Performance assessment of a membrane liquid desiccant dehumidification cooling system based on experimental investigations

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Abstract

A membrane-based liquid desiccant dehumidification cooling system is studied in this paper for energy efficient air conditioning with independent temperature and humidity controls. The system mainly consists of a dehumidifier, a regenerator, an evaporative cooler and an air-to-air heat exchanger. Its feasibility in the hot and humid region is assessed with calcium chloride solution, and the influences of operating variables on the dehumidifier, regenerator, evaporative cooler and overall system performances are investigated through experimental work. The experimental results indicate that the inlet air condition greatly affects the dehumidification and regeneration performances. The system regeneration temperature should be controlled appropriately for a high energy efficiency based on the operative solution concentration ratio. It is worth noting that the solution concentration ratio plays a considerable role in the system performance. The higher the solution concentration ratio, the better the dehumidification performance. However simultaneously more thermal input power is required for the solution regeneration, and a crystallization risk in the normal operating temperature range should be noted as well. The system mass balance between the dehumidifier and regenerator is crucial for the system steady operation. Under the investigated steady operating condition, the supply air temperature of 20.4°C and system COP of 0.70 are achieved at a solution concentration ratio of 36%.

Keywords: Liquid desiccant dehumidification, Membrane-based, Evaporative cooling, Experimental study, System mass balance

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Nomenclature

Symbols

c_p	Specific heat capacity (J/kg·K)
C_{sol}	Desiccant solution concentration
h	Specific enthalpy (J/kg)
$\dot{m}$	Mass flow rate (kg/s)
m_{float}	Flow meter float weight (kg)
$\dot{M}_a$	Mass addition rate (g/s)
$\dot{M}_r$	Mass removal rate (g/s)
P	Pressure (Pa)
$\dot{Q}_{cooling}$	System total cooling output (W)
$\dot{Q}_{DH\_cooling}$	Dehumidifier cooling output power (W)
$\dot{Q}_{RE}$	Regenerator thermal input power (W)
T	Temperature (°C)
T_{wb}	Wet bulb temperature (°C)
T_{w_f}	Hot water supply temperature (°C)
T_{w_r}	Hot water return temperature (°C)
U_X	Measured variable uncertainty
U_Y	Calculated variable uncertainty
v	Volumetric flow rate (L/min)
$\overline{V}$	Average air velocity (m/s)
V_{float}	Flow meter float volume (m³)
X_i	Measured variable

Y   Calculated variable

Greek letters

ε_{DH} Dehumidification effectiveness

ε_{EV} Evaporative cooling effectiveness

ρ Density (kg/m^3)

ω Humidity ratio of air flow (kg/kg$_{\text{dryair}}$)

Subscripts

air   Air

eq   Equilibrium condition

in   Inlet

out   Outlet

S   Saturation

sol   Solution

w   Water

Abbreviations

COP   Coefficient of performance

DH   Dehumidifier

EV   Evaporative cooler

LDD   Liquid desiccant dehumidification

LDDC   Liquid desiccant dehumidification cooling

MLDD   Membrane-based liquid desiccant dehumidification

MLDDC   Membrane-based liquid desiccant dehumidification cooling

RE   Regenerator

1. Introduction

In the hot and humid region, air conditioning plays an important role in handling both sensible and latent cooling loads. The main design criteria for air conditioning systems are thermal comfort, indoor air quality, energy efficiency and associated environmental effect [1]. Mechanical vapour compression is the most common applied technology, in which dehumidification is accomplished by cooling air to the dew point temperature, and consequently extra energy is consumed to reheat the airstream for the desired supply temperature [2]. It has been reported that energy consumption of an air conditioning system exceeds 50% of the total energy usage of a building in the hot and humid climate [3]. On the other hand, the associated risks of mechanical vapour compression system such as leakage, bacterial breeding, and fungi due to water condensation on the cooling coil surface, have been noticed with prominent effects on indoor air quality and occupants' health. To address the drawbacks, many innovative dehumidification cooling systems have been developed with efficient independent temperature and humidity controls and simultaneously less energy consumption. Desiccant cooling has been regarded as one of the environmental-friendly air conditioning approaches without overcooling and reheating problems [4]. In theory, desiccants which are classified into solid and liquid materials, remove moisture from an airstream through natural sorption process. Compared with the solid desiccant system, the liquid desiccant dehumidification (LDD) system has been a more promising and economical choice due to its flexibility in utilizing low-grade energy sources [5] and capability of independent humidity and temperature controls [6]. Moreover, the LDD system is capable to provide high quality supply air as liquid desiccants can filter the bacteria, microbial contaminations, viruses and moulds [7]. In terms of energy conservation, 19% reduction in the annual primary energy consumption could be achieved with an LDD system for an office building in Miami, Florida [8]. Regarding

to the economical aspect, 40% of the operation cost can be saved with an LDD system compared to a conventional air conditioning system [9].

Generally, the LDD system performance is influenced by many factors, including liquid desiccant characteristic, packing type and operating condition [10]. For the selection of a liquid desiccant, several parameters should be considered, such as boiling point elevation, energy storage density, regeneration temperature, thermo-physical property, availability and cost [11]. Halide salts are the most commonly selected desiccants, for instance lithium chloride (LiCl), lithium bromide (LiBr) and calcium chloride ($CaCl_2$). Among them, LiCl is mostly preferred due to its favourable equilibrium water vapour pressure in the dehumidification process [12]. Nonetheless, LiCl solution usually crystallizes at large vapour pressure depression [13]. On the other hand, $CaCl_2$ is regarded as the cheapest and most readily available desiccant. Better mass transfer potential in the regeneration process is obtained with $CaCl_2$ solution compared to LiCl solution under the same operating condition [14]. Besides, weak organic acid salts such as potassium and sodium formate are good alternatives [7] and ionic liquids become promising for the specific achievable dew point temperature at a comparatively lower driving temperature [13]. With respect to the regeneration of liquid desiccant solution, it can be performed by either heating dilute solution or inlet air to the required regeneration temperature. By comparison, heating dilute solution is proved to be more efficient in the solution regeneration process [15].

The LDD packing arrangement is another critical factor influencing the dehumidification performance [16]. The available packing types are namely, wetted wall, spray tower, packed column and membrane-based, which provide the solution and air flow in different patterns including parallel, counter and cross flows. The wetted wall, spray and packed towers have been popular options for the dehumidification purpose [17]. However, these direct contact packing types have a major problem of liquid desiccant droplet carryover, which could be

harmful to occupants' health, building structure and indoor equipment [18]. To eliminate this problem, a membrane-based liquid desiccant dehumidification (MLDD) system is adopted, which involves an indirect contact process for dehumidification. Membranes acting as selective barriers allow heat and moisture transfers between the solution and airstream but prevent the carryover of liquid desiccant solution into the supply airstream [18]. Membranes are categorized into dense and porous types depending on the pore dimension. The dense membrane is hydrophilic for vapour transportation, while the porous membrane with a more open volume and larger pores is hydrophobic [19]. With respect to the form, membranes can be constructed as flat sheets with a simple structure and easy fabrication, or hollow fibres with a large packing density and high effectiveness but a more complex design.

A liquid desiccant dehumidification cooling (LDDC) system is defined as a hybrid air conditioning system combining a liquid desiccant dehumidification unit to handle the latent cooling load and a cooling unit to deal with the sensible cooling load [20]. A variety of cooling technologies can be integrated with the LDD system, such as vapour compression, vapour absorption and evaporative cooling. Among them, the evaporative cooling system has been widely applied because of its lower installation and running costs [21]. Compared with a vapour compression air conditioning system, the reduction in energy consumption of an evaporative cooler is over 75% [22]. Generally, the evaporative cooling is classified into direct and indirect types. The effectiveness of the direct evaporative cooling system is in the range of 70% to 90%, while the effectiveness ranges only from 40% to 60% for the indirect system. The direct evaporative cooling system adds moisture to the cooled supply air, whereas the indirect evaporative cooling system provides only sensible cooling to the supply air without any moisture being added, which is more preferred in the humid climate [23].

The selection of an evaporative cooling unit for an LDDC system depends on climate condition, supply air demand, cost and etc. The feasibility of an LDDC system with an indirect evaporative cooling unit is evaluated by experimental work in [24], in which the indoor air temperature reduces from 33.8°C to 22.3°C and the relative humidity decreases from 68.6% to 35.5%. With the similar design concept, a drop of 7.5°C in the indoor air temperature is achieved in [25]. In response to the climate condition and air conditioning requirement in Hong Kong, a hybrid liquid desiccant air conditioning system is developed by integrating both direct and indirect evaporative cooling means [26], whose performance is investigated by theoretical modelling. The LDDC system with an evaporative cooling unit is proved with remarkable energy and cost saving potentials [27]. By installing an evaporative-cooling assisted LDDC system for an open office building in Seoul, South Korea, 12% saving of the annual primary energy consumption could be achieved compared with the conventional air conditioning system [28]. More than 50% of the lifetime operating cost can be saved with an LDDC system compared to the conventional air conditioning system in Singapore [29]. By utilizing renewable energy in the regeneration process, the LDDC system can be more sustainable and economical, for example the abundant solar energy. Not only solar thermal but also photovoltaic technologies can be integrated into a solar-assisted LDDC system [30]. The feasibility of a membrane-based liquid desiccant dehumidification cooling (MLDDC) system powered by solar thermal energy is proved in [31]with significant economic and environmental benefits.

The MLDDC system has been widely explored through modelling and simulation. For instance, a comprehensive model of a parallel-plate MLDDC system is developed to address the features of the conjugate heat and mass transfer in [32]. Various approaches of integrating an evaporative cooling unit into the MLDDC system result in different system designs and configurations. To overcome the LDDC system shortcomings of complexity and large geometrical size, a compact membrane-based air conditioning system is developed with an

evaporative inter-cooler unit for building application in [33], whose cooling output is in the range of 570W to 1362W and the dehumidification effectiveness is in the range of 30% to 37% based on the experimental results.

