	24.0	65.8
	R^2	0.9986	0.9878	0.9966
Coconut coir	q_{max} (mg g ⁻¹)	1.34	1.53	2.6
	b (l mg ⁻¹)	17.1	11.9	29.4
	R^2	0.9578	0.9791	0.9899
Moringa seeds	q_{max} (mg g ⁻¹)	23.3	42.3	16.1
	b (l mg ⁻¹)	0.11	0.12	0.1
	R^2	0.9945	0.9901	0.9932

399 The adsorptive capacities (q_{max}) of all three heavy metals for rice husk in this study is
 400 similar, compared to the other reports in literature, including the Langmuir adsorption model
 401 (Marshall et al., 1993; Araújo et al., 2010). Rice husk adsorbs 1.75 and 2.74 times more Cu
 402 than Zn and Ni, respectively. Maximum sorption capacity (q_{max} , Table 6) suggests the
 403 following order for metal ion selectivity for rice husk: Cu > Zn > Ni. In contrast, Zn is adsorbed
 404 1.8 and 1.2 times more than Cu for coconut coir and moringa seeds, respectively. Although Ni
 405 is the least adsorbed by coconut coir and moringa seeds, the max adsorption capacities observed
 406 using coconut coir and moringa seeds are 4 and 25 times higher than the one obtained for rice
 407 husks, respectively. The adsorption selectivity for coconut coir and rice husk is Zn > Cu > Ni.

408 The adsorption capacities and models (Langmuir) for coconut coir are similar to studies
409 reported in literature. However, in some studies, Ni adsorption capacity (2.51 mg g^{-1}) is higher
410 than adsorption capacity of Zn (1.83 mg g^{-1}) for coconut coir. This may be resulted from the
411 other additional heavy metal ions in the solution or the type/source of the biosorbents used. In
412 multi-element solutions, there may be a decrease in adsorption ability of specific heavy metals
413 due to the competitive adsorption (Sharma et al., 2007). Therefore, adsorption capacity and
414 model comparisons with literature may not be representative since there is no study in
415 literature, reporting the selected mixed heavy metals and metal concentrations without
416 biosorbent modification, similar to our study. Moringa seeds showed the highest adsorption
417 capacity for all heavy metals. However, the binding energies (represented by b) for heavy
418 metals were the highest for rice husk and coconut coir.

419 In this study, moringa seeds showed approx. an order of magnitude higher adsorption
420 capacities for Cu, Zn and Ni, compared to rice husk and coconut coir, under the same
421 experimental conditions. This may suggest that the functional groups, such as O-H, C-N, N-H
422 and C-O, which moringa seeds contain, play a role during adsorption process by either
423 developing electrostatic forces or complexation between groups and heavy metal ions. Swelam
424 et al (2018) compared the FTIR spectra of the moringa seeds before and after adsorption of
425 lead and observed significant shift or no difference in some peak positions of those functional
426 groups. Similarly, Maina et al (2016) also reported shifts or changes in the peak positions and
427 intensities in the FTIR spectra after heavy metal (lead, cadmium, iron, zinc, magnesium and
428 manganese) adsorption on moringa oleifera tree. The shifting in the peak positions and intensity
429 in the spectra, after lead adsorption, can be a proof for the participation of those specific groups
430 in adsorption process.

431 In addition to this, cation selectivity of a biosorbent can be influenced by electrostatic
432 attraction (influenced by hydrated radius), cation charge and enthalpy of hydration and

433 complex and precipitate formation (Hendricks, 2016). Effects of cation charge and complex
434 and precipitate formation were dismissed as all metals are divalent (same charge) and
435 experiments were performed at pH 6 to prevent the influence of precipitation. Surface charges
436 of the biosorbents are negative and in the same region for all biosorbents. Therefore, the
437 percentage of removal for metal ions may also be explained by the difference in hydrated
438 radius. Reports in literature show that in general, the greater the atomic weight,
439 electronegativity, and ionic size, the greater will be the affinity for sorption (Mattuschka and
440 Straube, 1993). Among the metals tested, Cu (0.419 nm) and Zn (0.430 nm) (Ouki and
441 Kavannagh, 1997; Oter and Akcay, 2007) present larger ionic radius and hence higher
442 adsorption capacity unlike the Ni (0.404 nm) (Mobasherpour et al., 2012), which presents lower
443 adsorption capacity (Araújo et al., 2010).

