

1 DOI: 10.1002/ ((please add manuscript number))

2 **Article type: Full Paper**

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5 **Synthesis of Methacrylate-Terminated Block Copolymers with Reduced**
6 **Transesterification by Controlled Ring-Opening Polymerization**

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25 **Abstract**

26 This work presents a robust method to achieve the synthesis of low molecular weight polyesters
27 via ring-opening polymerization (ROP) initiated by 2-hydroxyethyl-methacrylate (HEMA)
28 when using triazabicyclodecene (TBD) as catalyst. The effect that the HEMA:TBD ratio has
29 upon the final reaction rate and final polymer molecular architecture is discussed. The optimum
30 HEMA:TBD ratio and reaction conditions required to minimize competing transesterification
31 reactions were determined, in order to synthesize successfully the target ROP macromonomer
32 species containing only a single 2-methacryloyloxyethyl end-group. Additionally, to confirm
33 the terminal end-group fidelity of the product macromonomers and confirm TBD utility for
34 block copolymer manufacture, a small series of di-block polyesters were synthesized using
35 TBD and shown to exhibit good control over the final polymer structure whilst negating the
36 side transesterification reactions, irrespective of the monomers used.

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1. Introduction

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44 Synthetic aliphatic polyesters, such as poly(lactic acid) (PLA), polycaprolactone (PCL), or
45 polycarbonates such as poly(trimethylene carbonate) (PTMC) and their copolymers are widely
46 used for pharmaceutical and environmental applications due to their controllable
47 biodegradability and low cost of production.^[1,2] To extend their use into more demanding
48 applications, aliphatic polyesters with a wider variety of terminal or side-chain functionality are
49 required.^[3,4] For example, the introduction of a reactive double-bond, as either a side chain or
50 an end-terminus on the main polymeric backbone, has paved the way for the production of
51 highly functional copolymers where the functionality can be used as platform for post-
52 functionalization or further polymerization.^[5] In particular, the free hydroxyl group of 2-
53 hydroxyethylmethacrylate (HEMA) has been exploited as a ring-opening polymerization
54 (ROP) initiator for the production of polyesters bearing a methacrylate terminus.^[6] These
55 HEMA-terminated-polyester macromonomers have been used in copolymerization with other
56 (metha)acrylic monomers,^[7] to produce graft-copolymers *via* controlled radical polymerization
57 techniques such as ATRP and RAFT.^[8,9] However, the majority of the HEMA-based polyesters
58 and polycarbonates, including the examples reported above, have been prepared using Sn based
59 catalysts.^[10-14] Unfortunately, Sn-residues can be difficult to remove during polymer
60 purification, which may compromise the quality of the final product and the potential
61 applicability.^[15] An alternative route to polyesters utilizes enzymes as the catalyst system.^[16]
62 However, enzyme catalyzed ROP (eROP) generally results in slow reactions with limited
63 control over the final polymer architecture.^[17] In HEMA-initiated Lipase catalyzed eROP, even
64 at low monomer conversion, numerous unwanted by-products are routinely obtained. This has
65 been attributed to the low reaction selectivity of the enzyme, which allows competition between
66 ROP and other transesterification processes.^[16,17] The use of triazabicyclodecene (TBD) as a
67 catalyst for ROP has been demonstrated with a variety of cyclic monomers, resulting in the

68 synthesis of polymers with controlled molecular weight and polydispersity.^[18] The enhanced
69 catalytic activity of TBD when compared with other organo-catalysts such as 1,8-
70 Diazabicyclo[5.4.0]undec-7-ene (DBU) and 4-Dimethylaminopyridine (DMAP) results from
71 its ability to activate both monomer and initiator simultaneously.^[19]

72 Building on these previous reports, the present study focuses on the development of a synthetic
73 strategy which ensures good selectivity towards polymerization when using an α,ω -functional
74 initiator such as HEMA, without compromising the end-group functionality. The reported
75 method shows that TBD can be used as a catalyst to obtain HEMA-terminated-polyesters from
76 three classes of monomer while demonstrating good control over the final polymer structure.
77 These monomers, D,L-lactide (LA), ϵ -caprolactone (CL) and trimethylene carbonate (TMC),
78 were chosen to exemplify a wide range of polymers commonly produced by ROP. Previous
79 reports of TBD catalyzed ROP have suggested that implementing the correct initial
80 initiator:catalyst ratio (HEMA:TBD in this case) is of vital importance for maintaining
81 polymerization control, due to the dual nature of the catalyst activating both monomer and
82 initiator.^[18] Applying incorrect ratios and/or conditions can generate unwanted pre-
83 polymerization and concomitant acyl transfer side reactions. Therefore, we conducted a
84 systematic study of the extent of HEMA transesterification by varying the initial HEMA:TBD
85 ratio, to determine the optimum initiator:catalyst feed that would minimize undesired side
86 transesterification reactions in the synthesis of a target set of low molecular weight polymers.
87 To achieve the desired low molecular weight materials (i.e. DP's in the region 8 – 45), these
88 experiments require relatively high HEMA concentrations and so are susceptible to the onset
89 of side reactions. The present work has identified the reaction conditions which allowed the
90 successful production of mono(methyl)acrylated polymers with well-defined structures and
91 molecular weights, irrespective of the monomers used. More specifically, high conversion of
92 monomer into polymers as well as controlled molecular weight with respect to the initial [M]:[I]
93 feed-ratio, and polydispersity below 1.3 were simultaneously achieved. By identifying the

94 correct ratios of monomer, initiator and catalyst, the reported synthetic methodology has
95 overcome the previously described unsuccessful attempts to use TBD as catalyst in HEMA-
96 initiated ROP due to the formation of uncontrollable by-products.^[20] Finally, to validate the
97 overall robustness and versatility of the proposed synthetic strategy, the chain-extension of a
98 HEMAPCL polyester from the hydroxyl-end group, to generate mixed block copolymers, was
99 successfully demonstrated.

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101 **2. Experimental Section**

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103 **2.1 Materials and Methods**

104 D,L-lactide 99% (LA) was purchased from Alfa Aesar (by Thermo Fisher Scientific).
105 Trimethylene carbonate (TMC) was purchased from Polyscience. ϵ -caprolactone (CL), extra
106 dry dichloromethane (DCM), deuterated chloroform (CDCl_3) and triazabicyclodecene (TBD)
107 were acquired from Sigma Aldrich. Hexane, diethyl ether and methanol were obtained from
108 Fisher. In all cases the vials were dried in an oven at 100 °C overnight prior to use, and the
109 HEMA and DCM were stored over molecular sieves and under an inert atmosphere.

110 **2.2 Synthesis**

111 **HEMA Transesterification Kinetics in Presence of TBD.** In a typical procedure, pre-
112 calculated amounts of HEMA and TBD were mixed in 3 mL of DCM at room temperature to
113 commence the chemical transformations. As the reactions proceeded, aliquots of the solution
114 were taken at predetermined time points (0, 5, 15 and 60 min) and were analyzed by ^1H NMR
115 spectroscopy. The quantities of HEMA and TBD were selected in order to mimic the reaction
116 conditions in which 1000 mg of ϵCL (8.77 mmol) would be present as the initial monomer
117 loading. Namely, HEMA was used at two distinct feed levels which mimicked a hypothetical
118 final targeted molecular weight of 2000 Da and 10,000 Da respectively. They were defined as
119 the “high” and “low” levels of HEMA (High: 0.46 mmol, 60 mg and Low: 0.10 mmol, 13 mg).

120 TBD was also systematically introduced and two levels to reproduce the limiting reaction
121 conditions of 1 and 2.5 % mol:mol ratios when compared to the monomer, i.e. these are the
122 “low” (12 mg) and “high” (30 mg) TBD definitions. Four different boundary transesterification
123 scenarios were then applied and analyzed with respect to the result of the ROP reaction. An
124 unpaired t-test ($p < 0.05$ indicating significant difference) analysis was performed at each time-
125 point for each selected ratio.

126 **HEMA Initiated ROP of the Cyclic Monomers.** ROP experiments were performed adopting
127 ‘standard laboratory’ conditions, i.e. ambient temperature and atmosphere.^[21] The desired
128 amount of cyclic monomer (500-1000 mg) and HEMA-initiator ($[M]:[I]$ or DP_0 ratios targeted
129 to produce final molar masses of either 2500 or 5000 Da) were weighed into a vial, which had
130 been dried in an oven at 100 °C overnight and capped with a rubber septum. DCM (10 ml), was
131 then added via syringe and the mixture was allowed to dissolve at room temperature (RT) for
132 5-10 minutes. Varying amounts of catalyst (from 1-2.5 % mol/mol of TBD with respect to
133 monomer) were then added to trigger the ring-opening process. Reactions were observed to
134 occur in time-frames ranging from 1-240 minutes, according to the
135 monomer:initiator :solvent :catalyst adopted ratios. The reaction was terminated by catalyst
136 deactivation upon adding an acidic solution and the polymer purified by means of multiple
137 precipitation steps and dried in a vacuum oven.

138 **HEMAPCL (Entries 7 and 8, Table 1) Initiated ROP.** The required amount of cyclic
139 monomer (500-1000 mg) and PCLHEMA-initiator to give the $[M]:[I]$ ratios needed to achieve
140 a targeted extension of 10 units for TMC and 35 units for LA, were weighed into a vial which
141 had been dried in an oven at 100 °C overnight and capped using a rubber septum. DCM (10
142 ml), which had been dried over molecular sieves and kept under inert gas environment, was
143 then added via syringe and the mixture was allowed to dissolve at RT for 5-10 minutes. A
144 certain amount of TBD equal to 1% mol:mol compared to the amount of monomer was then

145 added to trigger the ring-opening process. The TBD was quenched by adding an acid solution
146 after 3 minutes to terminate the reaction.