Extensive experimental and theoretical studies have been conducted to investigate the effects of various parameters on the LDDC system performance. For example, the most significant dimensionless parameters affecting the dehumidification performance are identified through theoretical analyses [8, 34], which are NTU, solution to air thermal capacity ratio and solution concentration ratio. On the other hand, the experimental investigations in [35-37] demonstrated that the LDDC system dehumidification performance evidently varies with inlet air condition, solution concentration ratio and packing material density. However, limited researches have been carried out to evaluate the effects of operating variables on the MLDDC system performance by experimental work. In this study, a novel MLDDC system is proposed for experimental investigations. The system is featured:

a. Independent controls in the supply air temperature and humidity are achieved in the hot and humid climate without overcooling, reheating and water condensation problems.

b. The carryover problem of desiccant solution droplet into airstream is avoided by adopting the semi-permeable micro porous membranes in both the dehumidifier and regenerator units.

c. An indirect approach is employed to handle the sensible cooling load, where heat transfer takes place between the cool airstream from the direct evaporative cooling unit and the dehumidified airstream.

d. Low-grade heat sources could be utilized to regenerate the liquid desiccant (e.g. in a temperature range of 50.0°C to 80.0°C for $CaCl_2$).

The system feasibility and performance are evaluated under various operating conditions. The influences of inlet air condition, desiccant solution concentration ratio, hot water and cold water temperatures on the system dehumidification, regeneration, evaporative cooling and overall performances are investigated experimentally.

2. Experimental Set-up

2.1 System description

The proposed MLDDC system mainly consists of four components: a dehumidifier, a regenerator, an evaporative cooler and an air-to-air heat exchanger, in which four processes are involved as illustrated in Fig. 1:

a. Dehumidification process: the outdoor hot and humid air is dehumidified by liquid desiccant solution in the dehumidifier;

b. Regeneration process: the indoor return airstream passes through the regenerator and absorbs moisture from the dilute desiccant solution;

c. Direct evaporative cooling process: the evaporative cooler lowers the indoor return air temperature through water evaporation;

d. Sensible cooling process: the airstream from the evaporative cooler is used to cool the dehumidified air to meet the desired supply air requirement in the air-to-air heat exchanger.
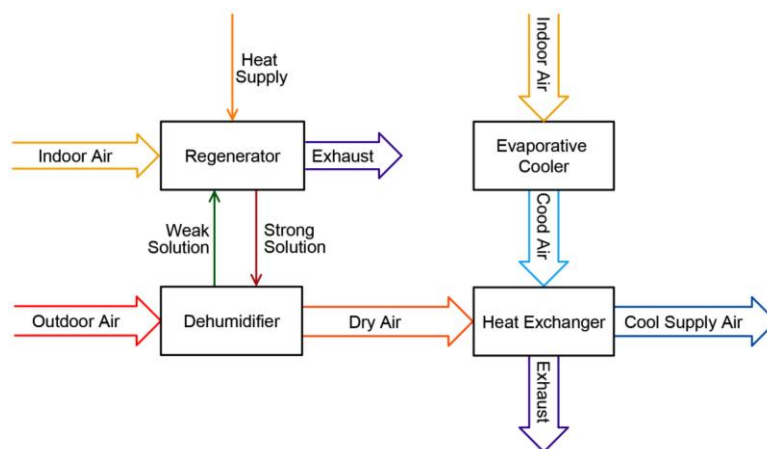
Fig. 1. Block diagram of the MLDDC system

A labelled schematic diagram of the experimental set-up is presented in Fig. 2. A 3kW boiler is used to provide hot water for the regeneration purpose. Three AC axial fans are fitted in the dehumidifier, regenerator and evaporative cooler respectively. Two 15W single phase magnetic-driven pumps are used to circulate the regenerated and dilute desiccant solutions. A liquid-to-liquid heat exchanger (HX2) allows heat recovery between the two solutions. In order to enhance the dehumidification performance, cold water is utilized to cool the regenerated solution prior to flowing into the dehumidifier. Ball valves (V1, V2, V3, and V4) are installed to control the desiccant solution and water flow rates.
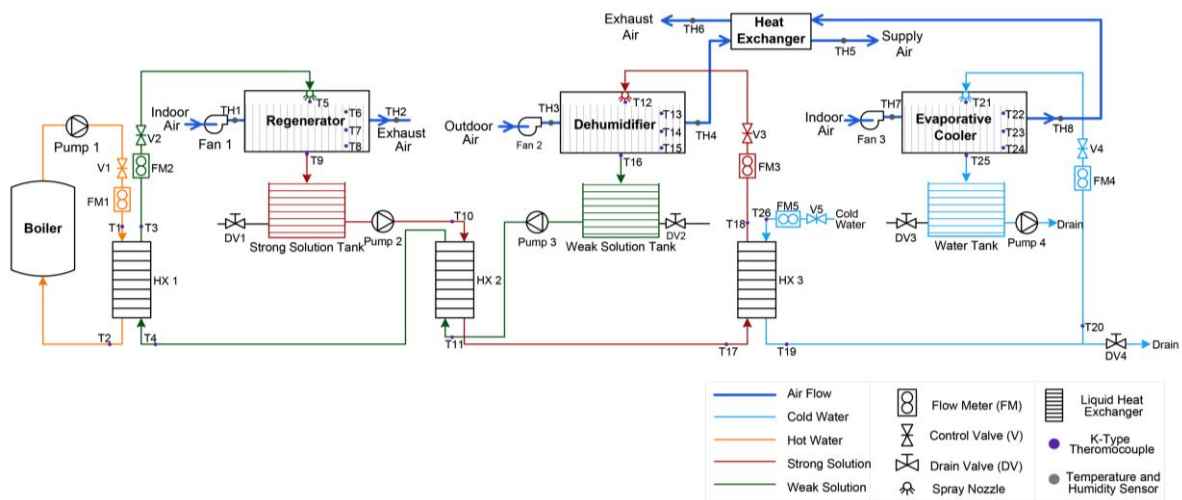
Fig. 2. Schematic graph of the MLDDC system

Aqueous $CaCl_2$ is selected as the liquid desiccant solution. Photos of the experimental rig are shown in Fig. 3. An environmental chamber is employed to provide inlet air for the dehumidifier unit, which is capable to simulate the hot and humid climate condition. On the other hand, an air conditioner is used to supply air for the regenerator and evaporative cooler. With consideration of the surrounding effect, components such as air ducting, pipe work and heat exchangers are well insulated.
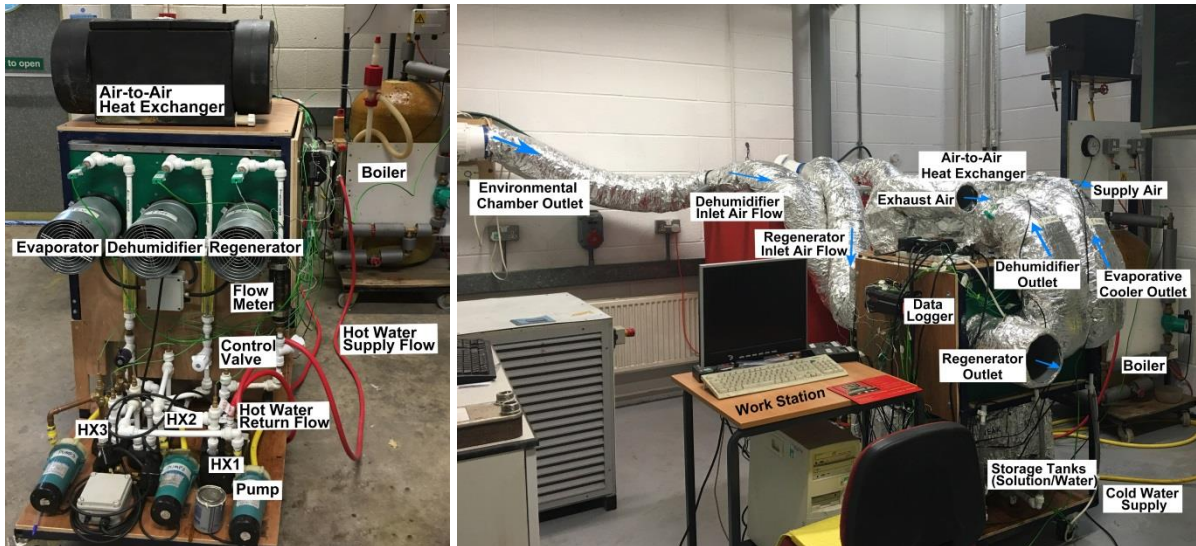
Fig. 3. Photos of the MLDDC system test rig

2.2 Membrane-based unit

Both the dehumidifier and regenerator are membrane-based units with specifications listed in Table 1. The evaporative cooler has the same dimensions as the membrane-based unit, whereas its air channels are formed only by fibre sheets, which provide wet surfaces for water evaporation.

Table 1. Membrane-based unit specifications

Unit dimension	Length	410mm
	Width	230mm
	Height	210mm
Membrane thickness	0.11mm	
Air channel barrier thickness	0.13mm	
Solution channel	Quantity	21
	Width	4.30mm
Air channel	Quantity	21
	Width	7.73mm

The membrane-based unit has a series of separate channels in the cross-flow manner for the airstream and desiccant solution, as depicted in Fig. 4. The semi-permeable micro-porous hydrophobic membranes allow heat and moisture transfers between the airstream and desiccant solution while the liquid desiccant cannot permeate. Each solution channel is formed by two flat membrane sheets. During operation, the desiccant solution passes through the permeable

barrier on the top and then flows downwards in the solution channels. Simultaneously, the gap between two solution channels allows the airstream to pass through for dehumidification or regeneration, where fibre materials are added only as supporting barriers.
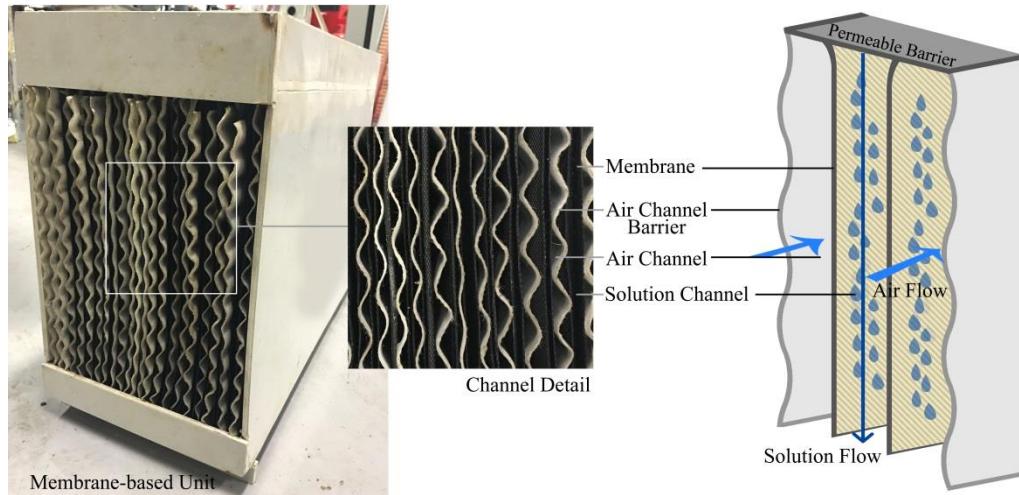

Fig. 4. Illustration of the membrane-based unit

2.3 Measurement method

The main measurement devices with their associated accuracies are presented in Table 2. A Testo anemometer is used to measure air velocity. Air temperatures and relative humidity at inlets and outlets of the dehumidifier, regenerator, evaporative cooler and air-to-air heat exchanger are obtained by Sensirion humidity sensors. K-type thermocouples are instrumented to measure the desiccant solution and water temperatures, and a data acquisition system is employed to record the data during operation.