444 **Conclusion**

445 We demonstrated the successful removal of Cu, Zn and Ni from contaminated water,
446 using rice husk, coconut coir and moringa seeds. without modification. For the first time, the
447 performance of these biosorbents were analysed under the same conditions. Heavy metals were
448 removed up to 99% using 40 g l⁻¹ biosorbents at pH 6, without precipitation. The highest
449 adsorption capacities (Cu= 23.3 mg g⁻¹, Zn= 42.3 mg g⁻¹ and Ni= 16.1 mg g⁻¹) were observed
450 using moringa seeds, followed by rice husk and coconut coir. Adsorption isotherms and
451 kinetics fitted Langmuir and Pseudo-second order models for all biosorbents.

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455 to characterisation instruments. We thank Dr Athil Al-Shihabi Al-Ani and Mrs Tasneem
456 Muhammed for FTIR and XRF characterisations, respectively.

457 **Appendix A. Supplementary Materials**

458 Supplementary Data.

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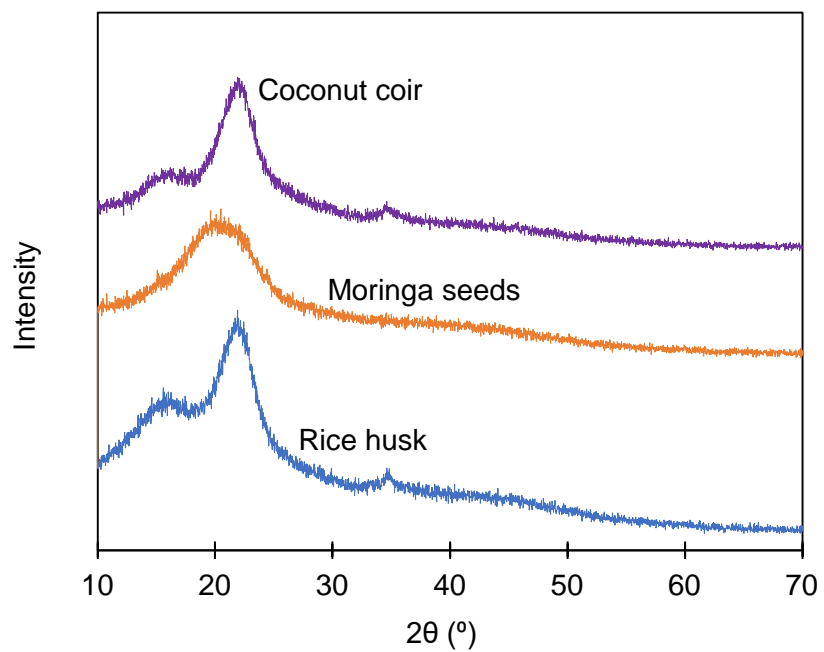
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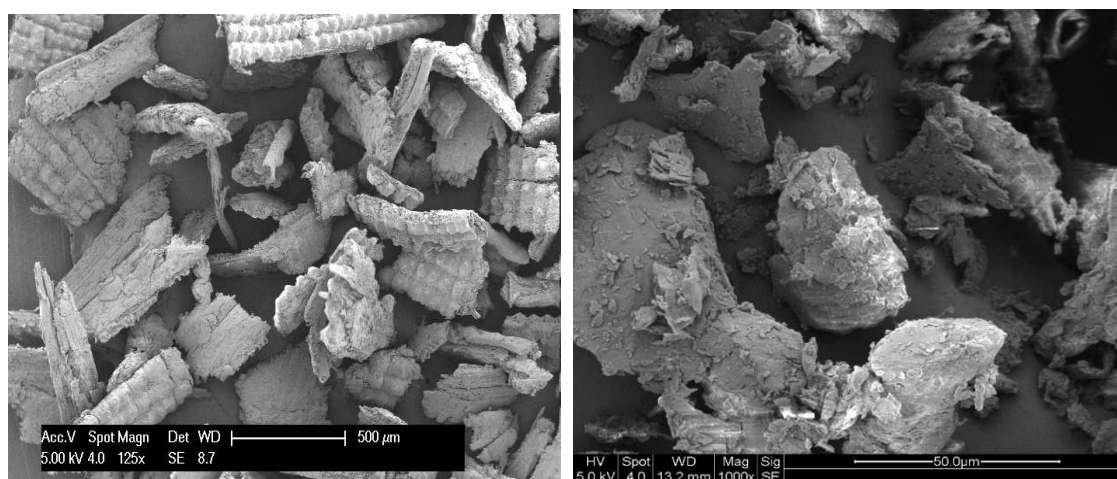
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596 *Res Int*, 2014, 496878-496886.