147 **2.3 Polymer Characterization**

148 **HEMA-PDLLA.** Characterization data was obtained after three precipitation cycles in hexane
149 and diethyl ether. 1H NMR (400 MHz, $CDCl_3$): δ 6.14 (s, 1H), 5.61 (s, 1H), 5.19 (m,
150 2H*[M]:[I]), 4.36 (m, 5H), 1.95 (m, 3H), 1.59 (m, 6H*[M]:[I]), presence of residual catalyst
151 and solvents (from synthesis and purification) can be spotted. *Conversion:* monomer to final
152 polymer conversion determined by NMR was 90-95% with a recorded gravimetric yield of 70-
153 75% (700-750 mg when aiming at theoretical 1000 mg of polymer). Further characterization
154 shown in Table 1. *Molecular Weight:* As all polymers exhibited transesterification levels below
155 10%, M_n values were evaluated by 1H NMR.^[6,8]

156 **HEMA-PTMC.** Characterization data was obtained after three precipitation cycles in hexane
157 and diethyl ether. 1H NMR (400 MHz, $CDCl_3$): δ 6.14 (s, 1H), 5.61 (s, 1H), 4.39 (m, 4H), 4.25
158 (m, 4H*[M]:[I]), 3.74 (m, 2H), 2.04 (m, 2H *[M]:[I]), 1.96 (m, 3H), presence of residual
159 catalyst and solvents (from synthesis and purification) can be spotted. *Conversion:* monomer
160 to final polymer conversion determined by NMR was 90-95% with a recorded gravimetric yield
161 of 50-60% (500-600 mg when aiming at theoretical 1000 mg of polymer). Further
162 characterization shown in Table 1. *Molecular Weight:* As all polymers exhibited
163 transesterification levels below 10% M_n values were evaluated by 1H NMR.^[6]

164 **HEMA-PCL.** Characterization data was obtained after purification *via* three cycles of
165 precipitation in cold MeOH. 1H NMR: (400 MHz, $CDCl_3$): δ 6.14 (s, 1H), 5.61 (s, 1H), 4.40-
166 4.30 (m, 4H), 4.08 (t, 2H*[M]:[I]), 3.68 (m, 2H), 2.33 (t, 2H*[M]:[I]), 1.97 (m, 3H), 1.67 (m,
167 4H*[M]:[I]), 1.41 (m, 2H*[M]:[I]), presence of residual catalyst and solvents (from synthesis
168 and purification) can be spotted. *Conversion:* monomer to final polymer conversion determined
169 by NMR was 75% with a recorded gravimetric yield of 70% (700 mg when aiming at theoretical

170 1000 mg of polymer). Further characterization is shown in Table 1. *Molecular Weight*: When
171 the degree of transesterification was below 10%, M_n values were evaluated by ^1H NMR.^[6]
172 **HEMAPCL-PTMC**. Characterization data was obtained after purification *via* three cycles of
173 precipitation in cold hexane-diethyl ether: ^1H NMR (400 MHz, CDCl_3): δ 6.14 (s, 1H), 5.61 (s,
174 1H), 4.40-4.20 (m, from HEMA and TMC), 4.08 (t, 2H*35), 3.80 (m, 2H), 2.33 (t, 2H*35),
175 1.97 (m, 3H), 2.04 (m, 2H *[M]:[I]), 1.67 (m, 4H*35), 1.41 (m, 2H*35), presence of residual
176 catalyst and solvents (from synthesis and purification) can be spotted. *Conversion*: TMC
177 monomer to final block copolymer monomer conversion determined by NMR was 80% with a
178 recorded gravimetric yield of 70%. Further characterization shown in Table 1. *Molecular*
179 *Weight*: As all polymers exhibited transesterification levels below 10% M_n values were
180 evaluated by ^1H NMR.^[6]

181 **HEMAPCL-PDLLA**. Characterization data was obtained after purification *via* three cycles of
182 precipitation in cold hexane-diethyl ether: ^1H NMR (400 MHz, CDCl_3): ^1H NMR (400 MHz,
183 CDCl_3): δ 6.14 (s, 1H), 5.61 (s, 1H), 5.19 (m, 2H*28), 4.40-4.20 (m, 5H from LA end group
184 and HEMA), 4.08 (t, 2H*35), 3.68 (m, 2H), 2.33 (t, 2H*35), 1.97 (m, 3H), 1.67 (m,
185 4H*35), 1.59 (m, 6H*28) 1.41 (m, 2H*35), presence of residual catalyst and solvents (from
186 synthesis and purification) can be spotted. *Conversion*: LA monomer to final block copolymer
187 monomer conversion determined was 80% with a recorded gravimetric yield of 75%. Further
188 characterization shown in Table 1. *Molecular Weight*: As all polymers exhibited
189 transesterification levels below 10% M_n values were evaluated by ^1H NMR.^[6]

190 **2.4 Characterization Methodologies**

191 **NMR Spectroscopy**: ^1H NMR spectra were recorded on a Bruker AV3400 400.1 MHz
192 spectrometer using CDCl_3 as the solvent reference (7.26 ppm). Chemical shifts are expressed
193 in parts per million (d) downfield from internal standard tetramethylsilane.

194 **2D-NMR Spectroscopy**: ^1H - ^{13}C heteronuclear single quantum correlation (HSQC) and ^1H -
195 ^{13}C heteronuclear multiple-bond correlation (HMBC) (one-bond suppression) spectra were

196 recorded on a Bruker AV 3500 (500.1 MHz for ^1H , 125.8 MHz for ^{13}C) spectrometer using
197 CDCl_3 as the solvent reference (7.26 ppm for ^1H , 77.16 ppm for ^{13}C). The final HSQC spectrum
198 depicts a peak for each unique pair of directly coupled nuclei (^1H - ^{13}C). The final HMBC
199 spectrum depicts correlations between coupled nuclei pairs (^1H - ^{13}C) that are separated by two
200 – four bonds, with direct one-bond correlations suppressed.

201 **GPC Analysis:** Gel Permeation Chromatography (GPC) was performed by using a PL50+
202 Polymer Laboratories system. An RI constructed calibration curve from PMMA (Mn range
203 350000-620 Da) was adopted to analyze polymer molar masses. 2 PL mixed-D columns at
204 50 °C were employed, using 0.1 % LiBr DMF as the mobile phase with a flow rate of 1 ml/min.

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211 3. Results and Discussion

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213 A number of prior reports have shown that TBD is an efficient acyl-transfer and
214 transesterification catalyst. Its high activity is linked to its ability to interact with both initiator
215 and monomer (**Scheme 1**),^[22] and it has been proposed to follow a pseudo bifunctional
216 nucleophilic catalytic mechanism.^[23] This feature allows TBD to catalyze the ROP reaction of
217 $\epsilon\text{-CL}$, commonly known as refractive monomer in ROP process, without the need to adopt a
218 co-catalyst (for example a thiourea) that is required for alternative organocatalyst such as
219 DBU.^[22] It the same way tin octoate, which is currently the most widely used catalyst for ROP,
220 exploits a coordination-insertion process allowing interactions with both initiator (nucleophile)
221 and monomer without the need of a co-catalyst.^[20] However, the main drawbacks related with
222 tin octoate are the intrinsic toxicity and the high temperature required to activate any ROP

223 reactions enabling intermolecular and intramolecular esterification to occur and thus
224 broadening the final polymer molecular polydispersity.^[22] .

225 On the basis of this, in the present work, it was speculated that TBD can also trigger a self-acyl
226 transfer of the methacrylic group of HEMA, producing ethylene bis-methacrylate and ethylene
227 glycol (**Scheme 2**).

228 This was supported by both species being detected in the ¹H NMR of the reaction mixture
229 (**Figure S1**). This HEMA self-transesterification can compete, as side reaction, with the ROP
230 process by altering the concentration and/or identity of the active initiator. Consequently, by
231 affecting the [M]:[I] ratio, the presence of this competitive acyl transfer process can severely
232 affect the quality of the final polymer in terms of molecular weight and architecture.

233 In order to evaluate the magnitude of the effect of the acyl transfer reaction, a kinetic study was
234 conducted by systematically varying the “high” and “low” [HEMA]:[TBD] ratios to mimic the
235 concentration ranges applied in an ideal ROP reaction to synthesize a 2000 Da and 10,000 Da
236 product. The results of these experiments are compared in **Figure 1** and the supporting NMR
237 data are shown in **Figure S1**.

238 These data show that transesterification is more pronounced when both the concentrations of
239 HEMA and TBD are at the “high” values, reaching almost 25 % of transesterification within 5
240 minutes. However, when the amount of HEMA was kept “high”, while the amount of TBD was
241 reduced to “low”, a reduction in transesterification was observed during the same time-frame,
242 namely, only 8-10 % of unwanted reaction was detected. Furthermore, when HEMA was
243 reduced (“low”), as expected, the kinetics of the reaction considerably reduced and,
244 independently of the TBD concentration, only 5-6 % of transesterification occurred after 5 min.

245 An unpaired t-test ($p < 0.05$ indicating significant difference) analysis was performed at each
246 time-point and confirmed that significant differences were observed at each time point between
247 the two selected initiator:catalyst ratios. Therefore, this set of experiments demonstrated that
248 keeping the HEMA concentration at the “low” level is important to reduce side-reactions.