Table 2. Measurement devices with associated accuracies

Instrument	Parameter	Measurement Range	Accuracy
Testo thermo-anemometer	Air velocity	0-10 m/s	±5%
Sensirion humidity sensor	Air temperature	-40 - +125°C	±0.3%
	Air relative humidity	0 - 100%	±2%
K-type thermocouple	Liquid temperature	0-1100°C	±0.75%
Data logger DT500	Data Acquisition		±0.15%
Brannan hydrometer 200 Series	Solution density	1.0-1.6 g/m^3	±2%
Parker Easiflow meter	Liquid flow rate	1-15 L/min	±5%
Parker liquid flow indicator	Liquid flow rate	4-22 L/min	±2%

The solution concentration ratio (C_{sol}) is a function of the solution density and temperature, which is expressed as [38]:

$$\rho_{sol}(C_{sol}, T_{sol}) = \rho_w(T_{sol}) \cdot [1 + 0.836014 \cdot (\frac{C_{sol}}{1-C_{sol}}) - 0.4363(\frac{C_{sol}}{1-C_{sol}})^2 + 0.105642(\frac{C_{sol}}{1-C_{sol}})^3] \quad (1)$$

where, T_{sol} and ρ_{sol} are solution temperature in °C and density in kg/m^3 respectively. The solution density is measured by a Brannan hydrometer. ρ_w is saturated water density at T_{sol}, in kg/m^3.

Desiccant solution and water volumetric flow rates are measured by Parker liquid flow meters, which are calibrated with water at 20°C. To equate the volumetric flow rate readings from the installed flow meters to the actual solution flow rates in the dehumidifier and regenerator, a correction correlation is used [39]:

$$v_{sol} = v_w \sqrt{\frac{(m_{float} - V_{float}\rho_{sol})\rho_w}{(m_{float} - V_{float}\rho_w)\rho_{sol}}} \quad (2)$$

where, v_{sol} and v_w are volumetric flow rates of the desiccant solution and water respectively, in L/min. m_{float} and V_{float} are flow meter float weight in kg and volume in m^3 respectively.

Once the desired inlet conditions for the three units are achieved, the entire system runs continuously until the steady state is reached and then the measured data is collected with a computer.

2.4 Uncertainty analysis

The uncertainty of each measurement instrument is listed in Table 2. Analysis is carried out to correlate the uncertainty of a calculated variable. The uncertainty U_Y of a variable Y can be derived from the function of uncertainty U_{X_i} of each measured variable X_i [40].

$$U_{\mathrm{Y}} = \sqrt{\sum_{i=1}^{N} (\frac{\partial Y}{\partial X_i})^2 \cdot U_{\mathrm{X}_i}{}^2} \tag{3}$$

Error bars associated with the respective uncertainties are provided in the result analysis section.

3. Performance Evaluation Metrics

In terms of the dehumidification performance, it is evaluated by the moisture removal rate ($\dot{M}_{\mathrm{r}}$), and dehumidification effectiveness ($\varepsilon_{\mathrm{DH}}$) which is defined as the ratio of the actual change in moisture content to the maximum moisture transfer.

$$\dot{M}_{\mathrm{r}} = \dot{m}_{\mathrm{air\_DH}} \cdot (\omega_{\mathrm{in\_DH}} - \omega_{\mathrm{out\_DH}}) \tag{4}$$

$$\varepsilon_{\mathrm{DH}} = \frac{\omega_{\mathrm{in\_DH}} - \omega_{\mathrm{out\_DH}}}{\omega_{\mathrm{in\_DH}} - \omega_{\mathrm{eq\_DH}}} \tag{5}$$

where, $\dot{m}_{\mathrm{air\_DH}}$ is mass flow rate of the airstream passing through the dehumidifier in kg/s, $\omega_{\mathrm{in\_DH}}$ and $\omega_{\mathrm{out\_DH}}$ represent air humidity ratios at the dehumidifier inlet and outlet respectively, in kg/kg$_{\mathrm{dryair}}$, which are calculated based on the measured air temperature and relative humidity [41]. $\omega_{\mathrm{eq\_DH}}$ is equilibrium humidity ratio of the desiccant solution at the inlet condition, in kg/kg$_{\mathrm{dryair}}$. Referred to the empirical correlation derived in [42], a psychrometric chart illustrating the correlation of CaCl$_2$ solution equilibrium humidity ratio with concentration ratio and temperature is presented in Fig. 5.
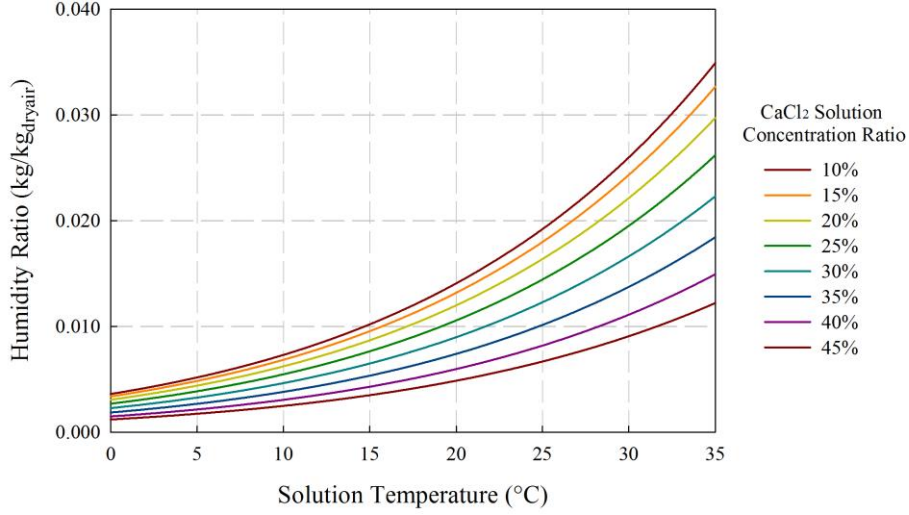
Fig. 5. CaCl₂ solution equilibrium humidity ratio with concentration ratio and temperature

The regeneration performance is assessed by the moisture addition rate ($\dot{M}_a$).

$$\dot{M}_a = \dot{m}_{air\_RE} \cdot (\omega_{out\_RE} - \omega_{in\_RE}) \tag{6}$$

where, $\dot{m}_{air\_RE}$ is air mass flow rate through the regenerator in kg/s. ω_{in_RE} and ω_{out_RE} are air humidity ratios at the regenerator inlet and outlet respectively, in kg/kg$_{dryair}$.

In addition, the evaporative cooling effectiveness (ε_{EV}) is defined to evaluate the evaporative cooler performance.

$$\varepsilon_{EV} = \frac{T_{in\_EV} - T_{out\_EV}}{T_{in\_EV} - T_{wb\_in\_EV}} \tag{7}$$

where, T_{in_EV} and T_{out_EV} are air dry bulb temperatures at the evaporative cooler inlet and outlet respectively, in °C. $T_{wb\_in\_EV}$ is air wet bulb temperature at the evaporative cooler inlet, in °C.

Based on the airstream enthalpy difference between the inlet and outlet, the dehumidifier cooling output ($\dot{Q}_{DH\_cooling}$) and system total cooling output ($\dot{Q}_{cooling}$) are determined:

$$\dot{Q}_{DH\_cooling} = \dot{m}_{air\_DH}(h_{in\_DH} - h_{out\_DH}) \tag{8}$$

$$\dot{Q}_{cooling} = \dot{m}_{air\_DH}(h_{in\_DH} - h_{supply}) \tag{9}$$

where, h_{in_DH} and h_{out_DH} are specific enthalpies of the airstream entering and leaving the dehumidifier respectively, in J/kg, and h_{supply} is supply air enthalpy, in J/kg.

The MLDDC system overall coefficient of performance (COP) is defined as:

$$\text{COP} = \frac{\dot{Q}_{cooling}}{\dot{Q}_{RE}} \tag{10}$$

where $\dot{Q}_{RE}$ is regenerator thermal input power in W and can be expressed as

$$\dot{Q}_{RE} = \dot{m}_{w\_RE} \cdot c_{p\_w\_RE}(T_{w\_f} - T_{w\_r}) \tag{11}$$

where, $\dot{m}_{w\_RE}$ and $c_{p\_w\_RE}$ are hot water mass flow rate in kg/s and specific heat capacity in J/kg·K. T_{w_f} and T_{w_r} are hot water supply and return temperatures in the heating circuit respectively, in °C.

4. Results and Discussion

The influences of operating variables on the dehumidification, regeneration, evaporative cooling and overall system performances are analysed respectively in this section. As defined in Section 3, the main performance parameters include the dehumidification moisture removal rate, effectiveness and cooling output, the regeneration moisture addition rate and thermal input power, the evaporative cooling effectiveness, the system total cooling output and COP. Based on the $CaCl_2$ solution operative concentration level for dehumidification, its concentration ratio ranging from 30% to 42% is selected in this study. Solution flow rates in the dehumidifier and regenerator units remain the same at 1L/min throughout investigations, which are able to provide sufficient wetting surfaces in the membrane units for continuous operation. Hot and cold water are supplied at flow rates of 2L/min and 12L/min respectively.