597 598 **Supplementary Materials**

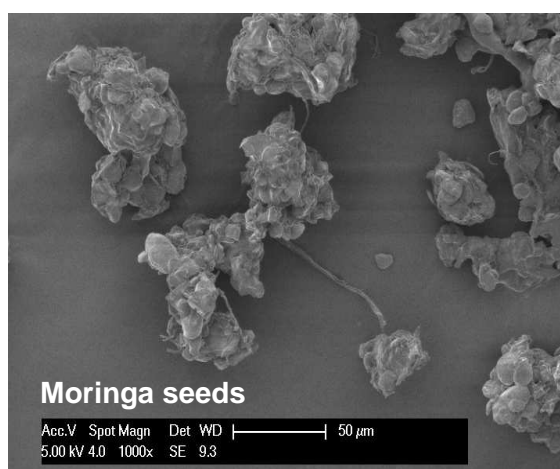


599

600 **Figure S1.** XRD patterns of rice husk, coconut coir and moringa seeds.

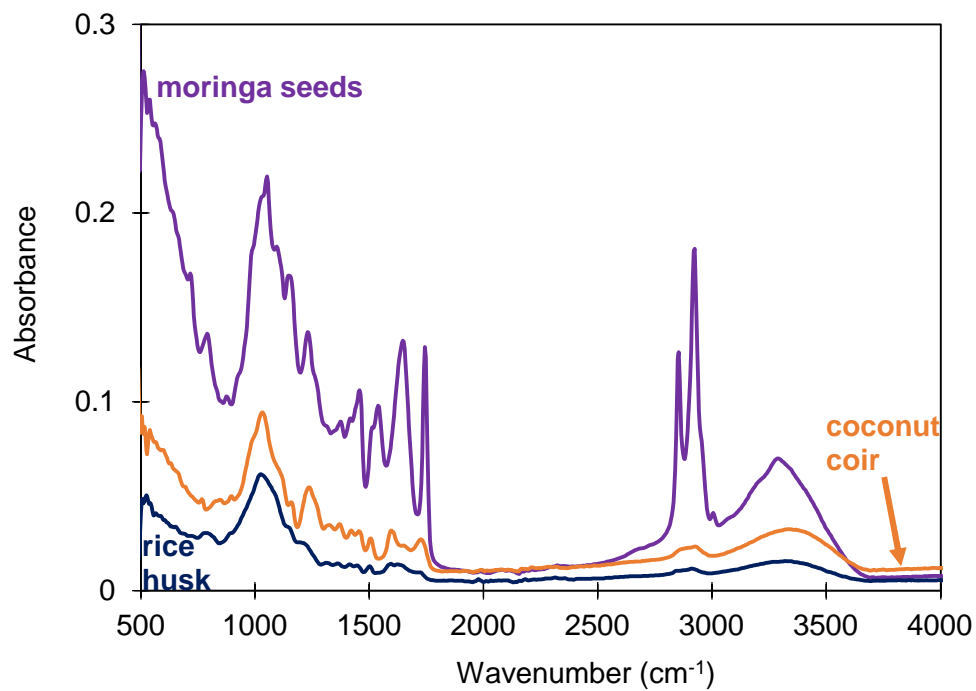


601



602

603 **Figure S2.** SEM images of rice husk, coconut coir and moringa seeds.



604

605 **Figure S3.** FTIR spectra of rice husk, coconut coir and moringa seeds obtained between 500-
606 4000 cm⁻¹.