249 We subsequently explored the ability of TBD to selectively catalyze ROP of lactide (LA), ϵ -
250 caprolactone (CL) and trimethylene carbonate (TMC) monomers, ^[18,22,23] while controlling
251 methacrylate transfer side reactions. LA polymerizations (**Figure 2**) were performed with
252 [LA]:[HEMA] ratios targeting final molecular weights of 5000 Da and 6500 Da (i.e. DP₀ of 35
253 and 45) respectively.

254 PDLLA polymers were produced within seconds of introducing the catalyst at room
255 temperature. The reactions exhibited good control of the molecular weight (\bar{M}_w/\bar{M}_n ranging from
256 1.18-1.21, **Table 1**), which was in agreement with prior literature reports.^[18,23]

257 The experimental DP of the PDLLA products (Entries 1 and 2, **Table 1**) were observed to match
258 the theoretical DP and subsequent analysis by ¹H-NMR (**Figure 2**) confirming the presence of
259 only a single set of methacrylic proton peaks indicating a good control of the polymer and no
260 evidence of transesterification.

261 Furthermore, 2D-NMR experiments indicated that the ROP mechanism was predominant, with
262 the HSQC spectrum (**Figure 3**) showing a single acrylic (vinylic) carbon peak directly
263 correlated to the two methacrylic protons (see inset **Figure 3A**). This confirms the presence of
264 only a single HEMA-terminated group per polymeric chain. The HMBC spectrum further
265 confirms a single correlation between the two methacrylic protons and both a single carbonyl
266 and methyl group species (**Figure 3B**), with no additional peaks related to the methacrylic
267 protons observed.

268 Good control over the final polymer features was also observed for the PTMC mono-
269 methacrylic polymer (**Figure 4**). Despite a change in the molecular structure of the cyclic
270 monomer, fast kinetics similar to that exhibited by the PDLLA were observed. The final
271 molecular weight was in agreement with the target of approximately 5000 Da as confirmed by
272 ¹H-NMR and GPC (Entry 3, **Table 1**). This confirmed the ability of TBD to selectively catalyze
273 the ROP of cyclic monomers of different molecular structures which exhibit fast polymerization
274 kinetics.

275 To exemplify further the importance of the TBD-catalyzed ring-opening kinetics to the
276 production of defined polymer structures, the polymerization of ϵ -CL was then explored, due
277 to its lower ROP reactivity when compared to monomers such as LA.^[18] In agreement with the
278 literature, a slower rate of polymerization was observed for CL when compared to LA and TMC
279 and as a consequence the overall reaction was noted to be less controlled (Entry 4-6, **Table 1**
280 and **Figure S3**). Analysis of the final products showed that this was due to both the tendency
281 of the PCL terminal chain group to transesterify^[18,24] and an increased level of HEMA:TBD
282 interaction prior to polymerization which generated a diol initiator over time. When the 1%
283 mol:mol of TBD:Monomer ratio was used as for TMC and LA, no CL polymerization was
284 observed. This was attributed to the slow ROP kinetics and consequent dominance of the self-
285 transesterification kinetics of HEMA. Thus, a TBD:monomer ratio of 2.5 % mol:mol was then
286 adopted. Polymerization was observed, and the reaction was complete within 120-240 min (see
287 Entry 4, **Table 1** and **Figure S2**). The formation of sub-products was evident in the NMR
288 analysis (**Figures S3** and **Figure 5** see methacrylate peaks inset). Thus, it was not possible to
289 evaluate the final molecular weight by ¹H NMR, due to a splitting of the HEMA peaks and the
290 contribution to the polymeric CL peaks arising from polymer formed from other initiating
291 species such as the diol. As a consequence, a broader value of \bar{M}_n (1.55) was observed in the
292 GPC data. The ¹H-NMR spectra showed that the transesterification occurred over time as the
293 splitting of the vinyl peaks in the 6.20 to 5.50 ppm region increased as the reaction proceeded
294 (see **Figure S2-S3**). This splitting was in accordance with the initial screening reported in
295 **Figure S1**.

296 A series of 2D-NMR experiments were performed, to clarify the presence of both HEMA and
297 methacrylic end-capped terminal groups and to link unambiguously the vinyl peak splitting to
298 a transesterification process. The HSQC spectrum (**Figure S3**) showed the presence of two
299 different types of carbons correlating to the two sub-families of methacrylic proton peaks. This
300 indicates the presence of two unique end-capping methacrylic groups, and thus an undesired

301 end-terminal methacrylic group in addition to the HEMA-initiation end-terminus. This was
302 further exemplified in the HMBC spectra, where two sets of multiple-bond correlations between
303 the two types of methacrylic protons and both of the two kinds of carbonyl and methyl group
304 species were observed (**Figure S4**).

305 By reducing the TBD loading to 1.5 % mol:mol, HEMAPCL could be synthesized with a
306 significant reduction of the side acyl transfer reactions (see ¹H-NMR, **Figure 5**, **Figure S5** and
307 **Entry 6, Table 1**).

308 Using these conditions and restricting the reaction time to 120 min, an average conversion of
309 monomer to polymer of *circa* 60-70 % could be reached before the reaction was quenched. This
310 confirmed that by reducing the amount of TBD, and thus tuning the initial HEMA:TBD ratio,
311 there was a drop in the undesired transesterification reaction at the 1.5 %mol:mol when
312 compared with the PCL synthesized using 2.5 % mol:mol of catalyst (see inset within **Figure**
313 **5**). At this TBD concentration only 2 to 5 % of bis-methacrylic chains were observed in a series
314 of experiments with targeted molecular weights of approximately 2500 and 5000 Da (Entries 5
315 and 6, **Table 1**) compared to the ~ 50% observed in prior literature by using Lipase catalysts.^[16]

316 Finally, in order to assess the level of retention of the hydroxyl group at the end of each
317 polymeric chain and thus confirming good end group fidelity, HEMA initiated PCL with a
318 targeted DP₀ of 35 (see **Entry 6, Table 1**) was then employed as a macroinitiator for the
319 synthesis of block copolymers with TMC or LA as the chain extending monomers. The targeted
320 DP₀ for the second TMC block was 10 units whilst for LA was 35 units (i.e. 35 + DP₀10 of
321 TMC or 35 + DP₀ 35 of LA). After the polymerization of TMC and post-purification steps an
322 experimental DP_e of 8 was observed (**Entry 7, Table 1** and **Figure 6**). For the LA extension, a
323 conversion of 80 % in the second block of PDLLA was achieved to reach a DP_e of 28 (**Entry 8**
324 **Table 1**), which is what would be expected from the conversion corrected target. In both cases,
325 the characteristic NMR peaks attributed to the main chains TMC and LA were present in spectra
326 of the final copolymer as were the characteristic end groups for the second added monomer

327 **(Figure 6 Left)**. Increases in the molecular weight of the polymers compared to that of the
328 HEMA initiated PCL-macroinitiator **(Figure 6 Right)** were evident in the GPC chromatograms,
329 i.e. 4307 Da (\bar{M}_n of 1.13) to 6295 Da (\bar{M}_n of 1.09) and 8125 Da (\bar{M}_n of 1.15) for TMC and LA
330 respectively. This confirmed the formation of block copolymers. The existence of only a single
331 peak for the sequential block copolymers proved the successful control over the addition of the
332 second monomer onto the initial HEMAPCL macroinitiator.

333 The success of the regrowth from the macro-initiator in this proof-of-concept experiment
334 confirmed both the control of the reaction conditions for the production of block copolymers,
335 as well as the end group (hydroxyl group in this case) fidelity that can be achieved in the
336 production of the macro-initiator. The increase in molecular weight shown in the GPC traces
337 (Entries 7 and 8, **Table 1**) to produce single monodispersed peaks confirmed both the
338 availability of the hydroxyl PCL terminal group to initiate the polymerization of the second
339 sequential block and the level of control exercised over the extension step on the initial
340 HEMAPCL macro-initiator.

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345 **4. Conclusions**

346 The synthetic strategy reported here is the first example of successful HEMA-initiated ROP
347 catalyzed by TBD. To highlight the novelty and the broad applicability of the synthetic
348 methodology developed in the present work, it is important to note that in recent work it has
349 been reported that when TBD was adopted, as catalyst of ROP reactions, with HEMA as
350 nucleophilic initiator, no controlled polymerization events were observed due to a series of
351 uncontrollable side reactions.^[20] Consequently, tin octoate was needed to prepare the targeted
352 (metha)acrylated-macromolecules. On the contrary, the present study has demonstrated that
353 TBD indeed can be employed as an active and selective catalyst for HEMA-initiated ROP of

354 LA, TMC, and CL, to synthesize polymers and block copolymers with controlled molecular
355 weight, low polydispersity and a mono-methacrylate final architecture (see **Table 1**).

356 Success in achieving the target ROP while minimizing polyester transesterification reactions
357 was demonstrated to be minimal when fast polymerization kinetics were obtained from the
358 monomer of choice. In the cases where monomer types presenting slower kinetics were
359 employed, both significant levels of “by-products” (> 50%) and subsequent loss of control over
360 the molecular structure of the polymer was observed. This study has shown that these unwanted
361 side reactions could be minimized (i.e. reduced to < 5%) by controlling the relative
362 HEMA:TBD ratio and the reaction time.