4.1 Dehumidification performance

4.1.1 Influence of inlet air condition

Experimental tests are firstly conducted to evaluate the dehumidification performance under various inlet air conditions at a $CaCl_2$ solution concentration ratio of 39%. The investigated inlet air conditions provided by the environmental chamber are shown in Fig. 6. To simulate different weather conditions in the hot and humid region, the dehumidifier inlet air is set in the temperature range of 28.0°C to 40.0°C and relative humidity ranges from 65% to 95%. The absolute humidity ratio varies from 16.39g/kg$_{dryair}$ to 36.48g/kg$_{dryair}$ accordingly.
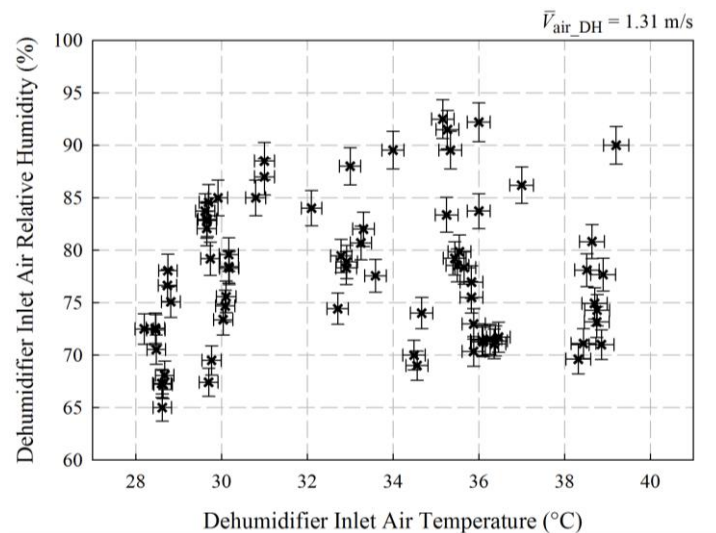
Fig. 6. Investigated dehumidifier inlet air condition range

As shown in Fig. 7, the dehumidification performance improves with inlet air temperature and relative humidity. The higher the air temperature and relative humidity, the higher the vapour pressure, and more mass transfer occurs owing to the greater vapour pressure difference between the airstream and desiccant solution. Consequently, the evident increases in the dehumidification moisture removal rate, effectiveness and cooling output are observed. For example, when the dehumidifier inlet air temperature is maintained at 36.0°C, the moisture removal rate increases from 0.15g/s to 0.25g/s as the air relative humidity rises from 71% to 92%, and correspondingly the dehumidification effectiveness increases from 0.50 to 0.68 and

the dehumidifier cooling output increases from 332.6W to 642.3W. This is because of the increase in the inlet air humidity ratio with relative humidity at a constant temperature, which causes more mass transfer in the dehumidification process. Similarly, the dehumidification performance improves with inlet air temperature under a constant relative humidity condition. For instance, at an inlet air relative humidity level of 75%, the moisture removal rate increases from 0.06g/s at air temperature of 29.0°C to 0.22g/s at air temperature of 39.0°C and simultaneously, the dehumidification effectiveness improves by 0.34 and the cooling output increases by 451.6W. This is due to the fact that the inlet air humidity ratio increases with air temperature while the relative humidity remains constant. Thus more heat and mass transfer takes place and the associated cooling load increases. The effects of inlet air condition on the dehumidification performance in this study are consistent with those in [24, 33, 36, 43, 44]. For instance, the dehumidifier performance of a MLDDC system with a potassium formate desiccant solution is experimentally investigated under various inlet air conditions in [33]. According to their experimental data, the moisture removal rate increases by approximately 35.69% at inlet air relative humidity of 60% as the inlet air temperature rises from 30°C to 35°C. Over the investigated inlet air relative humidity range of 50% to 70%, the dehumidification effectiveness improves from 0.32 to 0.47 and the dehumidifier cooling output increases by 303W at inlet air temperature of 35°C. These results indicate that the outdoor weather condition significantly affects the dehumidification performance and by comparison, the inlet air temperature has a more notable impact on the dehumidification performance.
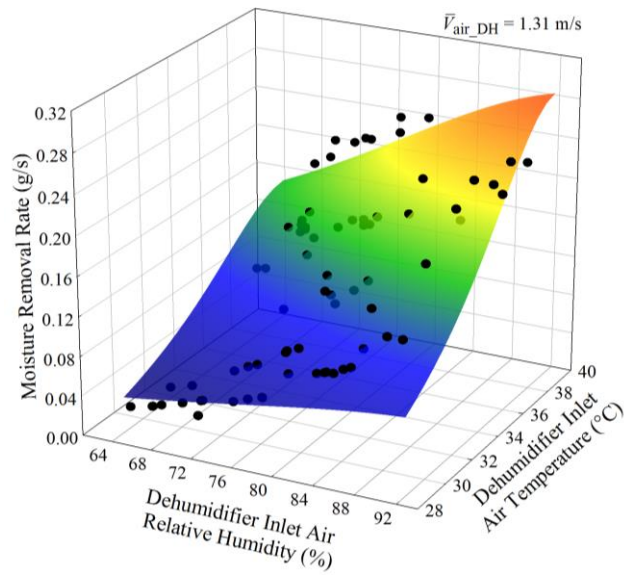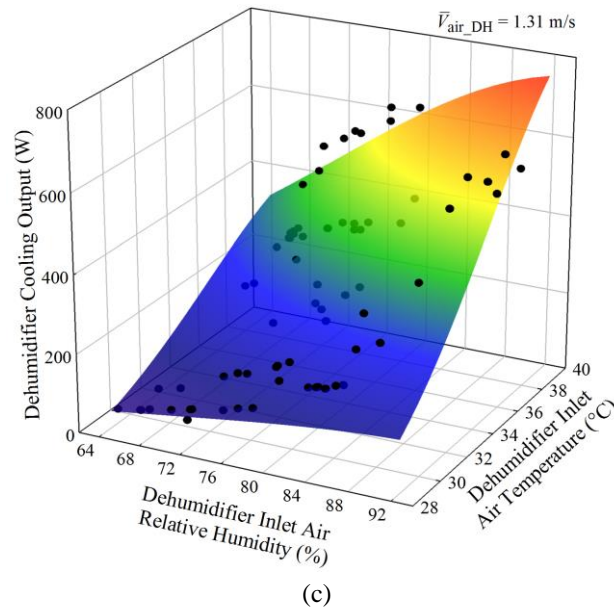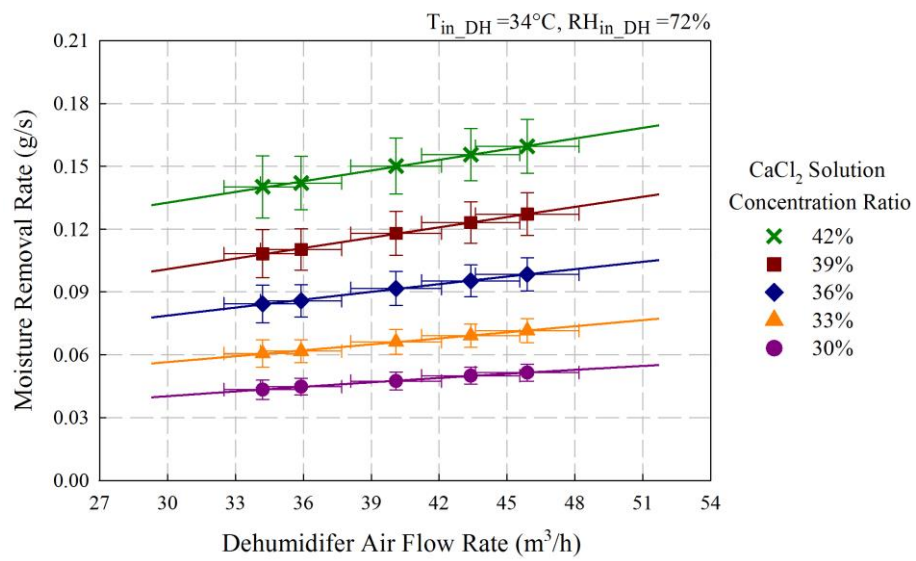
(a)
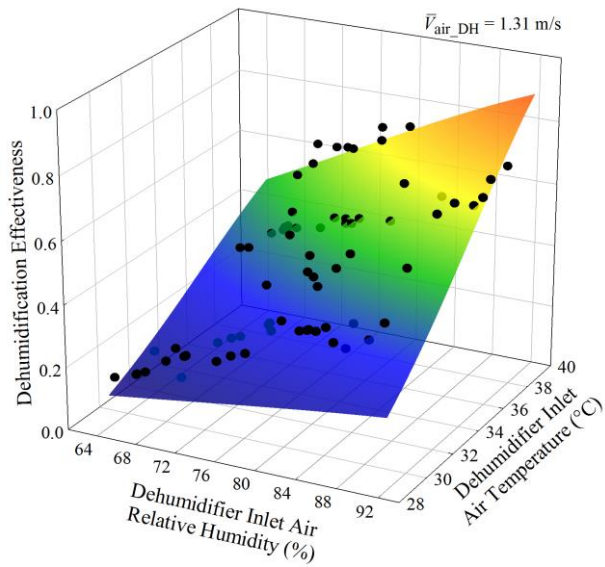
(b)

Fig. 7. Influences of inlet air condition on dehumidifier (a) moisture removal rate, (b) dehumidification effectiveness and (c) cooling output
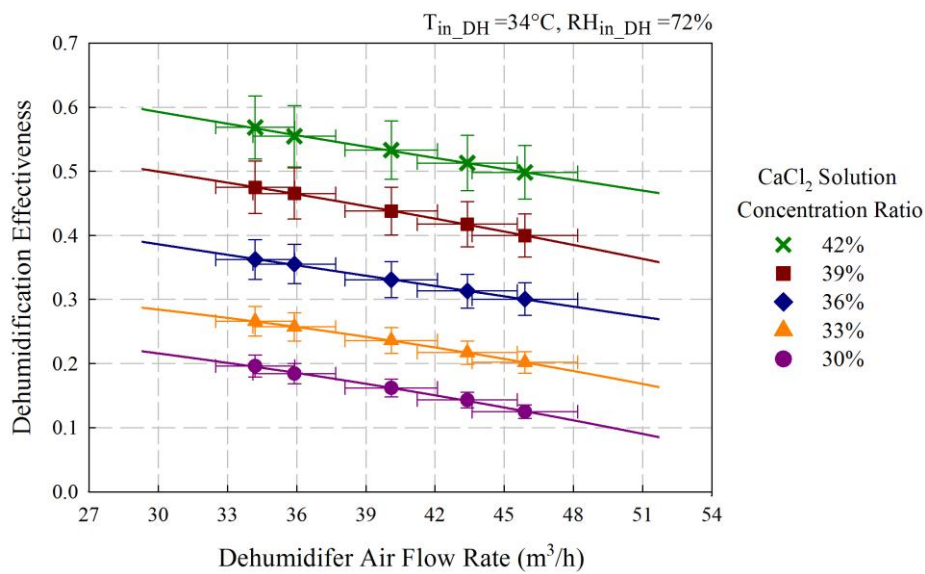
4.1.2 Influence of air flow rate