363 This study has also concluded that TBD is a more efficient ROP catalyst when compared to
364 lipases. In fact, it has been well documented that lipases cannot discriminate ROP from the
365 transesterification sub-processes in the presence of cleavable ester initiators such as HEMA,
366 even at low monomer conversion.^[16,17] This leads to the production of di-methacrylated
367 macromolecular chains and an inability to produce well-defined polymers. By comparison, this
368 study has demonstrated that, by using TBD as a catalyst in small scale reactions and adopting
369 the simple precautions of controlling the catalyst concentration and reaction times, mono-
370 methacrylated chains with no (for HEMA initiated PDLLA and HEMA initiated PTMC) or
371 limited (<5 % for HEMA initiated PCL) di-methacrylated chains can be produced. Additionally,
372 this ROP reaction can be achieved with reagents that are readily available and under mild
373 reaction conditions, i.e. room temperature and atmosphere, in comparison to tin octoate that
374 requires high temperature and longer reaction time. All the aforementioned properties of TBD
375 will facilitate the production of biodegradable polymers bearing an active (metha)acrylic group
376 with the view to produce novel biodegradable architectures not achievable with one synthetic
377 approach alone.^[27] In particular, HEMA-terminated-polyester macromonomers have been used
378 in copolymerization with a plethora of methacrylic-acrylic monomers,^[27] to produce graft-
379 copolymers *via* controlled radical polymerization techniques such as ATRP^[27] and RAFT.^[27]

380 By rendering more accessible and easier the ROP step it would quickly broaden the number of
381 possible novel “smart materials” that can be explored and developed.

382 Furthermore, it has also been shown that it is possible to produce block copolymers via
383 sequential ROP reaction from a preformed macroinitiator using the same processing strategies
384 with TBD. This confirms TBD as an accessible catalyst for solution-phase ROP of cyclic esters
385 initiated by cleavable esters and, as the macro-initiators chosen were synthesized from
386 caprolactone, it also confirms the high level of hydroxyl termination when the correct synthetic
387 strategies were applied. Thus, TBD has been shown to be a practical alternative to metal-based
388 catalysts that exhibits higher selectivity than Lipases in the reactions tested.

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392 **Acknowledgements**

393 This work was supported by the Engineering and Physical Sciences Research Council [grant
394 numbers EP/N024818/1, EP/N03371X/1, EP/H005625/1, EP/N006615/1]; grant names:
395 Formulation for 3D printing, creating a plug and play platform for a disruptive U.K. industry,
396 Radiotherapy activated materials for enhanced cancer treatments, Bar-Coded Biomaterials -
397 Designing Self-Authenticating Medicines and Programme Grant for Next Generation
398 Biomaterials Discovery. This work was also funded by the Royal Society (Wolfson Research
399 Merit Award WM150086 (to CA).

400

401 **Keywords:** Ring-Opening Polymerization, triazabicyclodecene (TBD) catalyst, hydroxyethyl-
402 methacrylate (HEMA) initiated, monofunctional -methacrylate polyesters

403

404 **Data access statement**

405 All raw data created during this research are openly available from the corresponding author
406 (vincenzo.taresco@nottingham.ac.uk) and at the University of Nottingham Research Data

407 Management Repository (<https://rdmc.nottingham.ac.uk/>) and all analyzed data supporting this
408 study are provided as supplementary information accompanying this paper.

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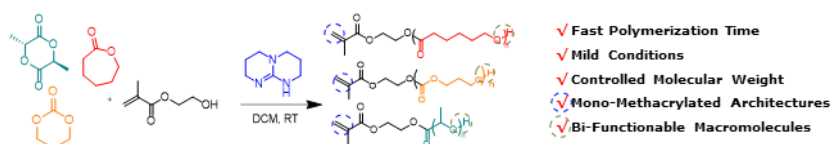
459 TOC

460 **Methacrylated block co-polyesters were synthesized via TBD catalyzed ROP.** TBD has
461 been successfully employed as an active and selective catalyst for HEMA- initiated ROP of LA,
462 TMC, and CL in order to synthesize, under mild and standard laboratory conditions,
463 homopolymers and block copolymers with controlled molecular weight, low polydispersity and
464 a mono-methacrylate final architecture.

465
466 Laura A. Ruiz-Cantu, Amanda K. Pearce, Laurence Burroughs, Thomas M. Bennett, Catherine
467 E. Vasey, Ricky Wildman, Derek J. Irvine*, Cameron Alexander*, and Vincenzo Taresco*

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471 **Synthesis of Methacrylate-Terminated Block Copolymers with Reduced** 472 **Transesterification by Controlled Ring-Opening Polymerization**



489 **Captions to Figures, Schemes and Tables**

490 **Scheme 1.** ϵ -CL ROP dual activation mechanism in presence of a generic alcohol catalyzed by
491 TBD.

492 **Scheme 2.** Schematic of TBD triggered self-acyl transfer of the methacrylic group of HEMA
493 producing ethylene bis-methacrylate and ethylene glycol from 2 equivalent of HEMA.

494 **Figure 1.** Comparison of the kinetic profiles showing the level of transesterification achieve
495 when varying the relative quantities of HEMA and TBD. An unpaired t-test ($p < 0.05$ indicating
496 significant difference) analysis was performed at each time-point and confirmed that significant
497 differences were observed at each time point between the two selected initiator:catalyst ratios.
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499 **Figure 2.** (Top) LA reaction scheme, polymer stoichiometry takes into account the corrected
500 conversion. (bottom) Full ^1H -NMR spectrum of purified HEMAPDLLA 5000, in the 7.5 to 1.0
501 ppm spectral range. Note: residual catalyst and diethyl ether in the spectral range of 4.0 to 3.2
502 ppm.

503 **Figure 3. A)** HSQC NMR spectra of PDLA, showing the presence of a single methacrylic
504 species (inlay) in the final polymer and confirming the presence of a single HEMA end group
505 for each polymeric chain. Peaks assigned a1 and b1 represent the two vinyl protons and c1
506 represents the vinylic carbon. **B)** HMBC ^1H - ^{13}C NMR spectra of HEMA initiated PDLA,
507 demonstrating the presence and multiple bond correlations confirming (inlay top) a single
508 methyl (methacrylate) species and (inlay bottom) a single carbonyl (methacrylate) species in
509 the final polymer.

510 **Figure 4.** (Top) HEMA initiated TMC reaction scheme, polymer stoichiometry takes into
511 account the corrected conversion and (Bottom) ^1H NMR spectrum. Inset, the vinyl region which
512 exhibits only two peaks as expected, demonstrating a satisfactory controlled ROP without side-
513 transesterification.

514 **Figure 5.** (Top) HEMAPCL reaction scheme, polymer stoichiometry takes into account the
515 corrected conversion. (Bottom) ^1H -NMR spectrum of HEMAPCL (synthesized employing 1.5

516 % mol:mol TBD) (red traces) showing a reduction of the vinyl peaks related to the
517 transesterification sub-products in the range of 6.2-5.5 ppm. (Inset) Difference in magnitude of
518 transesterification between the polymer synthesized with 2.5% (blue trace) and 1.5% (red trace)
519 catalyst.

520 **Figure 6. LEFT.** Stacking $^1\text{H-NMR}$ spectra, in the region between 6.5 to 3.5 ppm, of
521 HEMAPCL macroinitiator (red trace), HEMAPCL-PTMC (green trace) and HEMAPCL-
522 PDLLA (black trace) block copolymers showing that they characteristic peaks for PTMC and
523 PLA end groups, there PCL, PTMC and PDLLA end group functionalities are shown as *, Δ
524 and + respectively. **RIGHT.** GPC traces of HEMAPCL, HEMAPCL-PTMC and the
525 HEMAPCL-PDLLA block copolymers.

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543 **Table 1.** Characterization data for ROP polymers synthesized using HEMA, TBD. $DP_0 =$
 544 Theoretical M_n , $DP_e =$ Experimentally observed M_n (NMR) post-purification and DP_c is the
 545 conversion corrected M_n .

	Polymer (TBD Mole % wrt Monomer)	Time (Min)	DP₀:DP_c:DP_e	M_n^a (GPC) (g mol ⁻¹)	M_n^b (NMR) (g mol ⁻¹)	Đ	Yield^c (%)	Trans (%)
1	HEMAPDLLA (1.0)	< 3	35:33:35	4930	5090	1.18	95	--
2	HEMAPDLLA (1.0)	< 3	45:43:43	7860	6120	1.21	95	--
3	HEMAPTMC (1.0)	< 3	49:45:50	3600	5175	1.25	90	--
4	HEMAPCL (2.5)	120	45:--:--	3860	---	1.51	75	> 30
5	HEMAPCL (1.5)	120	22:17:24	3155	2780	1.14	75	< 3
6	HEMAPCL (1.5)	120	45:34:35	4310	4170	1.13	75	< 5
7	HEMAPCL- PTMC (1.0)	< 3	35+10:35+8: 35+10	6295	5190	1.09	80	< 3
8	HEMAPCL- PDLLA (1.0)	< 3	35+35:35+23 :35+28	8125	8200	1.15	80	< 3

546 a) Referenced to PMMA standards, ^{b)} calculated by ¹H-NMR, ^{c)} Quoted to nearest 5%

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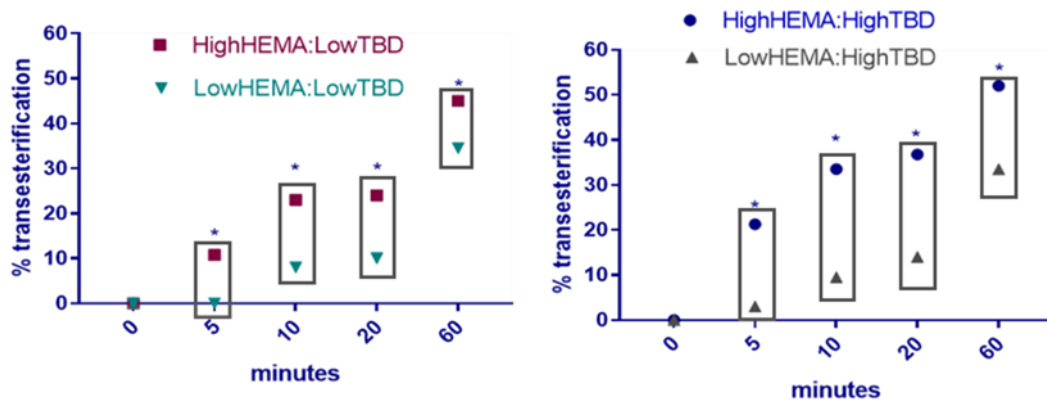
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559 **Figure 1**



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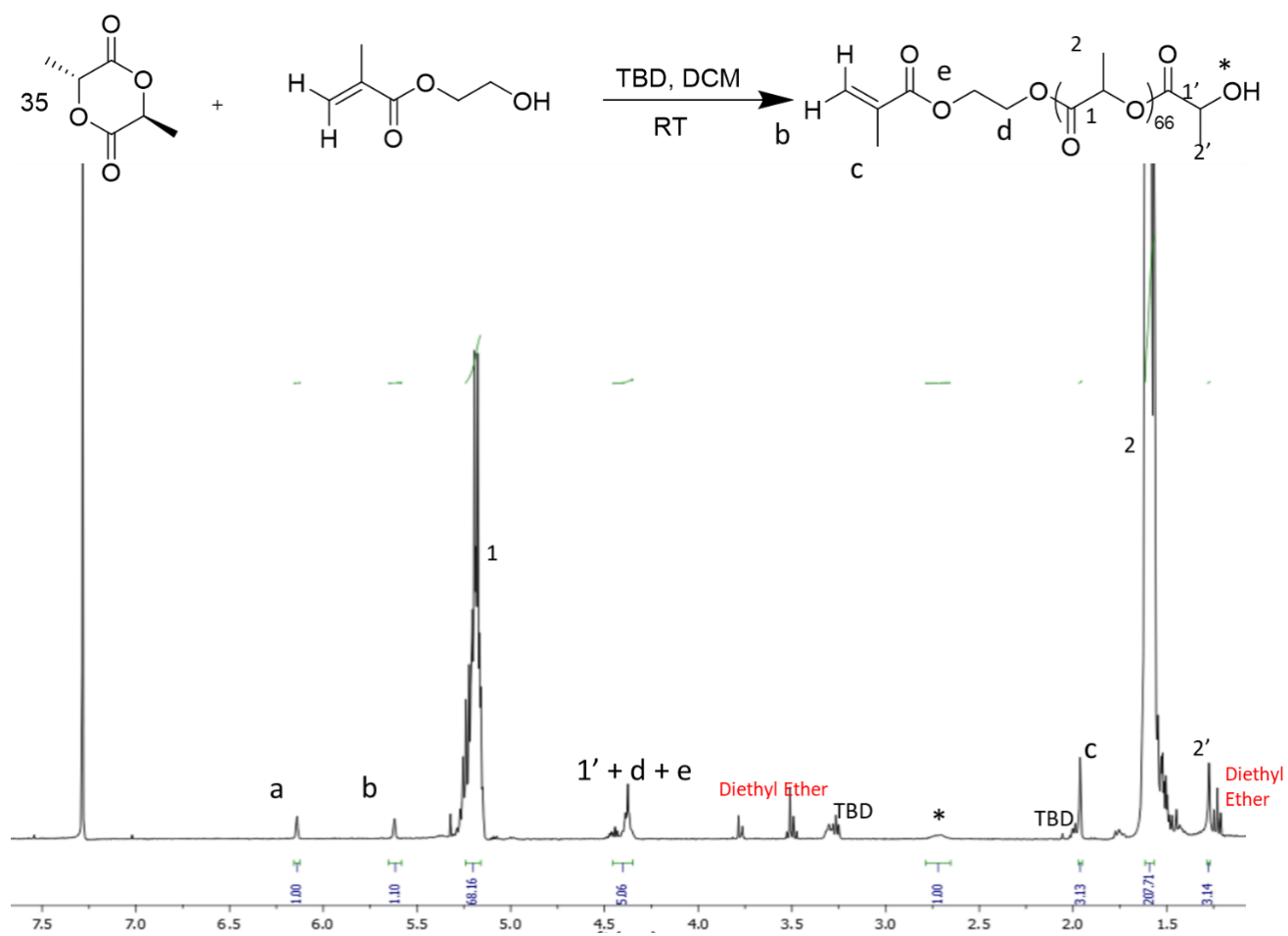
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579 **Figure 2**

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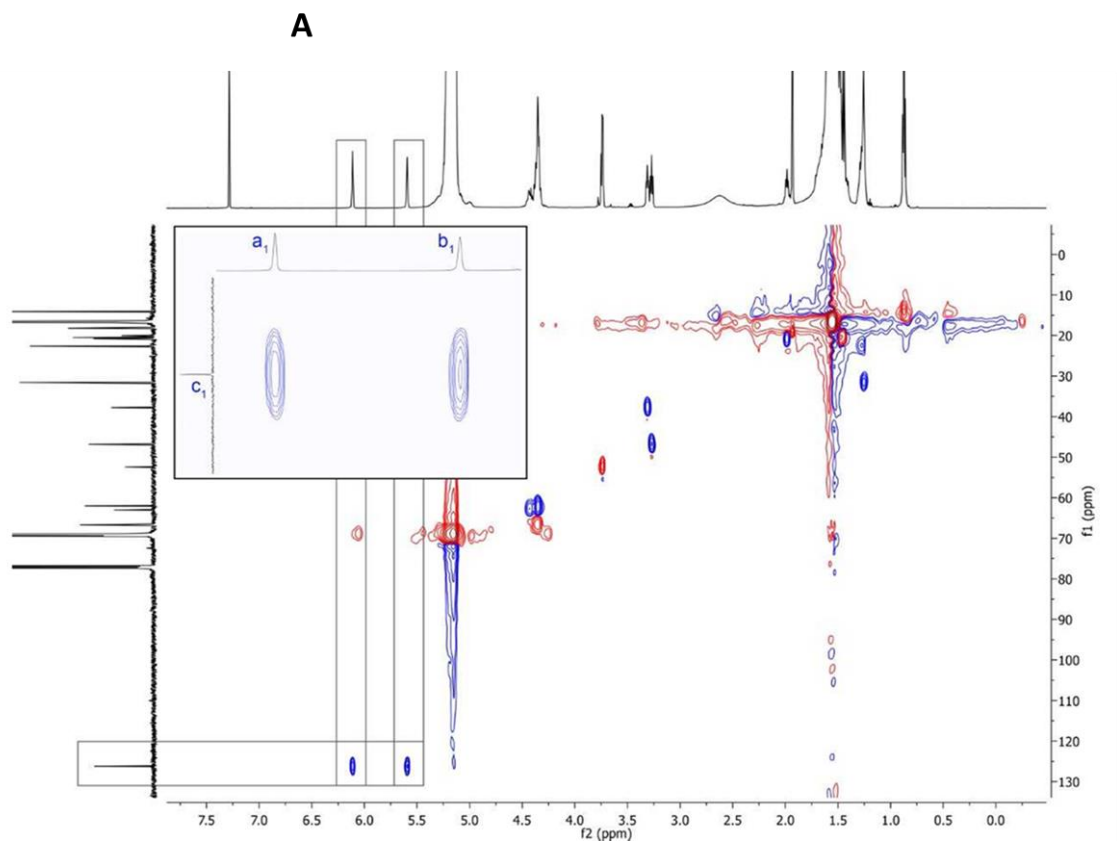
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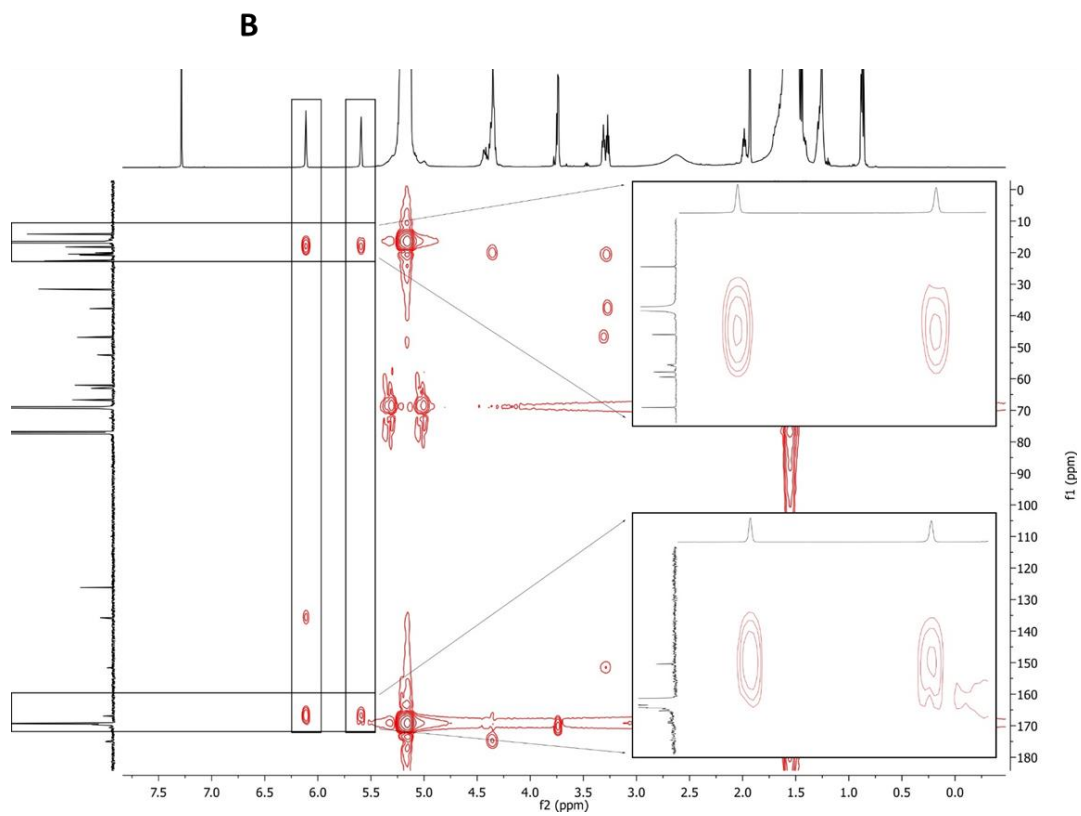
603 **Figure 3**