In order to assess the impact of air flow rate on the dehumidification performance, tests are carried out for the solution concentration ratio in the range of 30% to 42% with the inlet air temperature of 34.0°C and relative humidity of 72%. The influence of air flow rate is presented in Fig.8, it can be noted that the variation in the dehumidification performance is not very significant. At a solution concentration ratio of 42%, the moisture content change in the dehumidification process is 8.62g/kg$_{dryair}$ at air flow rate of 34.17m^3/h, and it reduces to 7.47g/kg$_{dryair}$ at air flow rate of 45.88m^3/h. This is due to the fact that the dehumidification capability decreases with air flow rate. However, the moisture removal rate is a function of air flow rate and moisture content change, which increases with air flow rate as displayed in Fig. 8(a). For instance, the moisture removal rate increases by 16.72% over the investigated air flow rate range at a concentration ratio of 36%. As indicated in Fig. 8(b), the dehumidification effectiveness decreases with air flow rate at a given solution concentration ratio. The influences of air flow rate on the moisture removal rate and dehumidification effectiveness in this study

are in good agreement with those in [45]. With LiCl as the liquid desiccant for an LDDC system, the dehumidifier moisture removal rate increases from 0.17g/s to 0.21g/s as the inlet air flow rate rises from 70kg/h to 115kg/h, while the dehumidification effectiveness reduces from 0.67 to 0.51 correspondingly [45]. On the other hand, a high flow rate causes a large volume of air being conditioned in the dehumidifier, thus the dehumidifier cooling output increases accordingly as shown in Fig. 8(c).

(a)

(b)
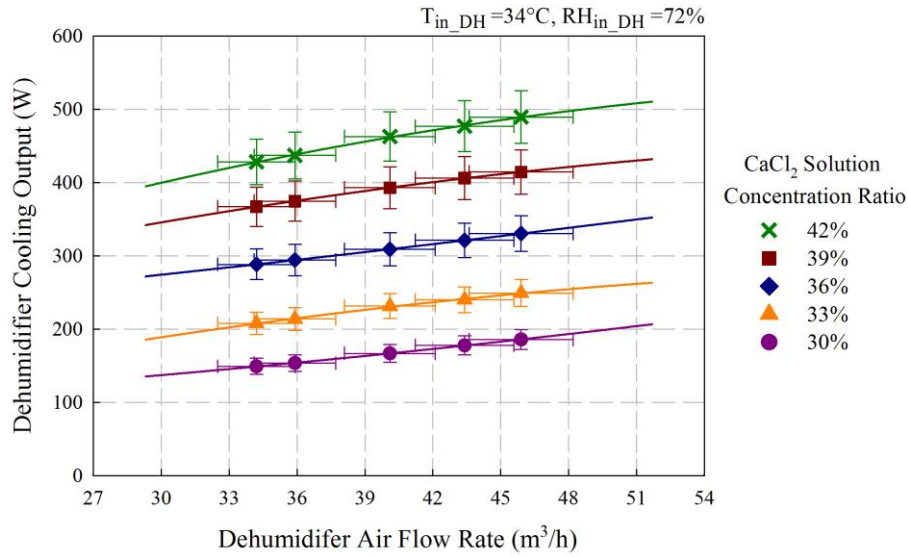
Fig. 8. Influences of air flow rate on dehumidifier (a) moisture removal rate, (b) dehumidification effectiveness and (c) cooling output

4.1.3 Influence of cold water temperature

The effect of cold water temperature on the dehumidification performance is then investigated as cold water is utilized to cool the regenerated solution prior to flowing into the dehumidifier. The dehumidifier inlet air condition is maintained constant, while cold water is supplied in the temperature range of 10.0°C to 20.0°C. Temperature variations in the dehumidifier sprayed solution and outlet air with cold water temperature are shown in Fig. 9. It can be seen that the desiccant solution spray temperature rises in accordance with cold water temperature from 13.9°C to 24.2°C at a solution concentration ratio of 42%, and the dehumidifier outlet air temperature increases from 29.5°C to 33.1°C accordingly.

$T_{in\_DH} = 34.3°C$, $RH_{in\_DH} = 72\%$, $\overline{V}_{air\_DH} = 1.31$ m/s
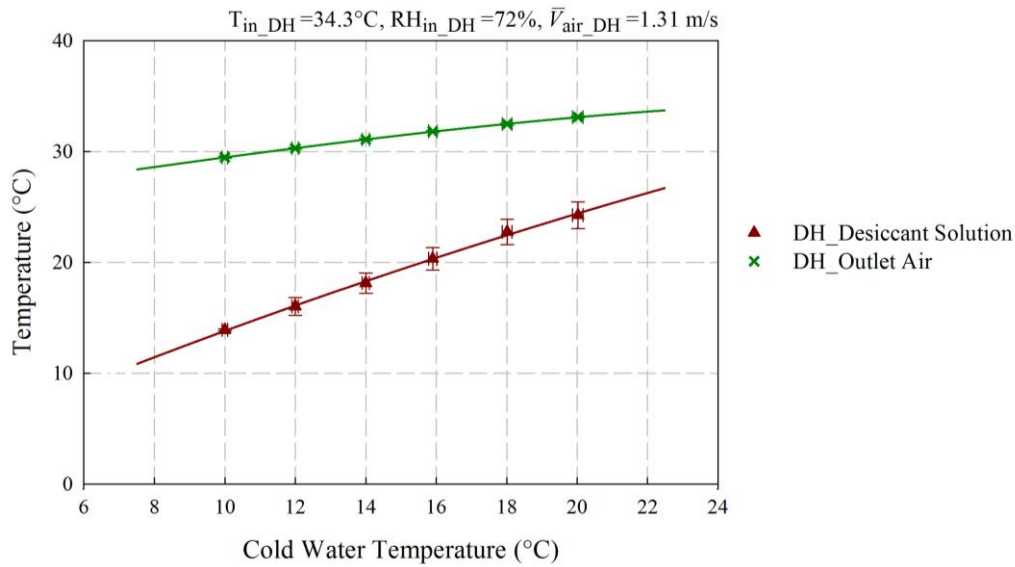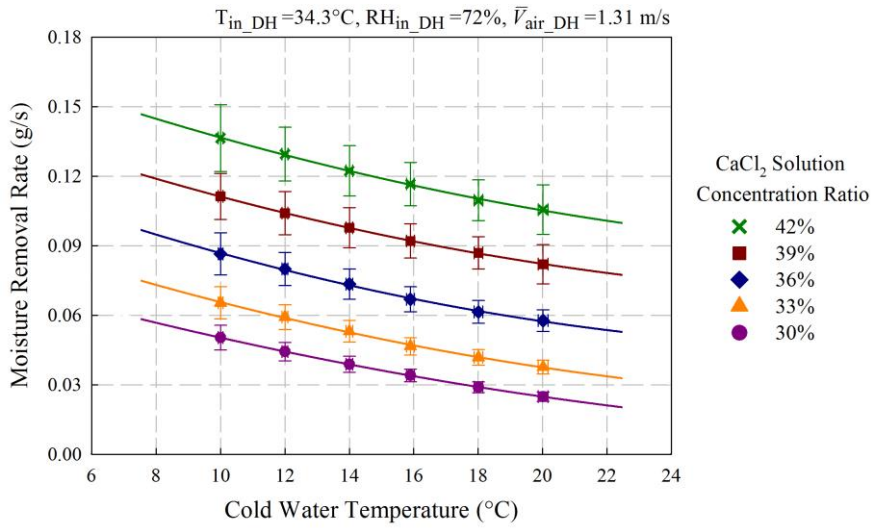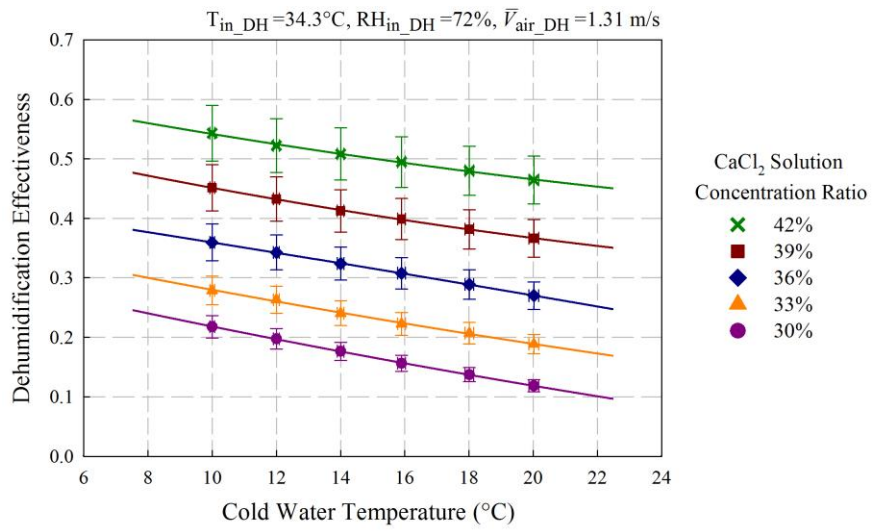
▲ DH_Desiccant Solution
✕ DH_Outlet Air

Fig. 9. Variations in dehumidifier solution spray temperature and outlet air temperature with cold water
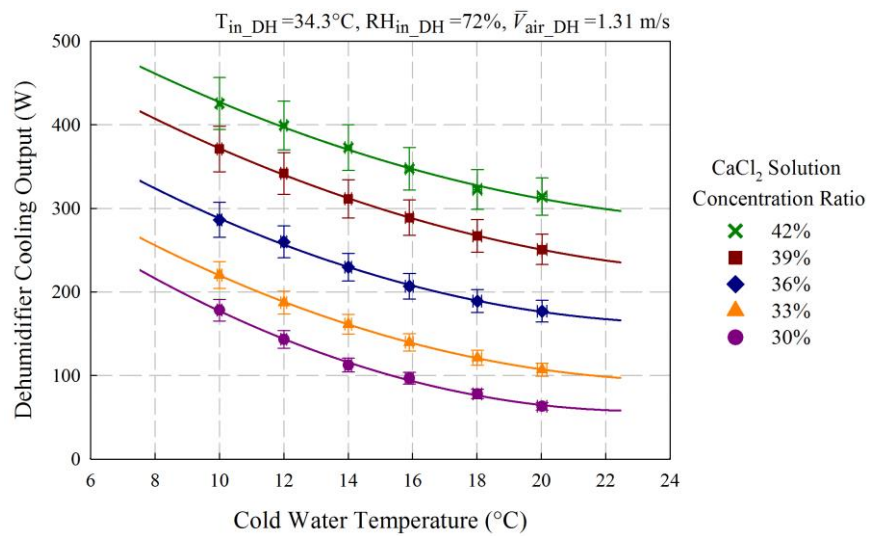
temperature

The increase in the desiccant solution spray temperature has a negative impact on the dehumidification performance as shown in Fig. 10. At a solution concentration ratio of 42%, the moisture removal rate reduces by 32.04% as the cold water temperature increases by 10°C, the dehumidification effectiveness decreases by 21.12% and the dehumidifier cooling output decreases by 28.23%. This is because that a higher desiccant solution temperature causes higher vapour pressure on the solution side, so less mass transfer occurs in the dehumidification process with a smaller vapour pressure difference between the solution and airstream. The results imply that an enhancement in the dehumidification performance can be achieved by lowering the desiccant solution spray temperature in the dehumidifier, which is also stated in [44]. Based on their experimental results of a MLDDC system, the dehumidifier moisture removal rate decreases by 41.2% as the dehumidifier solution inlet temperature rises from 15°C to 25°C at a LiCl solution concentration ratio of 30%.