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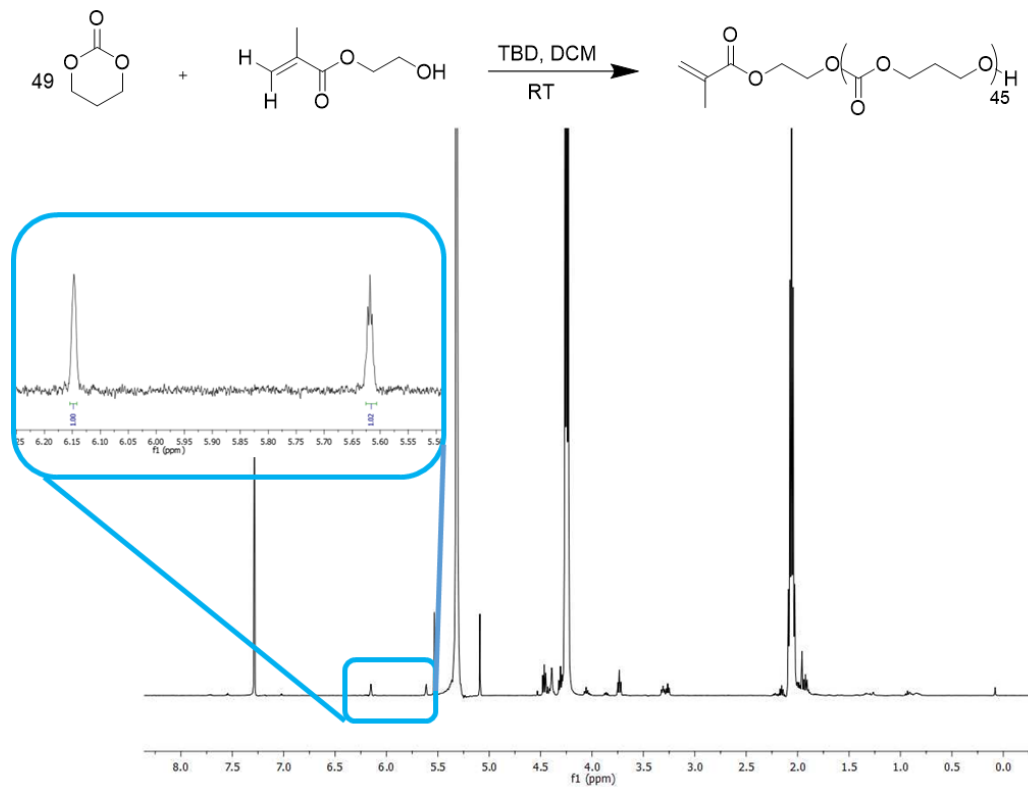
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609 **Figure 4**

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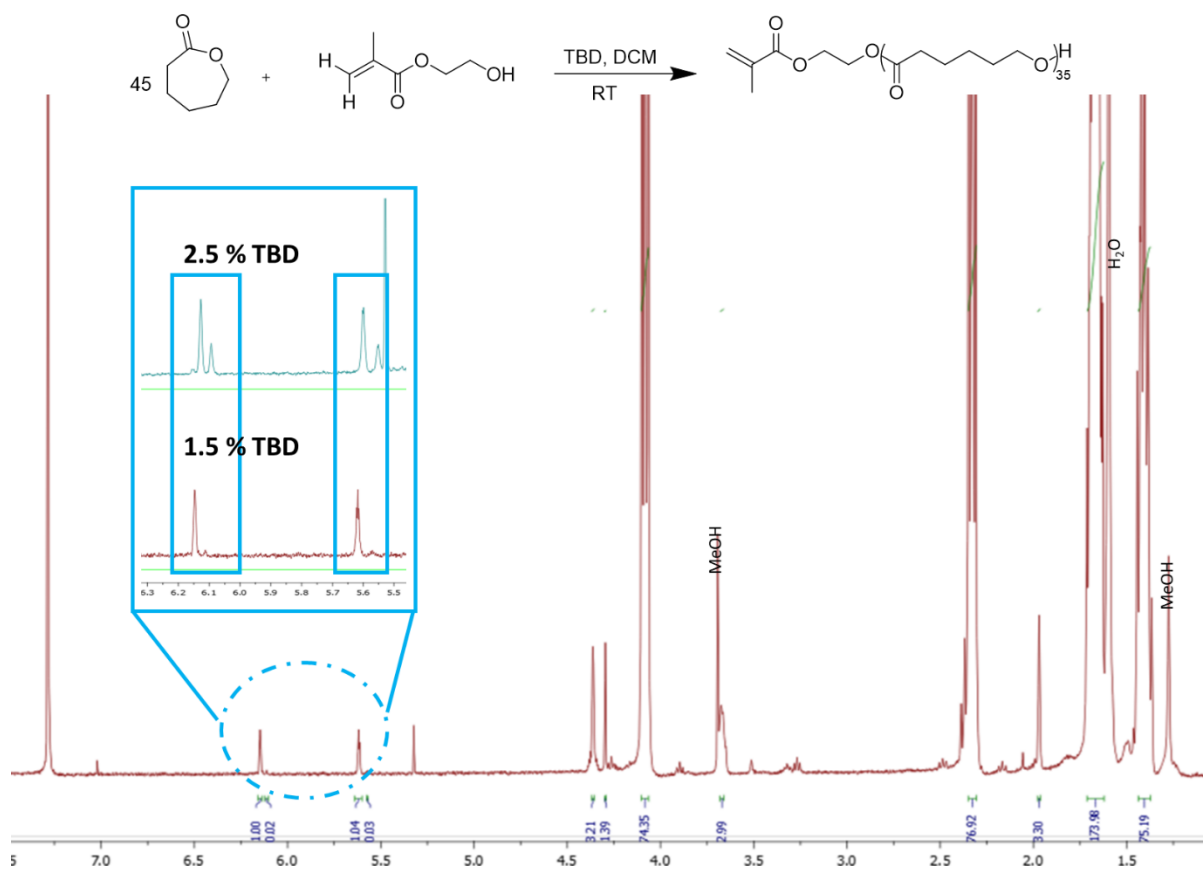
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636 **Figure 5**



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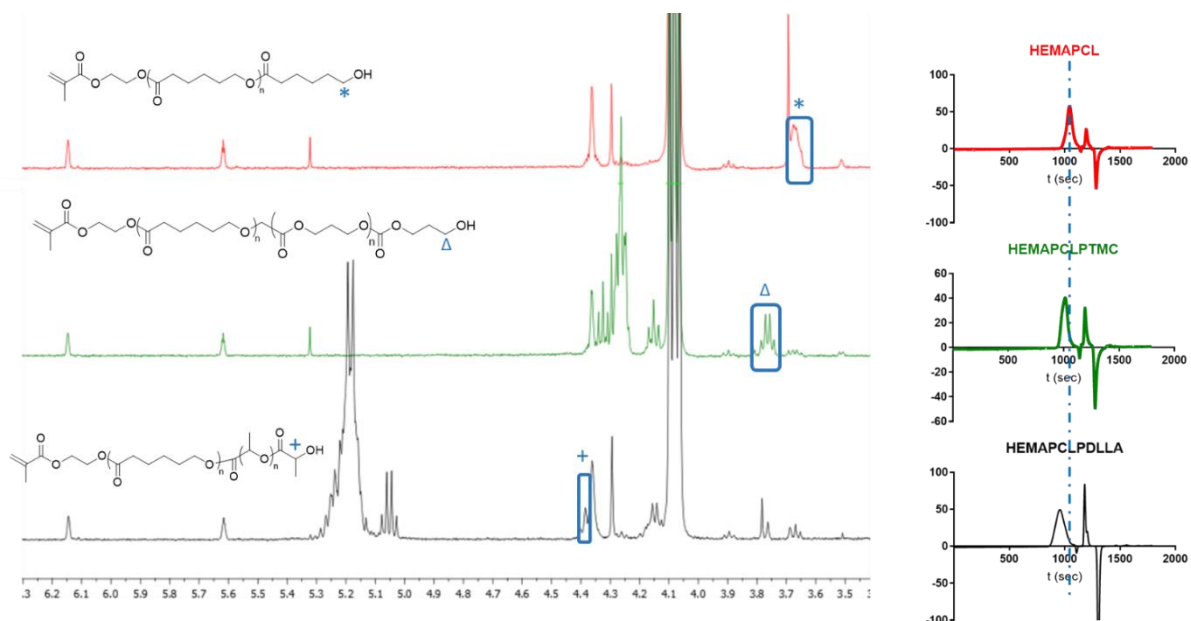
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663 **Figure 6**