$T_{in\_DH} = 34.3°C$, $RH_{in\_DH} = 72\%$, $\bar{V}_{air\_DH} = 1.31$ m/s

(a)

$T_{in\_DH} = 34.3°C$, $RH_{in\_DH} = 72\%$, $\bar{V}_{air\_DH} = 1.31$ m/s

(b)

$T_{in\_DH} = 34.3°C$, $RH_{in\_DH} = 72\%$, $\bar{V}_{air\_DH} = 1.31$ m/s

(c)

Fig. 10. Influences of cold water temperature on dehumidifier (a) moisture removal rate, (b) dehumidification

effectiveness and (c) cooling output

4.1.4 Influence of solution concentration ratio

It is noteworthy that the solution concentration ratio has a remarkable influence on the dehumidification performance, which has been confirmed by many researchers [45-48]. A higher solution concentration ratio contributes to better dehumidification performance as seen in Fig.8 and Fig.10. Under the investigated operating condition (i.e. the dehumidifier inlet air flow rate of 35.93m^3/h and cold water temperature of 10°C), the moisture removal rate is only 0.05g/s at a solution concentration ratio of 30%, while it increases to 0.14g/s at a concentration ratio of 42%, simultaneously, the dehumidification effectiveness improves from 0.22 to 0.56 and the dehumidifier cooling output increases from 178.2W to 425.4W. This is attributed to the larger vapour pressure difference between the airstream and desiccant solution at a higher concentration ratio, thus more moisture can be removed in the dehumidification process. A similar impact of LiCl solution concentration ratio on the dehumidification performance is presented in [45]. The dehumidifier moisture removal rate increases from 0.06g/s at a LiCl solution concentration ratio of 26% to 0.21g/s at a concentration ratio of 39% and the dehumidification effectiveness improves from 0.34 to 0.61 consequently.

4.2 Regeneration performance

4.2.1 Influence of air flow rate

Similarly, the effect of air flow rate on the regeneration performance is identified. The regenerator inlet air temperature and relative humidity are set at 26.0°C and 30% respectively, while its air flow rate rises from 43.82m^3/h to 148.44m^3/h. The increase in the regenerator air flow rate leads to a reduction in the moisture absorption capability. Nevertheless, the regeneration performance, which is assessed by the moisture addition rate, improves with air flow rate as shown in Fig. 11. At a concentration ratio of 30%, the moisture addition rate reaches 0.08g/s at air flow rate of 148.44m^3/h, while only 0.01g/s is achieved at flow rate of

43.82m^3/h. The same variation trend of the regenerator performance with air flow rate is indicated in [48], the moisture addition rate improves by 44.45% as the regenerator air flow rate increases from 0.12kg/s to 0.24kg/s.
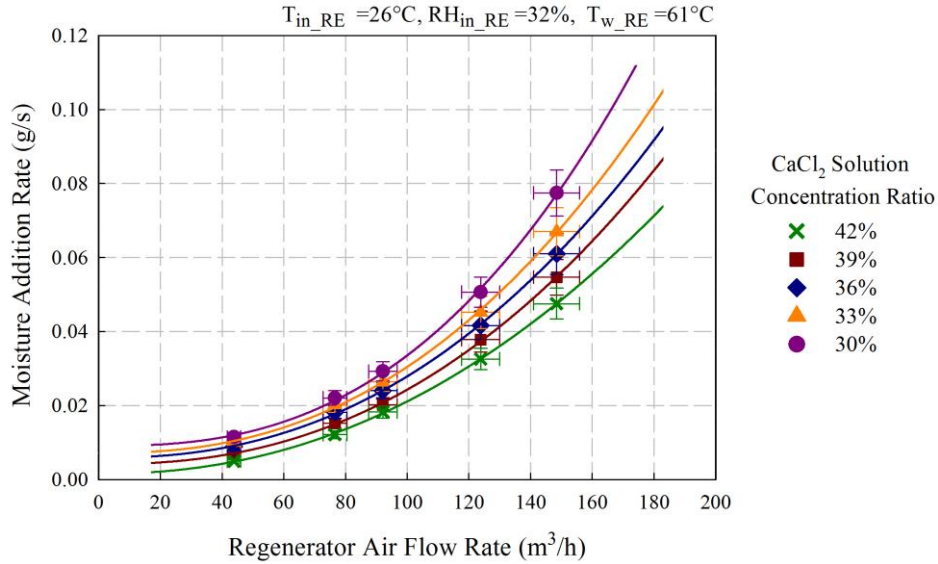

Fig. 11. Influence of air flow rate on regenerator moisture addition rate

The variation of the regenerator thermal input power with air flow rate at a solution concentration ratio of 42% is demonstrated in Fig. 12. Over the investigated air flow rate range, the hot water temperature difference in the heating circuit varies from 4.1°C to 5.2°C, as a result, the regenerator thermal input power is in the range of 568.9W to 728.6W. The higher the air flow rate, the more the thermal input power for heating the dilute solution. This finding is consistent with the statement in [47] that the regenerator air flow rate is a critical parameter influencing the regeneration performance. Therefore, the required thermal input power should be taken into account to determine the regenerator air flow rate.
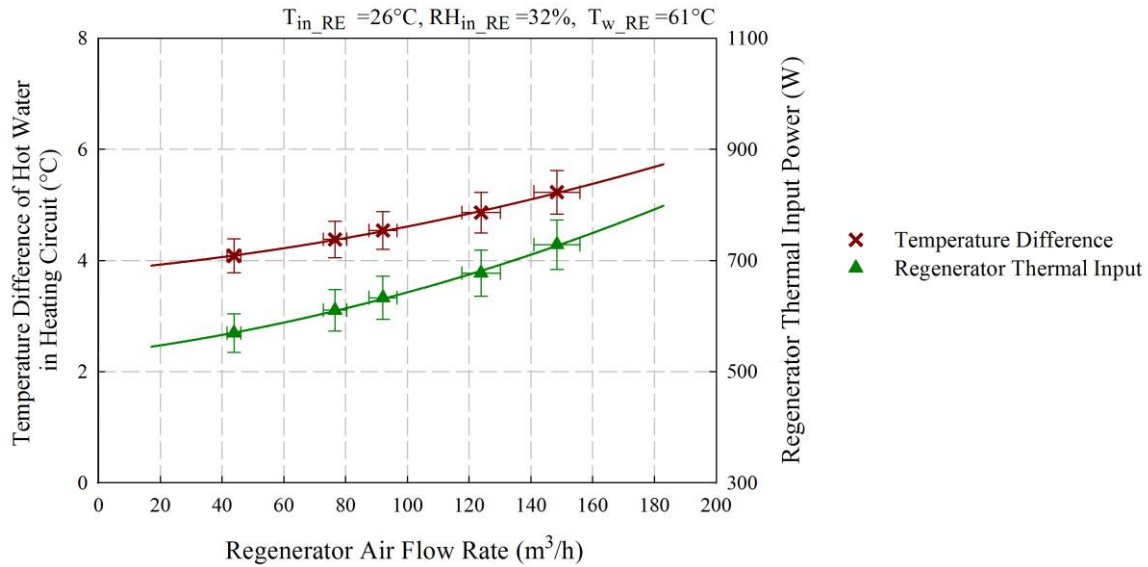
Fig. 12. Influence of air flow rate on regenerator thermal input power

4.2.2 Influence of regeneration hot water temperature

In this study, hot water from a boiler is utilized for regeneration purpose. In order to clarify the influence of the regeneration temperature on the regeneration performance, the hot water temperature is set in the range of 55.0°C to 80.0°C while the regenerator inlet air is maintained at a temperature of 26.0°C and relative humidity of 33%. The impact of hot water temperature on the regeneration moisture addition rate is indicated in Fig. 13. It can be observed that the regeneration performance greatly improves with hot water temperature. For instance, the moisture addition rate increases by 72.32% as the hot water temperature rises from 55.0°C to 80.0°C at a solution concentration ratio of 42%, while it doubles at a concentration ratio of 30%. A similar effect of hot water on the regeneration performance is found in an LDDC system using LiBr aqueous solution [48], an approximately 30% increase in the moisture addition rate is obtained as hot water temperature rises from 31°C to 42°C. A higher hot water temperature causes higher vapour pressure of the desiccant solution in the regenerator; hence more mass transfer from the solution to airstream occurs because of a greater vapour pressure difference.
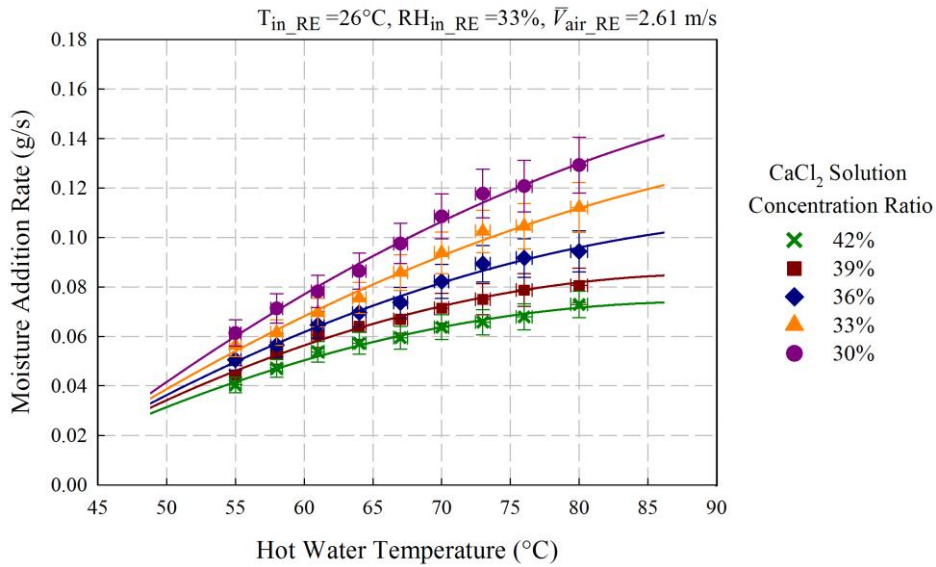
Fig. 13. Influence of hot water temperature on regenerator moisture addition rate