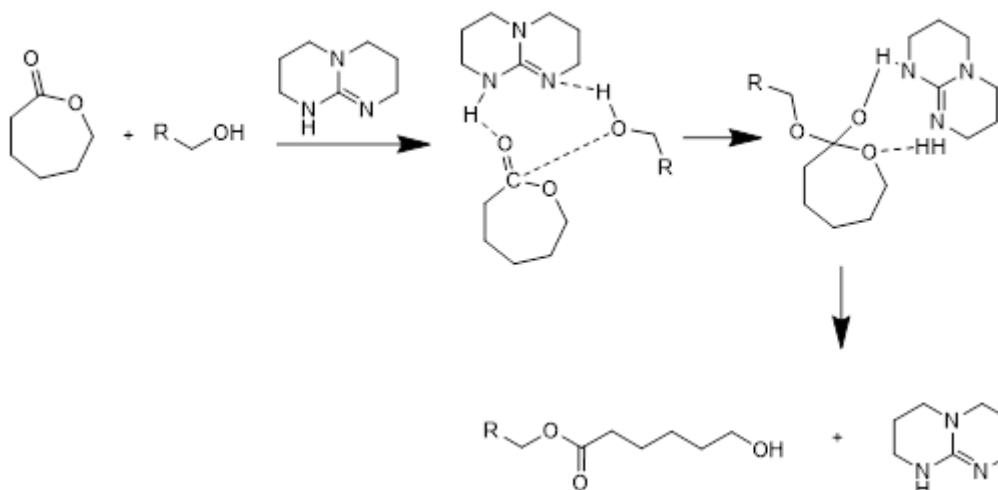
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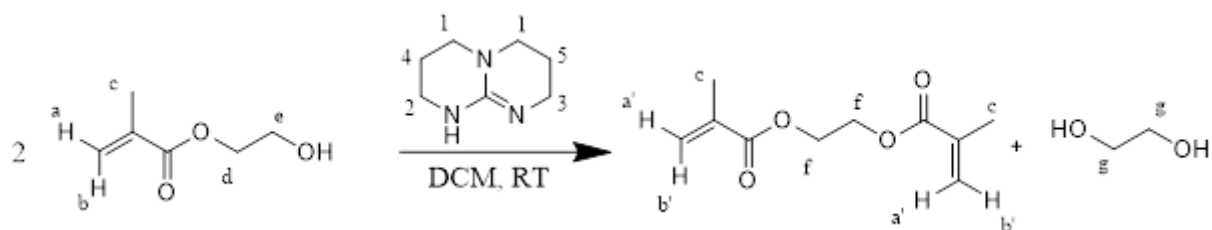
Scheme 1

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686 **Scheme 2**
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730 **Supporting Information**731
732733 **Synthesis of Methacrylate-Terminated Block Copolymers with Reduced**
734 **Transesterification by Controlled Ring-Opening Polymerization**

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754 **Figure S1.** NMR kinetics of HEMA self-transesterification in presence of TBD.

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756 **Figure S2.** Kinetic profile of HEMAPCL ROP.757 **Figure S3.** HEMAPCL reaction scheme and detailed NMR spectra.758 **Figure S4.** HMBC ¹H-¹³C NMR spectra of HEMAPCL.759 **Figure S5.** ¹H-NMR of HEMAPCL polymers showing full integration

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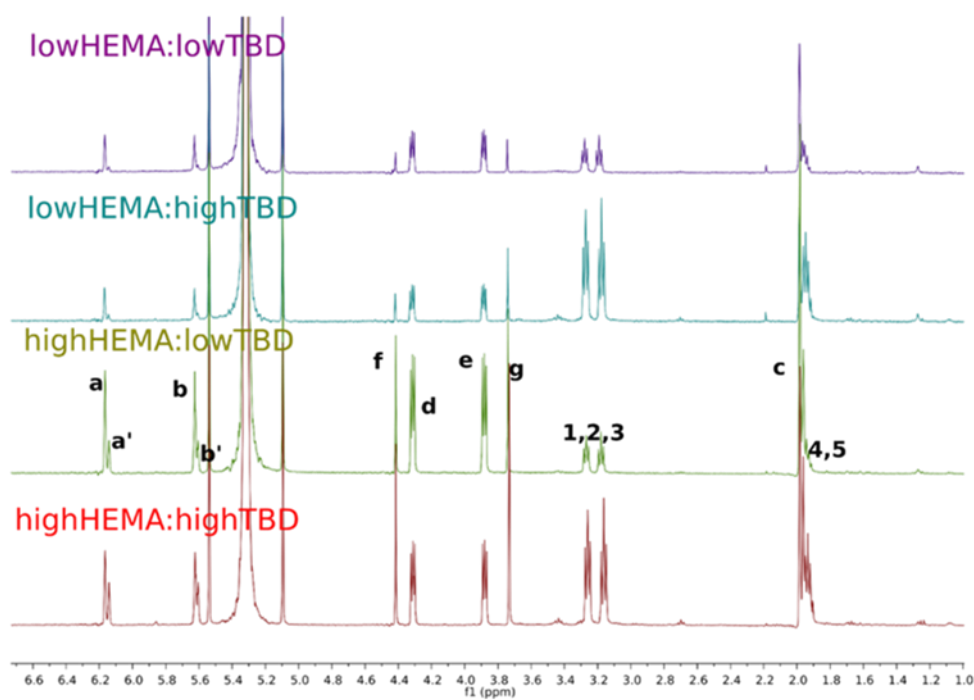
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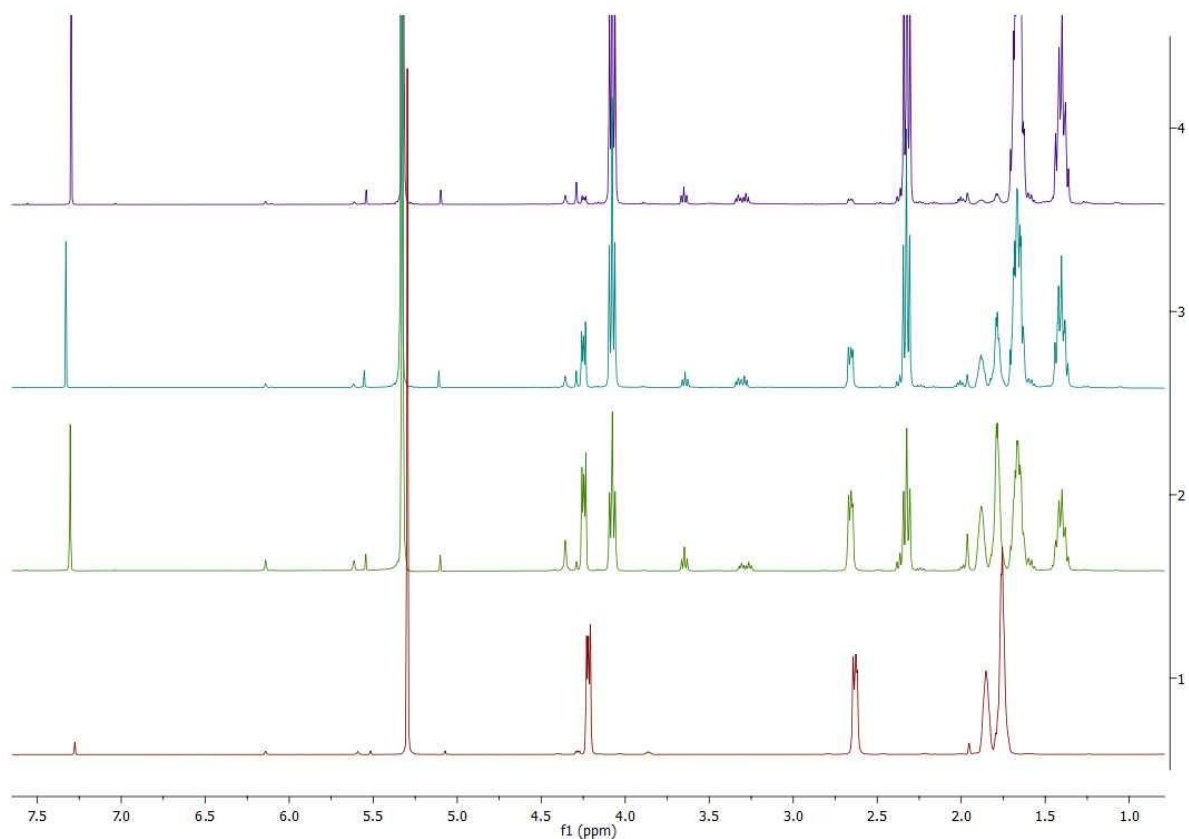
767 **Figure S1.** NMR spectra confirming feed ratio (HEMA:TBD) dependent presence of both
768 ethylene bis-methacrylate and ethylene glycol as secondary species.

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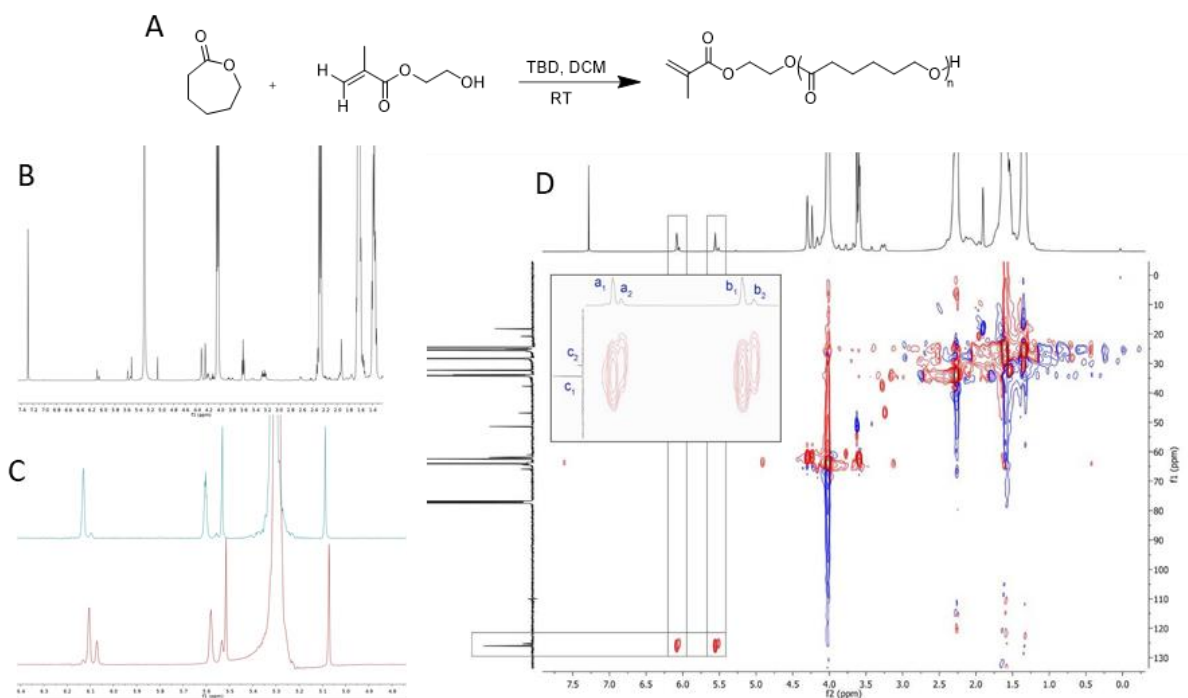
774 **Figure S2:** Kinetic profile of HEMAPCL ROP at 0, 20, 60, and 240 minutes (from bottom to
775 top). Note: 240 min is shown to justify the full conversion of monomer to polymer.

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781 **Figure S3. A)** CL scheme of reaction. **B)** Full ^1H -NMR spectrum HEMAPCL. **C)** Stacked ^1H -
 782 NMR methacrylic protons region; peaks splitting in two limiting acyl transfer conditions (6.1-
 783 5.5 ppm). **D)** HSQC NMR spectra of HEMAPCL, confirming the presence of a two different
 784 methacrylic species (inlay) in the final polymer. Peaks assigned a1, a2, b1 and b2 represent the
 785 4 vinyl proton species, and c1 and c2 represent the 2 vinylic carbon species in the final polymer.
 786 This effect is easily observed when a high amount of TBD was used leading to an uncontrolled
 787 polymer functionalization.

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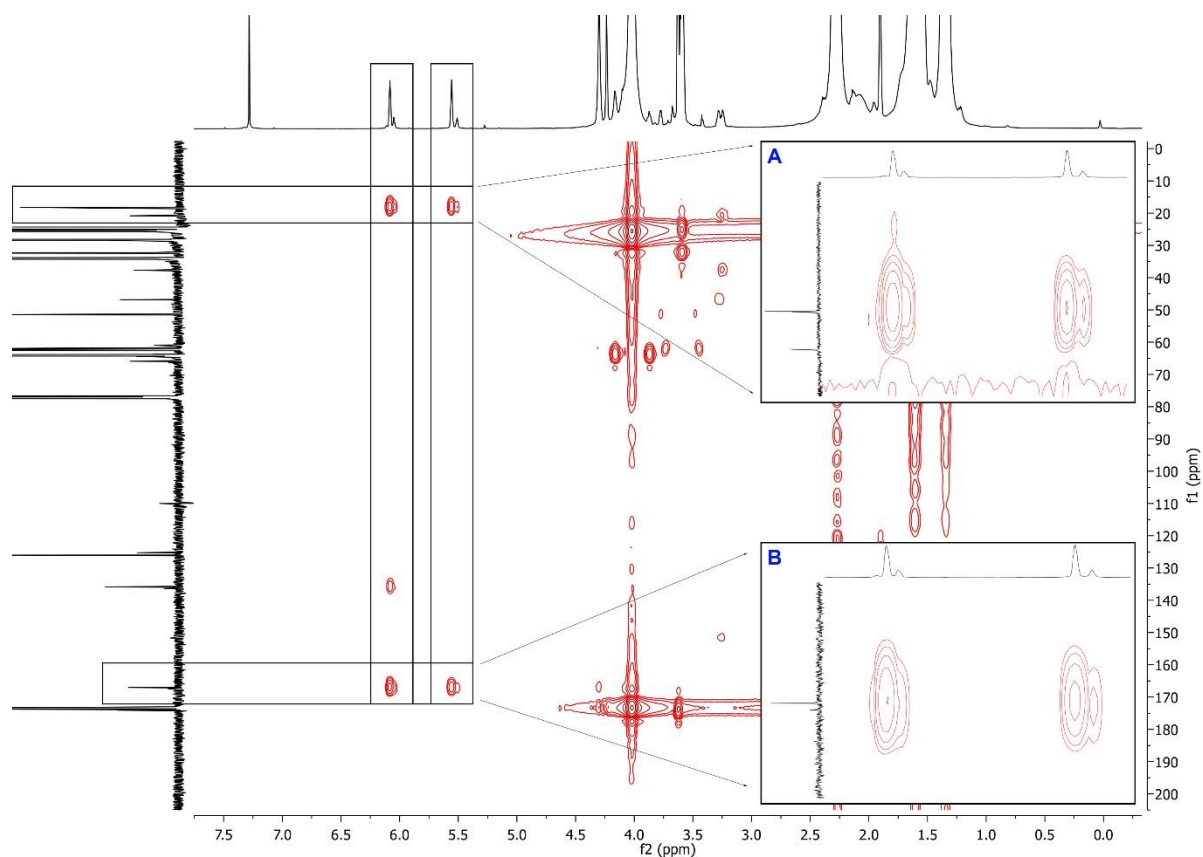
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803 **Figure S4.** HMBC ^1H - ^{13}C NMR spectra of HEMAPCL, demonstrating the presence and
804 multiple bond correlations confirming (inlay a) two different methyl (methacrylate) species and
805 (inlay b) two different carbonyl (methacrylate) species in the final polymer. This effect is easily
806 observed when a high amount of TBD was used leading to an uncontrolled polymer
807 functionalization.

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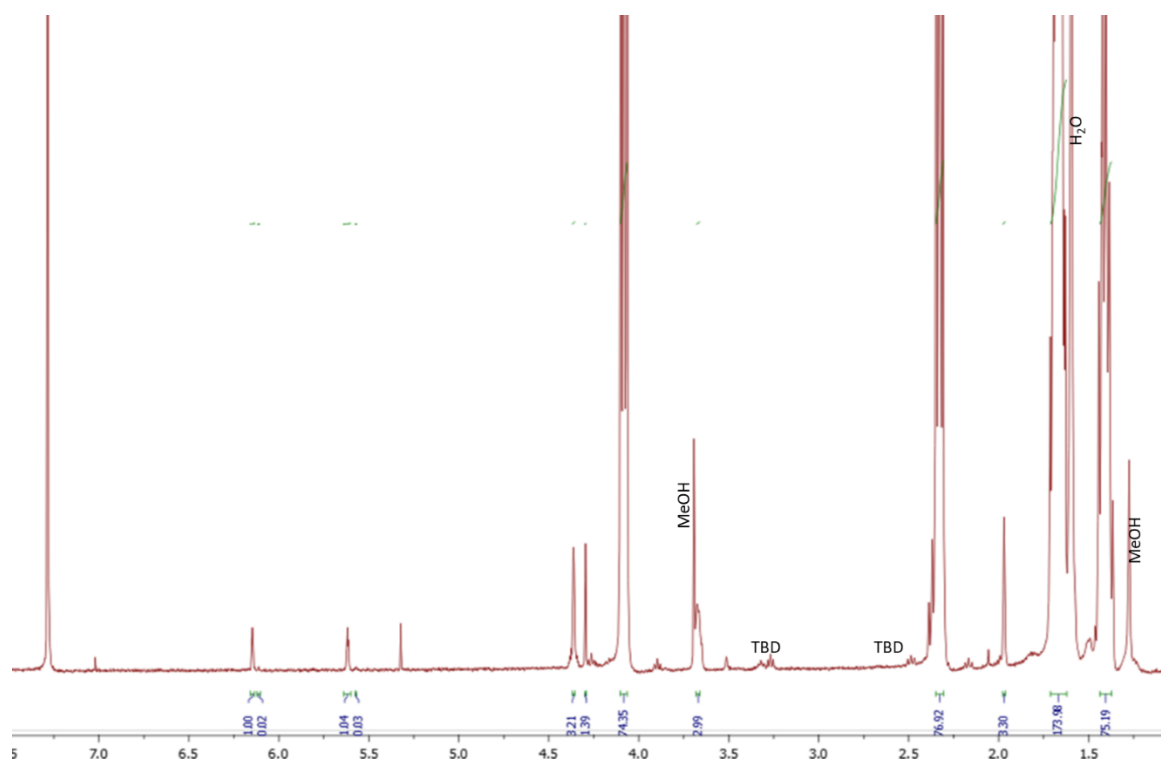
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822 **Figure S5.** ¹H-NMR of HEMAPCL polymers showing full integration, vinyl peaks splitting
823 ratios and PCLHEMA functionality proportions.

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