On the other hand, a considerable increase in the regenerator thermal input power with hot water temperature is observed, as illustrated in Fig. 14. At a solution concentration ratio of 42%, the thermal input power doubles as the hot water temperature rises from 55.0°C to 80.0°C. The higher the hot water temperature, the better the regeneration performance, but simultaneously more thermal input power is required.
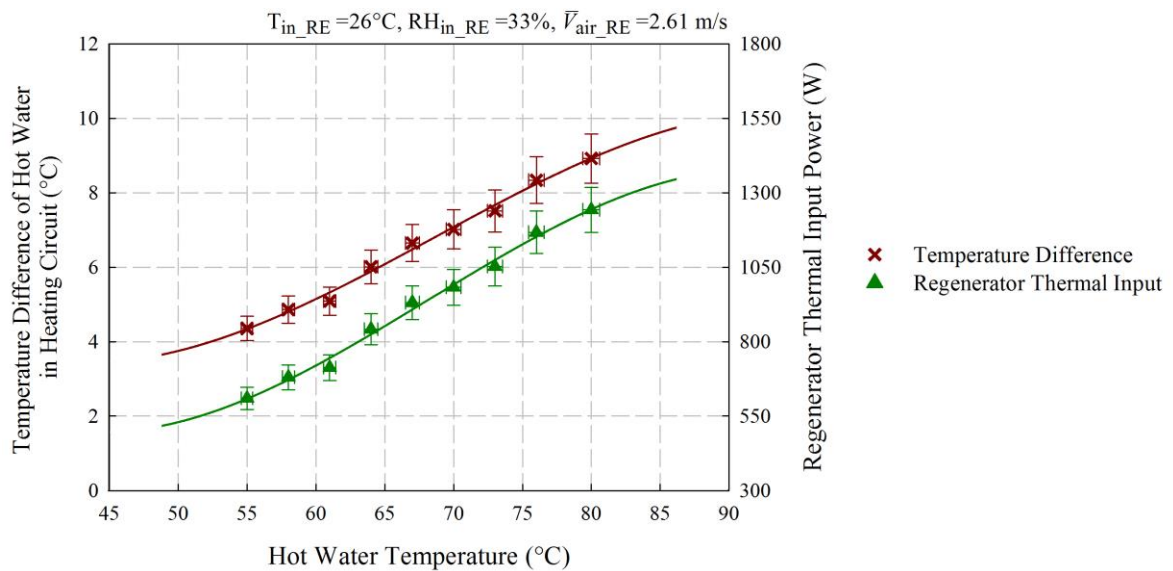

Fig. 14. Influence of hot water temperature on regenerator thermal input power

4.2.3 Influence of solution concentration ratio

It can be noted that a better regeneration performance is achieved at a lower solution concentration ratio as shown in Fig. 11 and Fig. 13. For example, at air flow rate of 148.44m^3/h, the moisture addition rate increases by 63.83% as the solution concentration ratio decreases from 42% to 30%. In the regeneration process, less mass transfer takes place at a higher concentration ratio due to the lower vapour pressure. Similarly, the effect of LiCl solution concentration ratio on the regeneration performance is demonstrated in [49]. The regenerator moisture addition rate reduces by 10.14% as the concentration ratio of LiCl solution increases from 32% to 35%. On the other hand, a more significant moisture addition rate variation with hot water temperature is observed at a lower concentration ratio as presented in Fig. 13. It is also worth noting that the increase rate in the moisture addition rate with hot water temperature slows down gradually. For example, at a concentration ratio of 42%, only a slight change in the moisture addition rate (i.e. 0.01g/s) is observed with a hot water temperature range of 65.0°C to 80.0°C. Thus, an appropriate regeneration temperature range should be determined for the adequate regeneration performance based on the operative solution concentration ratio in order to avoid the excessive thermal input power and improve the overall system energy performance.

4.3 Evaporative cooling performance

Tests are carried out to identify the effect of cold water temperature on the evaporative cooling performance. Variations of the cooler outlet air temperature and evaporative cooling effectiveness are shown in Fig. 15. Under the constant inlet air condition, the evaporative cooler outlet air temperature increases from 19.4°C to 23.8°C and the evaporative effectiveness decreases from 0.72 to 0.37 as the cold water temperature rises from 10.0°C to 20.0°C. In this system, the cold water supplied at a lower temperature not only evidently leads to the better

evaporative cooling performance [23] but also contributes to an improvement in the dehumidification performance as discussed in Section 4.1.3.
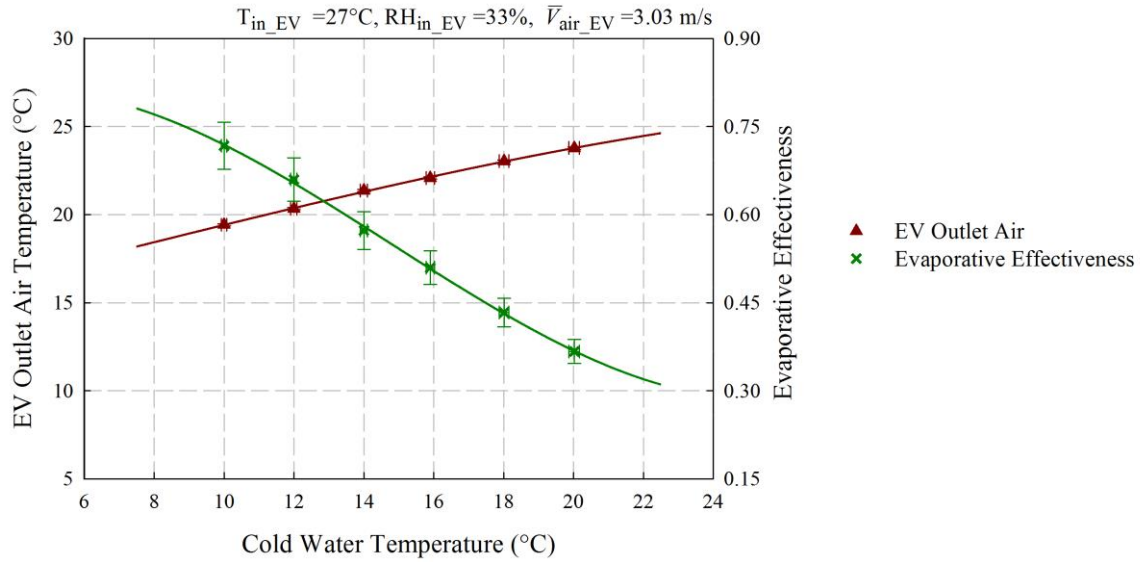

Fig. 15. Variations in evaporative cooler outlet air temperature and its effectiveness with cold water temperature

4.4 System performance

With respect to the system steady operation at a given solution concentration ratio, the performance balance between the dehumidifier and regenerator is of great importance as desiccant mass imbalance problems may occur over time, such as the dilution of the solution with insufficient regeneration and a more concentrated solution with excessive regeneration [33]. As mentioned previously, both the dehumidification and regeneration performances vary remarkably with the desiccant solution concentration ratio. Referred to Sections 4.1 and 4.2, the dehumidification moisture removal rate and regeneration moisture addition rate at different solution concentration ratios are presented in Fig. 16, which are obtained under the individual operating states. It is noteworthy that the entire system is capable to run steadily at a solution concentration ratio of 36% under the stated operating condition, at which the dehumidifier moisture removal rate and regenerator moisture addition rate match each other.

For the system operating steadily at the other concentration ratios, measures should be taken to balance the dehumidification and regeneration performances. For the concentration ratio below 36%, the dehumidification performance should be improved to match with that of the regeneration. As discussed in Section 4.1, increasing the dehumidifier air flow rate is one of the approaches to enhance the moisture removal rate. For example, the dehumidifier air flow rate of 110m^3/h is needed to ensure its moisture removal rate to match with the regenerator moisture addition rate at a solution concentration ratio of 30%, while the dehumidifier air flow rate is required at 55m^3/h for the concentration ratio of 33%. On the other hand, for the solution concentration ratio over 36%, the regenerator moisture addition rate should be increased to eliminate the imbalance issue. It is stated in Section 4.2 that the increases in the regenerator air flow rate and hot water temperature result in better regeneration performance. Based on the experimental analysis, the regenerator air flow rates should be kept at 200m^3/h and 240m^3/h for concentration ratios of 39% and 42% respectively. Moreover, an appropriate regeneration hot water temperature range should be selected to avoid the excessive thermal input power.
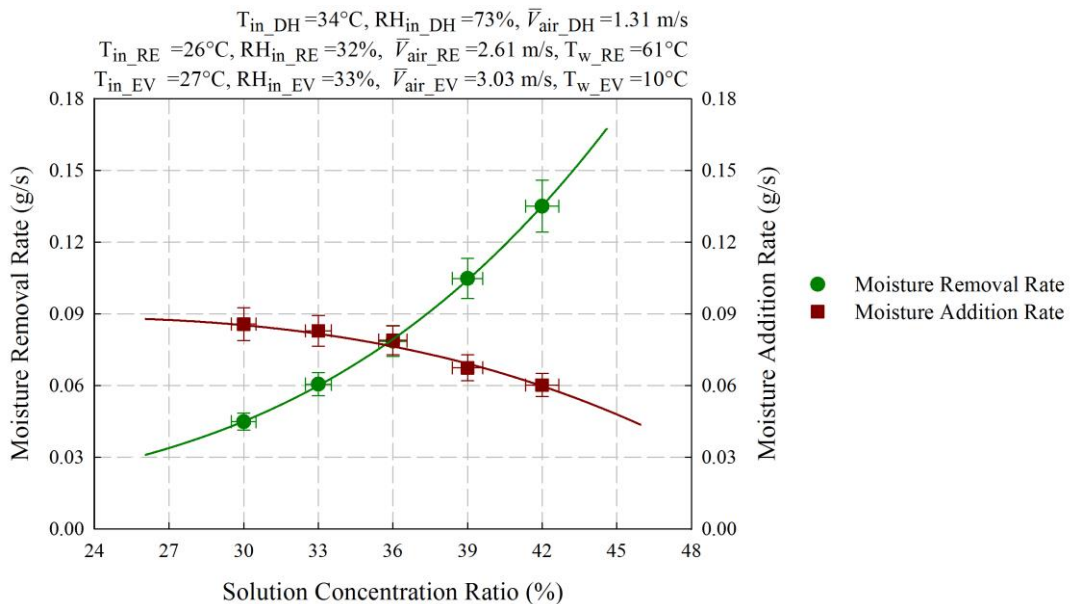

Fig. 16. Variations in system moisture removal and addition rates with solution concentration ratio

The overall system performance is evaluated by the system COP. Referred to the previous analysis, it can be projected that a higher system COP is obtained at a lower solution concentration ratio, for example, the system COP reaches 0.74 at a concentration ratio of 30% while it is only 0.61 at a concentration ratio of 42%. For the concentration ratio below 36%, improving the dehumidification performance (i.e. increasing the dehumidifier air flow rate) contributes to more total cooling output, and thus a comparatively higher system COP is achieved. On the contrary, for the concentration ratio over 36%, improving the regeneration performance (i.e. increasing the regenerator air flow rate or hot water temperature) requires much more thermal input power, so that the system COP is relatively lower. Alternatively, the regenerator could be designed with a large dimension as stated in [33], which provides a large contact area for more heat and mass transfer in the regeneration process. Furthermore, the crystallization problem may appear for a high concentrated solution, which causes the risks of fluid mal-distribution, channel blockage, high pumping pressure, and membrane fouling [48]. For example, at a solution concentration ratio of 42%, $CaCl_2$ solution begins crystalizing at a temperature of 16.0°C.

4.4.1 Influence of cold water temperature

Under the stated operating condition, the effect of cold water temperature on the system performance is assessed at solution concentration ratio of 36%. The evident declines in the system total cooling output and COP with cold water temperature are observed in Fig. 17. The system total cooling output reduces from 486.7W at cold water temperature of 10.0°C to 339.6W at cold water temperature of 20.0°C, and the COP decreases from 0.70 to 0.59 accordingly. As mentioned in Section 4.1.3, the cold water temperature influences the desiccant solution spray temperature in the dehumidifier, the solution spray temperature increases from 13.9°C to 24.2°C as the cold water temperature rises from 10°C to 20°C. A similar impact of the dehumidifier solution temperature is presented in [44], the system COP reduces from 0.75

to 0.65 as the LiCl solution temperature increases from 15°C to 25°C at the dehumidifier inlet. The results imply that colder water is preferred for better dehumidification and system performances, which is also suggested by Gandhidasan [12]. In addition, varying cold water temperature could also be a solution to reach the desired supply air temperature. According to the experimental data, the supply air temperature rises from 20.4°C to 24.8°C as the cold water temperature rises from 10°C to 20°C.
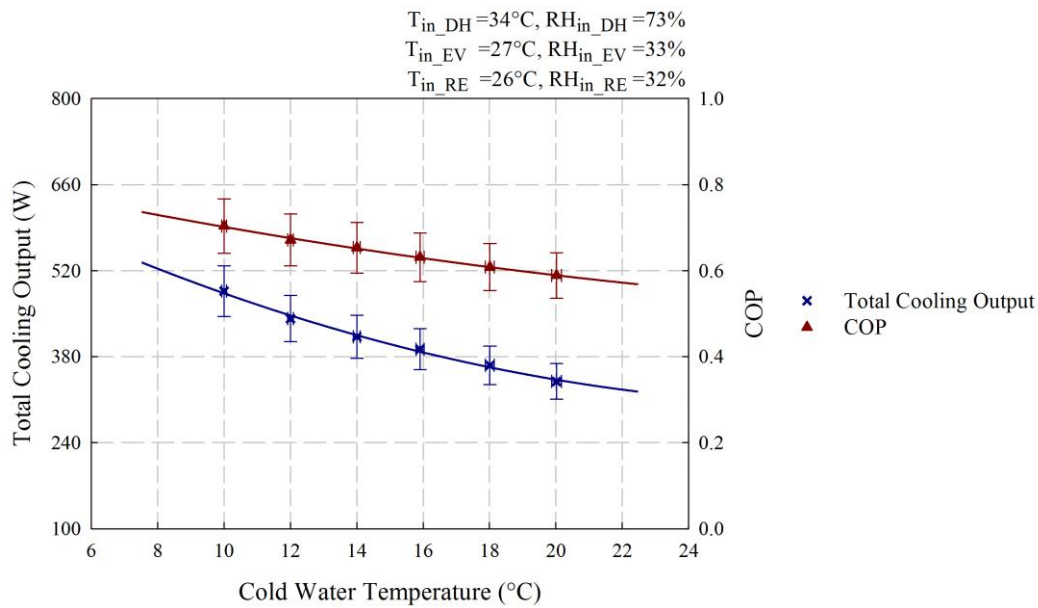

Fig. 17. Influences of cold water temperature on system cooling output and COP

4.4.2 Influence of regeneration temperature

The effect of hot water temperature on the system performance is indicated in Fig. 18. At a solution concentration ratio of 36%, the regenerator thermal input power increases by 635.3W while the system COP reduces by 21.33% as the hot temperature rises from 55.0°C to 80.0°C. The desiccant solution temperature at the regenerator inlet varies in line with the hot water temperature. Similarly, an evident reduction in the system COP with the regenerator desiccant solution temperature is also noted in [44], the system COP decreases by approximately 17% when the LiCl solution temperature at the regenerator inlet rises from 40°C to 65°C. The results reveal that more thermal input power is required to attain a higher regeneration temperature and thereby a lower system COP is obtained.
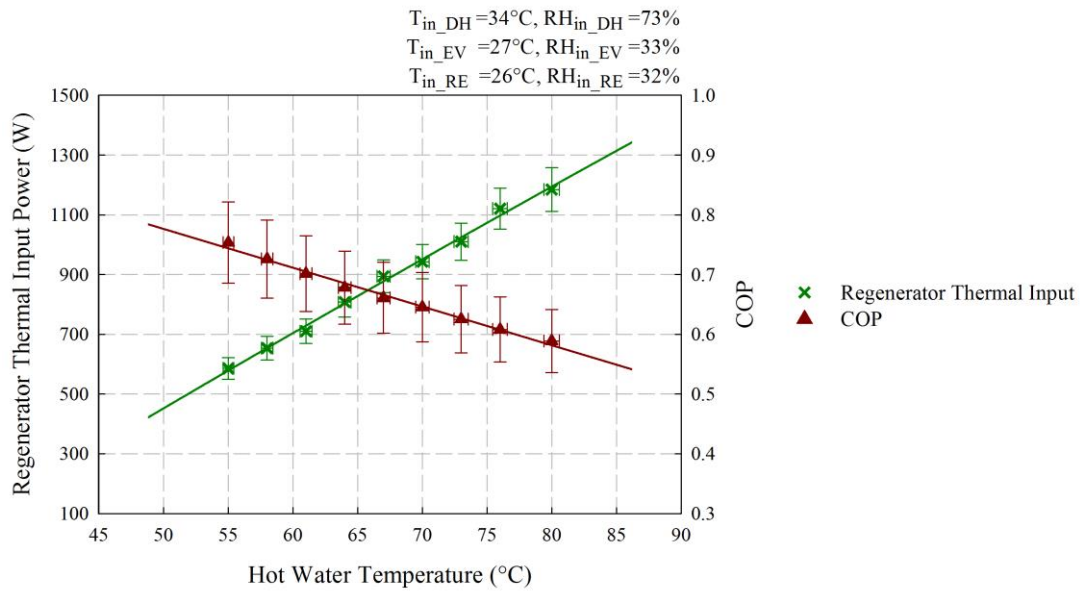
Fig. 18. Influences of hot water temperature on regenerator thermal input power and system COP

5. Conclusions

In this study, the performance of a hybrid membrane-based liquid desiccant dehumidification cooling system has been evaluated through experimental work. With $CaCl_2$ solution, the system is feasible for operating in the hot and humid region with efficient independent temperature and humidity controls. Based on the experimental results, the following conclusions are drawn.

- The system dehumidification performance is greatly influenced by the local weather condition, both the moisture removal rate and dehumidification effectiveness increase with inlet air temperature and humidity.

- The dehumidifier cooling output increases with air flow rate while its dehumidification effectiveness deceases simultaneously.

- The regeneration performance improves with air flow rate and hot water temperature, and the required thermal input power increases accordingly. At a solution concentration ratio of 42%, the regenerator moisture addition rate increases by 72.32% as the hot water temperature rises from 55.0°C to 80.0°C, whereas its thermal input power doubles.

- To avoid the excessive thermal input power for the desiccant solution regeneration, hot water temperature should be controlled within an appropriate range based on the operative solution concentration ratio.

- The dehumidification, evaporative cooling and overall system performances decrease with cold water temperature, while the supply air temperature increases. The supply air temperature increases from 20.4°C to 24.8°C as the cold water temperature rises from 10.0 °C to 20.0°C.

- The solution concentration ratio has a marked impact on the system performance. The higher the concentration ratio, the better the dehumidification performance, but the regeneration capability is degenerated, and the associated crystallization risk should be noted as well. As the desiccant solution becomes stronger from the concentration ratio of 30% to 42%, the dehumidification effectiveness improves by 0.37 whereas the regeneration moisture addition rate decreases by 58.38%.

- The system mass balance between the dehumidifier and regenerator is of vital importance for the system steady operation. Appropriate adjustments should be applied for the match between the dehumidification moisture removal rate and regeneration moisture addition rate at a given solution concentration ratio.

- The dehumidification effectiveness of 0.30 and system COP of 0.70 are achieved at a solution concentration of 36% under the investigated operating condition and the supply air is produced at a temperature of 20.4°C.

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